

November 7, 2016

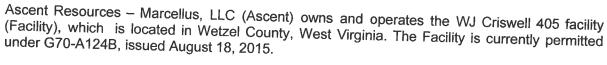
Division of Air Quality 601 57th Street, SE Charleston, WV 25304

**RE: Application for Rule 13 Construction Permit** 

Ascent Resources - Marcellus, LLC

WJ Criswell 405 Facility ID: 103-00098

Dear Sir/Madam,



Ascent is removing one (1) natural gas-fired compressor engine, updating the production and tank information, and requesting a conversion to a Rule 13 permit. To authorize the operation of equipment at the Facility, Ascent is submitting this application for a Rule 13 Construction Permit. The Facility consists of one (1) natural gas-fired generator, three (3) gas production units, one (1) line heater, one (1) flash separator heater, one (1) condensate stabilizer heater, three (3) condensate storage tanks, three (3) produced water storage tanks, one (1) enclosed combustor, and various support operations.

This Application has been prepared in accordance with the requirements set forth in 45CSR6, 45CSR13, and applicable guidance documents. Ascent will operate the Facility in compliance with applicable federal and state air quality regulations. The required attachments are included in addition to the application forms.

Enclosed is the original and two (2) copies of the application, along with the fee in the amount of \$2,000. If you have any questions or need additional information, please feel free to contact me at 405-252-7753.

Sincerely,

**Evan Foster Pearson** 

EH&S Air Compliance Specialist

**Enclosures** 

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#### WEST VIRGINIA DEPARTMENT OF ENVIRONMENTAL PROTECTION

# **DIVISION OF AIR QUALITY**

601 57th Street, SE

## APPLICATION FOR NSR PERMIT AND

Charleston, WV 25304 (304) 926-0475  www.dep.wv.gov/dag	TITLE V PERMIT REVISION (OPTIONAL)	
PLEASE CHECK ALL THAT APPLY TO NSR (45CSR13) (IF KNOW CONSTRUCTION MODIFICATION RELOCATION CLASS I ADMINISTRATIVE UPDATE AFTER-THE-FACT	☐ ADMINISTRATIVE AMENDMENT ☐ MINOR MODIFICATION ☐ SIGNIFICANT MODIFICATION	
FOR TITLE V FACILITIES ONLY: Please refer to "Title V Revi (Appendix A, "Title V Permit Revision Flowchart") and ability	sion Guidance" in order to determine your Title V Revision options y to operate with the changes requested in this Permit Application.	
Section Section	I. General	
Name of applicant (as registered with the WV Secretary of Ascent Resources – Marcellus, LLC	State's Office):  2. Federal Employer ID No. (FEIN): 46-5580354	
Name of facility (if different from above):     WJ Criswell 405	4. The applicant is the:  ☐ OWNER ☐ OPERATOR ☒ BOTH	
5A. Applicant's mailing address: PO Box 13678  SB. Facility's present physical address: 39.60737°N, -80.61828°W Four Mile Road, Wileyville, WV 26186		
6. West Virginia Business Registration. Is the applicant a resi  If YES, provide a copy of the Certificate of Incorporation/Control change amendments or other Business Registration Certificate  If NO, provide a copy of the Certificate of Authority/Authoramendments or other Business Certificate as Attachment	dent of the State of West Virginia?  YES NO  Drganization/Limited Partnership (one page) including any name atte as Attachment A.	
<ol><li>If applicant is a subsidiary corporation, please provide the nar</li></ol>	me of parent corporation:	
<ul> <li>8. Does the applicant own, lease, have an option to buy or other</li> <li>If YES, please explain: Lease</li> <li>If NO, you are not eligible for a permit for this source.</li> </ul>	wise have control of the proposed site? YES NO	
<ol> <li>Type of plant or facility (stationary source) to be constructed administratively updated or temporarily permitted (e.g., c crusher, etc.): Natural gas production</li> </ol>	I, modified, relocated, oal preparation plant, primary Classification System (NAICS) code for the facility: 211111	
G	st all current 45CSR13 and 45CSR30 (Title V) permit numbers sociated with this process (for existing facilities only): 70-A124B	
All of the required forms and additional information can be found un	der the Permitting Section of DAQ's website, or requested by phone.	

12A.				
For Modifications, Administrative Updates or I present location of the facility from the nearest state.	Femporary permits at an existing facility	/, please provide directions to the		
present location of the facility from the nearest sta     For Construction or Relocation permits, please road. Include a MAP as Attachment B.				
From Wileyville, WV, head south on Fairview Ridge Rd Turn right onto Barker Run Rd. and go 3.6 mi. Tu mi to facility location.	l. toward WV-7 W. Turn left at the first cr rn left onto N Fork Rd and go 4.4 mi. Tu	oss street onto WV-7 E for 1.6 mi. rn left onto Four Mile Rd. and go 0.9		
12.B. New site address (if applicable):	12C. Nearest city or town:	12D. County:		
	Wileyville	Wetzel		
12.E. UTM Northing (KM): 4,384.25	12F. UTM Easting (KM): 532.769	12G. UTM Zone: 17		
13. Briefly describe the proposed change(s) at the facili Ascent is removing one (1) natural gas-fired compresso	r engine and updating the production.			
<ul> <li>14A. Provide the date of anticipated installation or chan</li> <li>If this is an After-The-Fact permit application, proved change did happen:</li> </ul>	vide the date upon which the proposed	14B. Date of anticipated Start-Up if a permit is granted:		
14C. Provide a Schedule of the planned Installation of application as Attachment C (if more than one uni	it is involved).	units proposed in this permit		
<ol> <li>Provide maximum projected Operating Schedule o Hours Per Day 24 Days Per Week 7</li> </ol>	f activity/activities outlined in this applica Weeks Per Year 52	tion:		
16. Is demolition or physical renovation at an existing fac-	cility involved? YES NO			
17. Risk Management Plans. If this facility is subject to	112(r) of the 1990 CAAA, or will become	e subject due to proposed		
changes (for applicability help see www.epa.gov/cepp	o), submit your <b>Risk Management Pla</b> n	(RMP) to U.S. EPA Region III		
16. Regulatory Discussion. List all Federal and State air pollution control regulations that you believe are applicable to the				
proposed process (if known). A list of possible applicable requirements is also included in Attachment D of this application				
(Title V Permit Revision Information). Discuss applicability and proposed demonstration(s) of compliance (if known). Provide this				
information as Attachment D.				
Section II. Additional atta	chments and supporting do	cuments.		
<ol> <li>Include a check payable to WVDEP – Division of Air 0 45CSR13).</li> </ol>	Quality with the appropriate <b>application</b> t	fee (per 45CSR22 and		
<ol><li>Include a Table of Contents as the first page of your</li></ol>	application package.			
<ol> <li>Provide a Plot Plan, e.g. scaled map(s) and/or sketch source(s) is or is to be located as Attachment E (Ref</li> </ol>	h(es) showing the location of the property er to <i>Plot Plan Guidance</i> ).			
- Indicate the location of the nearest occupied structure (e.g. church, school, business, residence)				
<ol> <li>Provide a Detailed Process Flow Diagram(s) showing device as Attachment F.</li> </ol>	ng each proposed or modified emissions	unit, emission point and control		
3. Provide a Process Description as Attachment G.				
Also describe and quantify to the extent possible all  If of the required forms and additional to the extent possible all the required forms and additional to the required forms and additional to the extent possible all the required forms and additional to the extent possible all the required forms and additional to the extent possible all the required forms are additional to the extent possible all the required forms are additional to the extent possible all the required forms are additional to the extent possible all the required forms are additional to the extent possible and the required forms are additional to the extent possible and the required forms are additional to the extent possible and the required forms are additional to the required forms are additional to the extent possible and the required forms are additional to the required forms are additional to the extent possible and the required forms are additional to the extent possible and the required forms are additional to the extent possible and the required forms are additional to the extent possible and the required forms are additional to the extent possible and the required forms are additional to the extent possible and the required forms are additional to the extent possible and the required forms are additional to the extent possible and the required forms are additional to the extent possible and the required forms are additional to the extent possible and the	changes made to the facility since the la	ast permit review (if applicable)		
of the required forms and additional information can be fo	ound under the Permitting Section of DAQ	's website, or requested by phone.		
<ol> <li>Provide Material Safety Data Sheets (MSDS) for all r</li> </ol>	materials processed, used or produced a	s Attachment H.		
For chemical processes, provide a MSDS for each com	pound emitted to the air.			

25 Fill out the Fact of the				
25. Fill out the Emission Units Table and provide it as Attachment I.				
26. Fill out the Emission Points Data Summary Sheet (Table 1 and Table 2) and provide it as Attachment J.				
27. Fill out the Fugitive Emissions Data Summary Sheet and provide it as Attachment K.  28. Check all applicable Emissions Unit Data Sheets listed below:				
Bulk Liquid Transfer Operations				
☐ Chemical Processes	☐ Haul Road Emissions	☐ Quarry		
☐ Concrete Batch Plant	☐ Hot Mix Asphalt Plant	☐ Solid Materials Sizing, Handling and Storage Facilities		
Grey Iron and Steel Foundry	Incinerator	Storage Tanks		
General Emission Unit, specify Fugitives	☐ Indirect Heat Exchanger	Storage ranks		
and the second of the second o	,			
Fill out and provide the Emissions Unit Da	ta Sheet(s) as Attachment I			
29. Check all applicable Air Pollution Con	trol Device Sheets listed below			
☐ Absorption Systems	☐ Baghouse			
☐ Adsorption Systems	☐ Condenser	☑ Flare		
☐ Afterburner	☐ Electrostatic Precipitator	☐ Mechanical Collector		
Other Collectors, specify		Wet Collecting System		
Fill out and provide the Air Pollution Control	ol Device Sheet(s) as Attachme	ent M.		
30. Provide all Supporting Emissions Cald	culations as Attachment N, or a	attach the calculations directly to the forms listed in		
31. <b>Monitoring, Recordkeeping, Reporting and Testing Plans</b> . Attach proposed monitoring, recordkeeping, reporting and testing plans in order to demonstrate compliance with the proposed emissions limits and operating parameters in this permit application. Provide this information as <b>Attachment O</b> .				
Please be aware that all permits must be practically enforceable whether or not the applicant chooses to propose such measures. Additionally, the DAQ may not be able to accept all measures proposed by the applicant. If none of these plans are proposed by the applicant, DAQ will develop such plans and include them in the permit.				
32. Public Notice. At the time that the application is submitted, place a Class I Legal Advertisement in a newspaper of general				
circulation in the area where the source is or will be located (See 45CSR§13-8.3 through 45CSR§13-8.5 and <i>Example Legal Advertisement</i> for details). Places submit the Affile to 15 and				
Advertisement for details). Please submit the Affidavit of Publication as Attachment P immediately upon receipt.				
33. Business Confidentiality Claims. Does	s this application include confider	Otial information (per 45CS D24)		
33. Business Confidentiality Claims. Does this application include confidential information (per 45CSR31)?  YES NO				
If YES, identify each segment of information on each page that is submitted as confidential and provide justification for each segment claimed confidential, including the criteria under 45CSR§31-4.1, and in accordance with the DAQ's "Precautionary Notice – Claims of Confidentiality" guidance found in the General Instructions as Attachment Q.				
Section III. Certification of Information				
<ol> <li>Authority/Delegation of Authority. Only Check applicable Authority Form below:</li> </ol>	required when someone other	than the responsible official signs the application.		
Authority of Corporation or Other Business	Entity	pority of Dada and I		
Authority of Governmental Agency		nority of Partnership		
Submit completed and signed Authority Form	LI Autri Las Attachment P	nority of Limited Partnership		
All of the required forms and additional information can be found and				
Il of the required forms and additional information can be found under the Permitting Section of DAQ's website, or requested by phone.				

35A. Certification of Information. To cert 2.28) or Authorized Representative shall che	ify this permit application, a Responsible Or	fficial (per 45CSR§13-2.22 and 45CSR§30-		
Certification of Truth, Accuracy, and Completeness				
I, the undersigned Responsible Official / Authorized Representative, hereby certify that all information contained in this application and any supporting documents appended hereto, is true, accurate, and complete based on information and belief after stationary source described herein in accordance with this application and any amendments thereto, as well as the Department of and regulations of the West Virginia Division of Air Quality and W.Va. Code § 22-5-1 et seq. (State Air Pollution Control Act). If the notified in writing within 30 days of the official change.				
Compliance Certification  Except for requirements identified in the Title that, based on information and belief formed compliance with all applicable requirements.	V Application for which compliance is not a after reasonable inquiry, all air contaminant	chieved, I, the undersigned hereby certify sources identified in this application are in		
SIGNATURE		DATE: /////		
	use blue ink)	(Please use blue ink)		
35B. Printed name of signee: Tim Cummings		35C. Title: VP-Operations		
35D. E-mail: N/A	36E. Phone: N/A	36F. FAX: N/A		
36A. Printed name of contact person (if differe	nt from above): Evan Foster Pearson	36B. Title: EH&S Air Compliance Specialist		
36C. E-mail: evan.pearson@ascentresources.com	36D. Phone: 405-252-7753	36E. FAX: N/A		
PLEASE CHECK ALL APPLICABLE ATTACHMENTS INCLUDED WITH THIS PERMIT APPLICATION:  Attachment A: Business Certificate  Attachment B: Map(s)  Attachment C: Installation and Start Up Schedule  Attachment D: Regulatory Discussion  Attachment E: Plot Plan  Attachment E: Plot Plan  Attachment F: Detailed Process Flow Diagram(s)  Attachment G: Process Description  Attachment H: Material Safety Data Sheets (MSDS)  Attachment I: Emission Units Table  Attachment J: Emission Points Data Summary Sheet  Attachment A: Business Certificate  Attachment K: Fugitive Emissions Data Summary Sheet  Attachment K: Fugitive Emissions Data Summary Sheet  Attachment M: Attachment M: Air Pollution Control Device Sheet(s)  Attachment N: Supporting Emissions Calculations  Attachment O: Monitoring/Recordkeeping/Reporting/Testing Plans  Attachment P: Public Notice  Attachment Q: Business Confidential Claims  Attachment R: Authority Forms  Attachment S: Title V Permit Revision Information				
Please mail an original and three (3) copies of the complete permit application with the signature(s) to the DAQ, Permitting Section, at the address listed on the first page of this application. Please DO NOT fax permit applications.				
☐ For Title V Significant Modifications processed ☐ NSR permit writer should notify a Title \ ☐ Public notice should reference both 450 ☐ EPA has 45 day review period of a draft	Permitting Group and:  permit writer of draft permit,  priate notification to EPA and affected states opermit writer of draft permit.  in parallel with NSR Permit revision:  / permit writer of draft permit,  SR13 and Title V permits,  permit.			
All of the required forms and additional information	n can be found under the Permitting Section of	of DAQ's website, or requested by phone		
		, =		

All equipment at the WJ Criswell 405 facility (Facility) is owned and operated by Ascent Resources – Marcellus, LLC (Ascent) and has been included in this application.

Traditionally, source aggregation has been determined based on a "three-prong" approach, including:

- SIC Code: Surrounding or associated sources belong to the same 2-digit industrial grouping (2-digit SIC code) as this facility, OR surrounding or associated sources that belong to different 2-digit SIC codes are support facilities for this source.
- 2. <u>Common Ownership or Control</u>: Surrounding or associated sources are under common ownership or control as this source.
- 3. <u>Contiguous or Adjacent</u>: Surrounding or associated sources are contiguous or adjacent with this source.

On June 3, 2016, the United States Environmental Protection Agency (US EPA) finalized a rule clarifying oil and gas source aggregation at major sources. The final rule states that sources shall be aggregated if they are:

- 1. Under Common Control,
- 2. <u>Located within ¼ mile</u> of one another (measured from the center of the equipment on the surface site), and
- 3. <u>Share Equipment</u> (including, but not limited to, produced fluids storage tanks, phase separators, natural gas dehydrators or emissions control devices)

While states are not required to implement this definition, it provides additional reference in determining source aggregation.

Ascent has determined that there are currently no additional sources under the same SIC, under common control, contiguous or adjacent to this Facility, within a quarter (1/4) mile of the Facility, or that share equipment; therefore any additional source aggregation analysis is not required.

# Attachment A: Business Certificate



# I, Natalie E. Tennant, Secretary of State of the State of West Virginia, hereby certify that

the attached true and exact copy of the Articles of Amendment to the Articles of Organization of

### AMERICAN ENERGY-MARCELLUS, LLC

are filed in my office, signed and verified, as required by the provisions of West Virginia Code §31B-2-204 and conform to law. Therefore, I issue this

# CERTIFICATE OF AMENDMENT TO THE CERTIFICATE OF AUTHORITY

changing the name of the limited liability company to

ASCENT RESOURCES - MARCELLUS, LLC

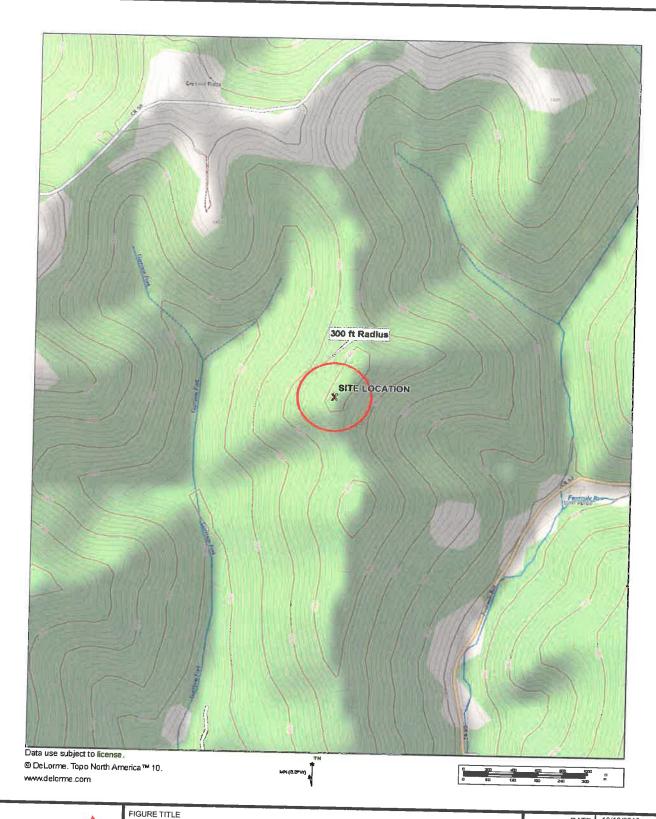


Given under my hand and the Great Seal of the State of West Virginia on this day of July 9, 2015

Vlateril E Jemie

Secretary of State

# Attachment B: Map(s)





1015 N. Broadway, Suite 300 Oklahoma City, OK 73102 (405) 842-1066

www.eccgrp.com

AREA MAP

DOCUMENT TITLE

RULE 13 CONSTRUCTION APPLICATION

CLIENT

ASCENT RESOURCES - MARCELLUS, LLC

LOCATION WJ CRISWELL 405 FACILITY
WETZEL COUNTY, WEST VIRGINA

DATE	10/18/2016	
SCALE	AS SHOWN	
DESIGNED BY	AD	
APPROVED BY	LWL	
DRAWN BY	AD	
PROJECT NUMBER		
ARMAWV0001		
ATTACHMENT		
В		

# Attachment C: Installation and Start-Up Schedule

# Installation and Start-up Schedule

Equipment	Unit ID	Installation Date	Startup Date
HiPower PSI/GM 3.0L Generator (47 Hp)	9E	2015	2015
Gas Production Unit (1.50 MMBtu/hr)	1E	2015	2015
Gas Production Unit (1.50 MMBtu/hr)	2E	2015	2015
Gas Production Unit (1.50 MMBtu/hr)	3E	2015	2015
Line Heater (1.50 MMBtu/hr)	4E	2015	2015
Flash Separator Heater (1.00 MMBtu/hr)	7E	2015	2015
Condensate Stabilizer Heater (0.75 MMBtu/hr)	11E	2015	2015
Condensate Storage Tank (400-bbl)	15E (CTK-1)	2015	2015
Condensate Storage Tank (400-bbl)	16E (CTK-2)	2015	2015
Condensate Storage Tank (400-bbl)	17E (CTK-3)	2015	2015
Produced Water Storage Tank (400-bbl)	18E (PTK-1)	2015	2015
Produced Water Storage Tank (400-bbl)	19E (PTK-2)	2015	2015
Produced Water Storage Tank (400-bbl)	20E (PTK-3)	2015	2015
Enclosed Combustor (18.42 MMBtu/hr)	10E	2015	2015
Condensate Truck Loading	12E	2015	2015
Produced Water Truck Loading	13E	2015	2015
Sitewide Fugitive	14E	2015	2015
Jnpaved Road Sources	21E	2015	2015

# Attachment D: Regulatory Discussion

## **Applicable State Requirements**

# 45CSR6 CONTROL OF AIR POLLUTION FROM COMBUSTION OF REFUSE

Ascent is applying for a permit to authorize the operation of the flare that will be used on site to control the storage tanks. Ascent will comply with all requirements of this rule.

45CSR13 PERMITS FOR CONSTRUCTION, MODIFICATION, RELOCATION AND OPERATION OF STATIONARY SOURCES OF AIR POLLUTANTS, NOTIFICATION REQUIREMENTS, ADMINISTRATIVE UPDATES, TEMPORARY PERMITS, GENERAL PERMITS, PERMISSION TO COMMENCE CONSTRUCTION, AND PROCEDURES FOR EVALUATION

Ascent is submitting this application in accordance with this rule. Ascent will comply will all requirements of this rule.

## **Applicable Federal Requirements**

40 CFR PART 60 NEW SOURCE PERFORMANCE STANDARDS (NSPS) SUBPART 0000/0000a

The storage tanks were constructed after August 23, 2011, however a federally enforceable limit of less than six (6) tons per year (TPY) was requested in the previous permits. Therefore, the storage tanks are not affected equipment under this subpart for the Facility. In addition, no other equipment or modifications at the Facility trigger NSPS Subpart OOOO or OOOOa at this time.

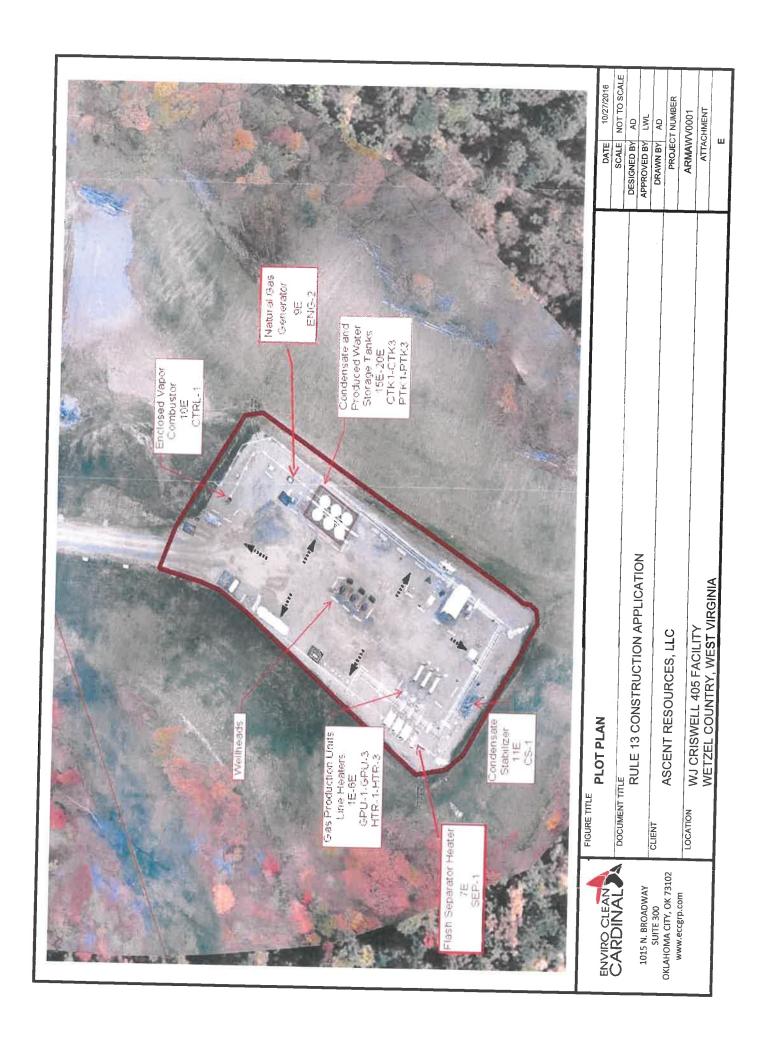
## 40 CFR PART 60 NSPS SUBPART JJJJ

The natural gas-fired generator (ENG-2), which is rated at 47 horsepower (Hp), was manufactured and constructed after July 1, 2008. Therefore, the Facility is subject to NSPS Subpart JJJJ and NESHAP Subpart ZZZZ. Specifically, ENG-2 is subject to the emission limitations of Table 3 of the preamble to the final rule for NSPS Subpart JJJJ as published in the Federal Register dated January 18, 2008. In accordance with the rule, Ascent will maintain documentation from the manufacturer that PUMP1 is certified to meet the applicable emission limitations.

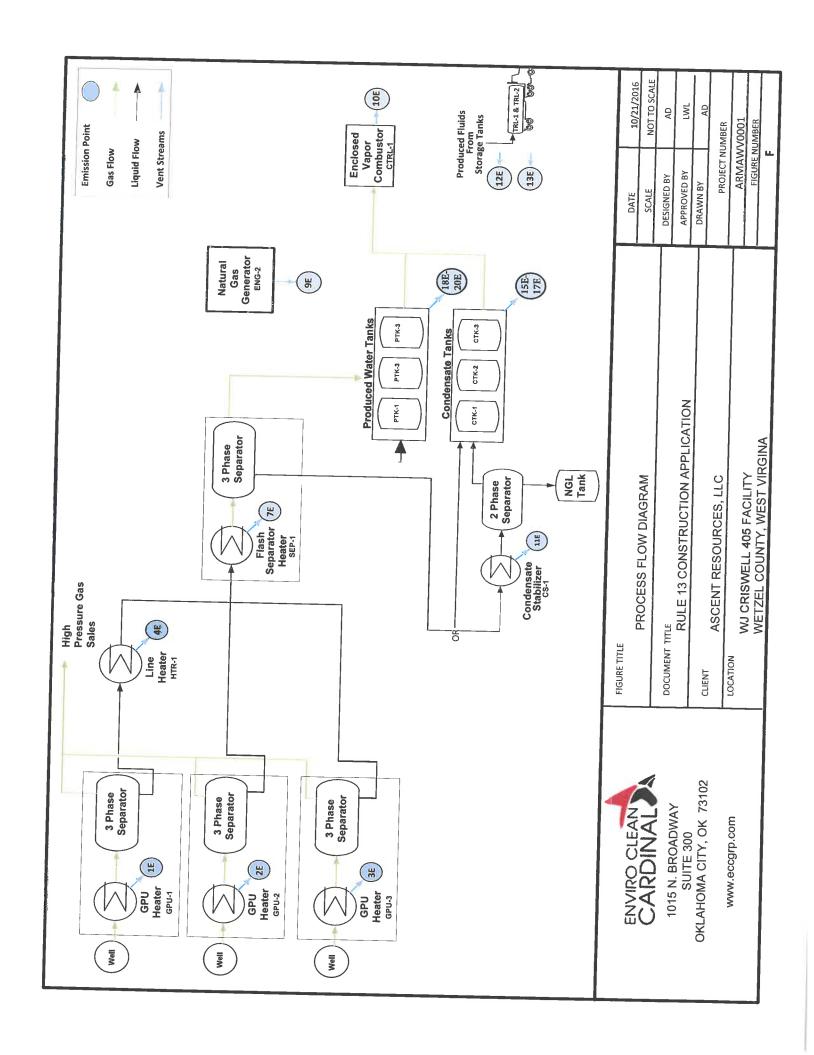
 $40~\mathrm{CFR}$  PART  $63~\mathrm{NATIONAL}$  EMISSION STANDARDS FOR HAZARDOUS AIR POLLUTANTS (NESHAP) SUBPART ZZZZ

NESHAP Subpart ZZZZ has no additional requirements for area sources. Ascent is complying with NESHAP Subpart ZZZZ by complying with NSPS Subpart JJJJ for ENG-2.

# Attachment E: Plot Plan



# Attachment F: Detailed Process Flow Diagram(s)



# **Attachment G: Process Description**

### **Process Description**

Natural gas, condensate, and produced water flow from the three (3) wellheads located on the WJ Criswell 405 Facility. In this application, Ascent is removing one (1) natural gas-fired compressor engine and updating production estimates at the Facility.

The inlet streams are first routed through the three (3) 1.5 million British thermal units per hour (MMBtu/hr) gas production units (GPUs) (GPU-1 to GPU-3) where the first stage of fluid separation occurs. The GPUs separate the well stream flow into a high pressure natural gas sales stream and condensate liquid stream. In the second stage of separation, the liquid streams are routed through three (3) 1.5 MMBtu/hr line heaters (HTR-1 to HTR-3) to aid in the downstream separation process.

The fluids are then routed to the 1.0 MMBtu/hr low pressure flash separator heater (SEP-1) where condensate and produced water are separated. The flash from the low pressure separator is sent to the storage tanks, which are controlled by an enclosed combustor (CTRL-1). Produced water from the flash separator is routed to three (3) 400-bbl produced water storage tanks (PTK-1 to PTK-3). The condensate from the flash separator is typically routed to the three (3) 400-bbl condensate storage tanks (CTK-1 to CTK-3).

The natural gas stream will exit the facility for transmission via pipeline. Condensate and produced water are transported offsite via tank truck (TRL-1 and TRL-2). Flashing, working, and breathing, emissions from the three (3) 400-bbl produced water storage tanks and three (3) 400-bbl condensate storage tanks will be routed to the enclosed combustion device (CTRL-1).

Ascent requests to maintain the permitted 1,200 bbl/day condensate stabilizer with a 0.75 MMBtu/hr burner assembly (CS-1). The condensate stabilizer raises the temperature of the condensate and drives off hydrocarbons. These hydrocarbons are then transferred under pressure to the natural gas liquids (NGL) tank on site. The depleted condensate stream is transferred to the three (3) 400-bbl condensate storage tanks.

Based upon current observed daily condensate production, Ascent does not expect the quantity of condensate production that would justify the operation of the condensate stabilizer. Ascent is filling this application to account for the loading of the condensate tank directly from the flash separator. At this time, Ascent requests that the condensate stabilizer remain an authorized emission source. With this permitting approach, Ascent is reasonably conservative in its permitting actions and has the authorization to operate the condensate stabilizer should field conditions deem it necessary.

One (1) 47 horsepower (Hp) Hipower prime-power natural gas generator (ENG-2) is located on-site for Facility electrical generation.

# Attachment H: Material Safety Data Sheets (MSDS)



## **Natural Gas Liquids**

Safety Data Sheet

# Section 1: Identification of the substance or mixture and of the supplier

**Product Name:** 

SDS Number:

Natural Gas Liquids

786340

Synonyms/Other Means of Identification:

Natural Gas Liquids, Raw

Natural Gas Liquids, Ethane Free

Plant Condensate

Raw NGL **EPBC Mix PBC Mix** Y-Grade Gas Liquids

**MARPOL Annex I Category:** 

Intended Use:

Naphthas and Condensates

Feedstock

Manufacturer:

Ascent Resources 3501 N.W. 63rd

Oklahoma City, OK 73116

**Emergency Health and Safety Number:** 

Chemtrec: 800-424-9300 (24 Hours)

SDS Information:

Phone: 800-642-3074

URL: www.ascentresources.com

## Section 2: Hazard(s) Identification

#### **Classification**

H224 -- Flammable liquids -- Category 1

H315 - Skin corrosion/irritation - Category 2

H304 - Aspiration Hazard - Category 1

H336 - Specific target organ toxicity (single exposure) - Category 3

H350 - Carcinogenicity - Category 1B

H411 - Hazardous to the aquatic environment, chronic toxicity - Category 2

#### Hazards not Otherwise Classified

May contain or release poisonous hydrogen sulfide gas

#### **Label Elements**









#### **DANGER**

Extremely flammable liquid and vapor. (H224)\*

Causes skin irritation. (H315)\*

May contain or release poisonous hydrogen sulfide gas May be fatal if swallowed and enters airways. (H304)\*

May cause drowsiness or dizziness. (H336)\*

May cause cancer. (H350)\*

Toxic to aquatic life with long lasting effects. (H411)\*

786340 - Natural Gas Liquids Date of Issue:1-Sep-2015

Page 1/11 Status: FINAL

Page 2/11 Status: FINAL

#### Precautionary Statement(s):

Obtain special instructions before use. (P201)\*

Do not handle until all safety precautions have been read and understood. (P202)\*

Keep away from heat/sparks/open flames/hot surfaces. - No smoking. (P210)\*

Keep container tightly closed. (P233)\*

Ground/bond container and receiving equipment. (P240)\*

Use with explosion-proof equipment. (P241)\*

Use only non-sparking tools. (P242)\*

Take precautionary measures against static discharge. (P243)\*

Avoid breathing dust/fume/gas/mist/vapours/spray. (P261)\*

Wash thoroughly after handling. (P264)\*

Use only outdoors or in a well-ventilated area. (P271)\*

Wear protective gloves / protective clothing / eye protection / face protection. (P280)\*

IF ON SKIN: Remove/Take off immediately all contaminated clothing. Rinse skin with water/shower. (P303+P361+P353)\*

In case of fire: Use dry chemical, carbon dioxide, or foam for extinction.(P370+P378)\*

If skin irritation occurs: Get medical advice/attention. (P313)\*

Take off contaminated clothing and wash before reuse. (P362)\*

IF SWALLOWED: Immediately call a POISON CENTER or doctor/physician. (P301+P310)\*

Do NOT induce vomiting. (P331)\*

IF INHALED: Remove victim to fresh air and keep at rest in a position comfortable for breathing. (P304+P340)\*

Call a POISON CENTER or doctor/physician if you feel unwell. (P312)\*

In case of fire: Use dry chemical, carbon dioxide, or foam for extinction.(P370+P378)\*

Store in a well-ventilated place. Keep cool (P403+P235)\*

Store locked up. (P405)\*

Dispose of contents/container to approved disposal facility. (P501)\*

# Section 3: Composition / Information on Ingredients

Component	CASRN	Concentration <sup>1</sup>
Natural gas (petroleum), raw liq. mix	64741-48-6	100
n-Hexane	110-54-3	5-25
Benzene	71-43-2	0.1-5
lydrogen Sulfide otal Sulfur: > 0.5 wt%	7783-06-4	<1

All concentrations are percent by weight unless ingredient is a gas. Gas concentrations are in percent by volume.

## Section 4: First Aid Measures

Eye Contact: If irritation or redness develops from exposure, flush eyes with clean water. If symptoms persist, seek medical attention.

Skin Contact: Remove contaminated shoes and clothing, and flush affected area(s) with large amounts of water. If skin surface is damaged, apply a clean dressing and seek medical attention. If skin surface is not damaged, cleanse affected area(s) thoroughly by washing with mild soap and water or a waterless hand cleaner. If irritation or redness develops, seek medical attention. Wash contaminated clothing before reuse.

Inhalation (Breathing): If respiratory symptoms or other symptoms of exposure develop, move victim away from source of exposure and into fresh air in a position comfortable for breathing. If symptoms persist, seek immediate medical attention. If victim is not breathing, clear airway and immediately begin artificial respiration. If breathing difficulties develop, oxygen should be administered by qualified personnel. Seek immediate medical attention.

Ingestion (Swallowing): Aspiration hazard: Do not induce vomiting or give anything by mouth because this material can enter the lungs and cause severe lung damage. If victim is drowsy or unconscious and vomiting, place on the left side with the head down. If possible, do not leave victim unattended and observe closely for adequacy of breathing. Seek medical attention.

<sup>\* (</sup>Applicable GHS hazard code.)

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Most important symptoms and effects

Acute: Headache, drowsiness, dizziness, loss of coordination, disorientation and fatigue.

Delayed: Dry skin and possible irritation with repeated or prolonged exposure.

Notes to Physician: At high concentrations hydrogen sulfide may produce pulmonary edema, respiratory depression, and/or respiratory paralysis. The first priority in treatment should be the establishment of adequate ventilation and the administration of 100% oxygen. Animal studies suggest that nitrites are a useful antidote, however, documentation of the efficacy of nitrites in humans is lacking. If the diagnosis of hydrogen sulfide poisoning is confirmed and if the patient does not respond rapidly to supportive care, the use of nitrites may be an effective antidote if delivered within the first few minutes of exposure. For adults the dose is 10 mL of a 3% NaNO2 solution (0.5 gm NaNO2 in 15 mL water) I.V. over 2-4 minutes. The dosage should be adjusted in children or in the presence of anemia, and methemoglobin levels, arterial blood gases, and electrolytes should be monitored

Epinephrine and other sympathomimetic drugs may initiate cardiac arrhythmias in persons exposed to high concentrations of hydrocarbon solvents (e.g., in enclosed spaces or with deliberate abuse). The use of other drugs with less arrhythmogenic potential should be considered. If sympathomimetic drugs are administered, observe for the development of cardiac arrhythmias.

Federal regulations (29 CFR 1910.1028) specify medical surveillance programs for certain exposures to benzene above the action level or PEL (specified in Section (i)(1)(i) of the Standard). In addition, employees exposed in an emergency situation shall, as described in Section (i)(4)(i), provide a urine sample at the end of the shift for measurement of urine phenol.

Other Comments: Before attempting rescue, first responders should be alert to the possible presence of hydrogen sulfide, a poisonous gas with the smell of rotten eggs, and should consider the need for respiratory protection (see Section 8). Remove casualty to fresh air as quickly as possible. Immediately begin artificial respiration if breathing has ceased. Consider whether oxygen administration is needed. Obtain medical advice for further treatment.

## Section 5: Fire-Fighting Measures



NFPA 704 Hazard Class

Health: 1 Flammability: 4 Instability: 0

(0-Minimal, 1-Slight, 2-Moderate, 3-Serious, 4-Severe)

Unusual Fire & Explosion Hazards: Extremely flammable. This material can be ignited by heat, sparks, flames, or other sources of ignition (e.g., static electricity, pilot lights, mechanical/electrical equipment, and electronic devices such as cell phones, computers, calculators, and pagers which have not been certified as intrinsically safe). Vapors may travel considerable distances to a source of ignition where they can ignite, flash back, or explode. May create vapor/air explosion hazard indoors, in confined spaces, outdoors, or in sewers. This product will float and can be reignited on surface water. Vapors are heavier than air and can accumulate in low areas. If container is not properly cooled, it can rupture in the heat of a fire. Hazardous combustion/decomposition products, including hydrogen sulfide, may be released by this material when exposed to heat or fire. Use caution and wear protective clothing, including respiratory protection.

**Extinguishing Media:** Dry chemical, carbon dioxide, or foam is recommended. Water spray is recommended to cool or protect exposed materials or structures. Carbon dioxide can displace oxygen. Use caution when applying carbon dioxide in confined spaces. Simultaneous use of foam and water on the same surface is to be avoided as water destroys the foam. Water may be ineffective for extinguishment, unless used under favorable conditions by experienced fire fighters.

**Fire Fighting Instructions:** For fires beyond the initial stage, emergency responders in the immediate hazard area should wear protective clothing. When the potential chemical hazard is unknown, in enclosed or confined spaces, a self contained breathing apparatus should be worn. In addition, wear other appropriate protective equipment as conditions warrant (see Section 8).

Isolate immediate hazard area and keep unauthorized personnel out. Stop spill/release if it can be done safely. Move undamaged containers from immediate hazard area if it can be done safely. Water spray may be useful in minimizing or dispersing vapors and to protect personnel. Cool equipment exposed to fire with water, if it can be done safely. Avoid spreading burning liquid with water used for cooling purposes.

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**Hazardous Combustion Products:** Combustion may yield smoke, carbon monoxide, and other products of incomplete combustion. Hydrogen sulfide and oxides of nitrogen and sulfur may also be formed.

See Section 9 for Flammable Properties including Flash Point and Flammable (Explosive) Limits

## Section 6: Accidental Release Measures

Personal Precautions: Extremely flammable. Spillages of liquid product will create a fire hazard and may form an explosive atmosphere. Keep all sources of ignition and hot metal surfaces away from spill/release if safe to do so. The use of explosion-proof electrical equipment is recommended. May contain or release poisonous hydrogen sulfide gas. If the presence of dangerous amounts of H2S around the spilled product is suspected, additional or special actions may be warranted, including access restrictions and use of protective equipment. Stay upwind and away from spill/release. Avoid direct contact with material. For large spillages, notify persons down wind of the spill/release, isolate immediate hazard area and keep unauthorized personnel out. Wear appropriate protective equipment, including respiratory protection, as conditions warrant (see Section 8). See Sections 2 and 7 for additional information on hazards and precautionary measures.

Environmental Precautions: Stop spill/release if it can be done safely. Prevent spilled material from entering sewers, storm drains, other unauthorized drainage systems, and natural waterways. Use foam on spills to minimize vapors. Use water sparingly to minimize environmental contamination and reduce disposal requirements. If spill occurs on water notify appropriate authorities and advise shipping of any hazard. Spills into or upon navigable waters, the contiguous zone, or adjoining shorelines that cause a sheen or discoloration on the surface of the water, may require notification of the National Response Center (phone number 800-424-8802).

Methods for Containment and Clean-Up: Notify relevant authorities in accordance with all applicable regulations. Immediate cleanup of any spill is recommended. Dike far ahead of spill for later recovery or disposal. Absorb spill with inert material such as sand or vermiculite, and place in suitable container for disposal. If spilled on water remove with appropriate methods (e.g. skimming, booms or absorbents). In case of soil contamination, remove contaminated soil for remediation or disposal, in accordance with local regulations.

Recommended measures are based on the most likely spillage scenarios for this material; however local conditions and regulations may influence or limit the choice of appropriate actions to be taken.

## Section 7: Handling and Storage

Precautions for safe handling: Keep away from ignition sources such as heat/sparks/open flame — No smoking. Take precautionary measures against static discharge. Nonsparking tools should be used. May contain or release dangerous levels of hydrogen sulfide. Obtain special instructions before use. Do not handle until all safety precautions have been read and understood. Avoid breathing vapors or mists. Use only outdoors or in well-ventilated area. Wear protective gloves/clothing and eye/face protection. Wash thoroughly after handling. Use good personal hygiene practices and wear appropriate personal protective equipment (see section 8).

Extremely Flammable. May vaporize easily at ambient temperatures. The vapor is heavier than air and may create an explosive mixture of vapor and air. Beware of accumulation in confined spaces and low lying areas. Open container slowly to relieve any pressure. Electrostatic charge may accumulate and create a hazardous condition when handling or processing this material. To avoid fire or explosion, dissipate static electricity during transfer by grounding and bonding containers and equipment before transferring material. The use of explosion-proof electrical equipment is recommended and may be required (see appropriate fire codes). Refer to NFPA-70 and/or API RP 2003 for specific bonding/grounding requirements. Do not enter confined spaces such as tanks or pits without following proper entry procedures such as ASTM D-4276 and 29CFR 1910.146. Do not wear contaminated clothing or shoes. Keep contaminated clothing away from sources of ignition such as sparks or open flames.

Static Accumulation Hazard: Electrostatic charge may accumulate and create a hazardous condition when handling this material. To minimize this hazard, bonding and grounding of tanks, transfer piping, and storage tank level floats are necessary but may not, by themselves, be sufficient. Review all operations which have the potential of generating and accumulating an electrostatic charge and/or a flammable atmosphere (including tank and container filling, splash filling, tank cleaning, sampling, gauging, switch loading, filtering, mixing, agitation, and vacuum truck operations) and use appropriate mitigating procedures. Special care should be given to ensure that special slow load procedures for "switch loading" are followed to avoid the static ignition hazard that can exist when higher flash point material (such as fuel oil or diesel) is loaded into tanks previously containing low flash point products (such as gasoline or naphtha). For more information, refer to OSHA Standard 29 CFR 1910.106, 'Flammable and Combustible Liquids', National Fire Protection Association (NFPA 77, 'Recommended Practice on Static Electricity', and/or the American Petroleum Institute (API) Recommended Practice 2003, 'Protection Against Ignitions Arising Out of Static, Lightning, and Stray Currents'.

meet OSHA standards and appropriate fire codes.

Conditions for safe storage: This material may contain or release poisonous hydrogen sulfide gas. In a tank, barge, or other closed container, the vapor space above this material may accumulate hazardous concentrations of hydrogen sulfide. Check atmosphere for oxygen content, H2S, and flammability prior to entry. Keep container(s) tightly closed and properly labeled. Use and store this material in cool, dry, well-ventilated areas away from heat, direct sunlight, hot metal surfaces, and all sources of ignition. Store only in approved containers. Post area "No Smoking or Open Flame." Keep away from any incompatible material (see Section 10). Protect container(s) against physical damage. Outdoor or detached storage is preferred. Indoor storage should

"Empty" containers retain residue and may be dangerous. Do not pressurize, cut, weld, braze, solder, drill, grind, or expose such containers to heat, flame, sparks, or other sources of ignition. They may explode and cause injury or death. "Empty" drums should be completely drained, properly bunged, and promptly shipped to the supplier or a drum reconditioner. All containers should be disposed of in an environmentally safe manner and in accordance with governmental regulations. Before working on or in tanks which contain or have contained this material, refer to OSHA regulations, ANSI Z49.1, and other references pertaining to cleaning, repairing, welding, or other contemplated operations.

## Section 8: Exposure Controls / Personal Protection

Component	ACGIH	OSHA	Other
Natural gas (petroleum), raw liq. mix	TWA: 300 ppm (as Gasoline)	TWA: 400 mg/m³ TWA: 100 ppm	0.5 ppm TWA8hr (as benzene) 0.25 ppm TWA12hr (as benzene) 2.5 ppm STEL (as benzene)
n-Hexane	TWA: 50 ppm Skin	TWA: 500 ppm TWA: 1800 mg/m³	(American Energy Guidelines
Benzene	STEL: 2.5 ppm TWA: 0.5 ppm Skin	Ceiling: 25 ppm STEL: 5 ppm TWA: 10 ppm TWA: 1 ppm	
-lydrogen Sulfide	STEL: 5 ppm TWA: 1 ppm	Ceiling: 20 ppm	TWA: 5 ppm 8hr TWA: 2.5 ppm 12hr STEL: 15 ppm (American Energy Guidelines)

Note: State, local or other agencies or advisory groups may have established more stringent limits. Consult an industrial hygienist or similar professional, or your local agencies, for further information.

Engineering controls: If current ventilation practices are not adequate to maintain airborne concentrations below the established exposure limits, additional engineering controls may be required.

Eye/Face Protection: The use of eye protection that meets or exceeds ANSI Z.87.1 is recommended to protect against potential eye contact, irritation, or injury. Depending on conditions of use, a face shield may be necessary.

Skin/Hand Protection: The use of gloves impervious to the specific material handled is advised to prevent skin contact. Users should check with manufacturers to confirm the breakthrough performance of their products. Depending on exposure and use conditions, additional protection may be necessary to prevent skin contact including use of items such as chemical resistant boots, aprons, arm covers, hoods, coveralls, or encapsulated suits. Suggested protective materials: Nitrile

Respiratory Protection: A NIOSH approved, self-contained breathing apparatus (SCBA) or equivalent operated in a pressure demand or other positive pressure mode should be used in situations of oxygen deficiency (oxygen content less than 19.5 percent), unknown exposure concentrations, or situations that are immediately dangerous to life or health (IDLH).

A respiratory protection program that meets or is equivalent to OSHA 29 CFR 1910.134 and ANSI Z88.2 should be followed whenever workplace conditions warrant a respirator's use.

If benzene concentrations equal or exceed applicable exposure limits, OSHA requirements for personal protective equipment, exposure monitoring, and training may apply (29CFR1910.1028 - Benzene).

Other Protective Equipment: Eye wash and quick-drench shower facilities should be available in the work area. Thoroughly clean shoes and wash contaminated clothing before reuse.

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Suggestions provided in this section for exposure control and specific types of protective equipment are based on readily available information. Users should consult with the specific manufacturer to confirm the performance of their protective equipment. Specific situations may require consultation with industrial hygiene, safety, or engineering professionals.

## Section 9: Physical and Chemical Properties

Note: Unless otherwise stated, values are determined at 20°C (68°F) and 760 mm Hg (1 atm). Data represent typical values and are not intended to be specifications.

Appearance:

**Physical Form:** 

Odor:

**Odor Threshold:** 

pH:

Vapor Pressure:

Vapor Density (air=1):

Initial Boiling Point/Range: Melting/Freezing Point:

Solubility in Water:

Partition Coefficient (n-octanol/water) (Kow):

Specific Gravity (water=1):

Percent Volatile:

Evaporation Rate (nBuAc=1):

Flash Point:

**Test Method:** 

Lower Explosive Limits (vol % in air): Upper Explosive Limits (vol % in air):

Auto-ignition Temperature:

Colorless

Liquid

Gasoline; Rotten egg / sulfurous

No data

Not applicable

150 - 200 psia (Reid VP) @ 100°F / 37.8°C

No data No data

Negligible

No data

(estimated) 0.5 - 0.7 @ 68°F / 20°C

100%

No data

< -99 °F / < -73 °C

(estimate)

No data

No data No data

## Section 10: Stability and Reactivity

Stability: Stable under normal ambient and anticipated conditions of use.

Conditions to Avoid: Avoid high temperatures and all sources of ignition. Prevent vapor accumulation.

Materials to Avoid (Incompatible Materials): Avoid contact with strong oxidizing agents and strong reducing agents.

Hazardous Decomposition Products: Not anticipated under normal conditions of use.

Hazardous Polymerization: Not known to occur.

## Section 11: Toxicological Information

Information on Toxicological Effects of Substance/Mixture

Hazard	Additional Information	LCEON DEC D
Expected to have a low degree of toxicity by inhalation	May contain or release poisonous hydrogen sulfide gas - see Other Comments.	> 5.2 mg/L (vapor)
Unlikely to be harmful		> 2 g/kg
Unlikely to be harmful		> 5 g/kg
	Expected to have a low degree of toxicity by inhalation  Unlikely to be harmful	Expected to have a low degree of toxicity by inhalation  May contain or release poisonous hydrogen sulfide gas - see Other Comments.  Unlikely to be harmful

Aspiration Hazard: May be fatal if swallowed and enters airways.

Skin Corrosion/Irritation: Causes skin irritation. Repeated exposure may cause skin dryness or cracking.

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Serious Eye Damage/Irritation: Causes mild eye irritation. .

Signs and Symptoms: Effects of overexposure can include slight irritation of the respiratory tract, nausea, vomiting, and signs of nervous system depression (e.g., headache, drowsiness, dizziness, loss of coordination, disorientation and fatigue). Continued exposure to high concentrations can result in vomiting, cardiac irregularities and sudden loss of consciousness.

Skin Sensitization: Not expected to be a skin sensitizer.

Respiratory Sensitization: No information available.

Specific Target Organ Toxicity (Single Exposure): May cause drowsiness and dizziness.

Specific Target Organ Toxicity (Repeated Exposure): Not expected to cause organ effects from repeated exposure.

Carcinogenicity: May cause cancer Based on component information.

Germ Cell Mutagenicity: Not expected to cause heritable genetic effects.

Reproductive Toxicity: Not expected to cause reproductive toxicity.

Other Comments: This material may contain or liberate hydrogen sulfide, a poisonous gas with the smell of rotten eggs. The smell disappears rapidly because of olfactory fatigue so odor may not be a reliable indicator of exposure. Effects of overexposure include irritation of the eyes, nose, throat and respiratory tract, blurred vision, photophobia (sensitivity to light), and pulmonary edema (fluid accumulation in the lungs). Severe exposures can result in nausea, vomiting, muscle weakness or cramps, headache, disorientation and other signs of nervous system depression, irregular heartbeats, convulsions, respiratory failure, and death.

## Information on Toxicological Effects of Components

## Natural gas (petroleum), raw lig. mix

Carcinogenicity: Two year inhalation studies of vaporized unleaded gasoline produced an increased incidence of kidney tumors in male rats and liver tumors in female mice. Repeated skin application of various petroleum naphthas in mice for two years resulted in an increased incidence of skin tumors but only in the presence of severe skin irritation. Follow-up mechanistic studies suggest that the occurrence of these tumors may be the consequence of promotional processes and not relevant to human risk assessment. Epidemiology data collected from a study of more than 18,000 petroleum marketing and distribution workers showed no increased risk of leukemia, multiple myeloma, or kidney cancer from gasoline exposure. Unleaded gasoline has been identified as a possible carcinogen by the International Agency for Research on Cancer.

Target Organs: Two year inhalation studies of wholly vaporized unleaded gasoline, and 90 days studies of various petroleum naphthas, did not produce significant target organ toxicity in laboratory animals. Nephropathy in male rats, characterized by the accumulation of alpha-2-u- globulin in epithelial cells of the proximal tubules was observed, however follow-up studies suggest that these changes are unique to the male rat.

Reproductive Toxicity: No evidence of developmental toxicity was found in pregnant laboratory animals (rats and mice) exposed to high vapor concentrations of unleaded gasoline and petroleum naphthas via inhalation. A two-generation reproductive toxicity study of vapor recovery gasoline did not adversely affect reproductive function or offspring survival and development.

#### n-Hexane

Target Organs: Excessive exposure to n-hexane can result in peripheral neuropathies. The initial symptoms are symmetrical sensory numbness and paresthesias of distal portions of the extremities. Motor weakness is typically observed in muscles of the toes and fingers but may also involve muscles of the arms, thighs and forearms. The onset of these symptoms may be delayed for several months to a year after the beginning of exposure. The neurotoxic properties of n-hexane are potentiated by exposure to methyl ethyl ketone and methyl isobutyl ketone.

Reproductive Toxicity: Prolonged exposure to high concentrations of n-hexane (>1,000 ppm) resulted in decreased sperm count and degenerative changes in the testes of rats but not those of mice.

Benzene

Carcinogenicity: Benzene is an animal carcinogen and is known to produce acute myelogenous leukemia (a form of cancer) in humans. Benzene has been identified as a human carcinogen by IARC, the US National Toxicology Program and the US-Occupational Safety and Health Administration.

Target Organs: Prolonged or repeated exposures to benzene vapors can cause damage to the blood and blood forming organs, including disorders like leukopenia, thrombocytopenia, and aplastic anemia.

Reproductive Toxicity: Some studies in occupationally exposed women have suggested benzene exposure increased risk of miscarriage and stillbirth and decreased birth weight and gestational age. The size of the effects detected in these studies was small, and ascertainment of exposure and outcome in some cases relied on self-reports, which may limit the reliability of these results.

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Germ Cell Mutagenicity: Benzene exposure has resulted in chromosomal aberrations in human lymphocytes and animal bone marrow cells. Exposure has also been associated with chromosomal aberrations in sperm cells in human and animal studies.

#### <u>Toluene</u>

Carcinogenicity: Exposure of rats and mice to toluene at concentrations ranging from 120-1200 ppm for two years did not demonstrate evidence of carcinogenicity. Toluene has not been listed as a carcinogen by IARC.

Target Organs: Epidemiology studies suggest that chronic occupational overexposure to toluene may damage color vision. Subchronic and chronic inhalation studies with toluene produced kidney and liver damage, hearing loss and central nervous system (brain) damage in laboratory animals. Intentional misuse by deliberate inhalation of high concentrations of toluene has been shown to cause liver, kidney, and central nervous system damage, including hearing loss and visual disturbances. Reproductive Toxicity: Exposure to toluene during pregnancy has demonstrated limited evidence of developmental toxicity in laboratory animals. Decreased fetal body weight and increased skeletal variations in both inhalation and oral studies, but only at doses that were maternally toxic. No fetal toxicity was seen at doses that were not maternally toxic. Decreased sperm counts have been observed in male rats in the absence of a reduction in fertility. Toluene has been reported to cause mental or growth retardation in the children of solvent abusers who directly inhale toluene during pregnancy. Cyclohexane

Reproductive Toxicity: Two-generation reproduction and developmental toxicity studies using rats and rabbits exposed (whole-body) to atmospheric concentrations up to 7000 ppm cyclohexane did not detect evidence of developmental toxicity in either species.

## Section 12: Ecological Information

Toxicity: Acute aquatic toxicity studies on samples of gasoline and naphtha streams show acute toxicity values greater than 1 mg/L and mostly in the range 1-100 mg/L. These tests were carried out on water accommodated fractions, in closed systems to prevent evaporative loss. Results are consistent with the predicted aquatic toxicity of these substances based on their hydrocarbon composition. These substances should be regarded as toxic to aquatic organisms, with the potential to cause long term adverse effects in the aquatic environment. Classification: H411; Chronic Cat 2.

Persistence and Degradability: The hydrocarbons in this material are not readily biodegradable but are regarded as inherently biodegradable since their hydrocarbon components can be degraded by microorganisms.

Persistence per IOPC Fund definition: Non-Persistent

Bioaccumulative Potential: Log Kow values measured for the hydrocarbon components of this material range from 3 to greater than 6 and therefore are regarded as having the potential to bioaccumulate. In practice, metabolic processes or physical properties may prevent this effect or limit bioavailability.

Mobility in Soil: On release to water, hydrocarbons will float on the surface and since they are sparingly soluble, the only significant loss is volatilization to air. In air, these hydrocarbons are photodegraded by reaction with hydroxyl radicals with half lives varying from 6.5 days for benzene to 0.5 days for n-dodecane.

Other Adverse Effects: None anticipated.

# Section 13: Disposal Considerations

The generator of a waste is always responsible for making proper hazardous waste determinations and needs to consider state and local requirements in addition to federal regulations.

This material, if discarded as produced, would not be a federally regulated RCRA "listed" hazardous waste. However, it would likely be identified as a federally regulated RCRA hazardous waste for the following characteristic(s) shown below. See Sections 7 and 8 for information on handling, storage and personal protection and Section 9 for physical/chemical properties. It is possible that the material as produced contains constituents which are not required to be listed in the MSDS but could affect the hazardous waste determination. Additionally, use which results in chemical or physical change of this material could subject it to regulation as a hazardous waste.

Container contents should be completely used and containers should be emptied prior to discard. Container residues and rinseates could be considered to be hazardous wastes.

#### **EPA Waste Number(s)**

- D001 Ignitability characteristic
- D018 Toxicity characteristic (Benzene)

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## Section 14: Transport Information

U.S. Department of Transportation (DOT)

**Shipping Description:** If vapor pressure is > 300 kPa (43.5 psia) at 50° C (122° F) shipping description is:

UN1965, Hydrocarbon gas mixture, liquefied, n.o.s., 2.1;

If vapor pressure is <= 300 kPa (43.5 psia) at 50° C (122° F) shipping description is: UN3295, Hydrocarbons, liquid, n.o.s., 3, I or II [I if BP < 95°  $\dot{F}$  (35° C), II if BP > 95°  $\dot{F}$ 

Non-Bulk Package Marking: Must be consistent with shipping description, either:

Hydrocarbon gas mixture, liquefied, n.o.s., UN1965

or

Hydrocarbons, liquid, n.o.s., UN3295

Non-Bulk Package Labeling: For UN1965: Flammable gas

For UN3295: Flammable liquid

**Bulk Package/Placard Marking:** For UN1965: Flammable gas / 1965

For UN3295: Flammable / 3295

Packaging - References: For UN1965: 49 CFR: 173.306; 173.304; 173.314 & .315

For UN3295: 49 CFR 173.150; 173.201; 173.243 [ PG I ]

-or-

49 CFR 173.150; 173.202; 173.242 [ PG II ]

(Exceptions; Non-bulk; Bulk)

Hazardous Substance:

**Emergency Response Guide:** 

Note:

See Section 15 for RQ's UN1965 - 115; UN3295 - 128:

The following alternate shipping description order may be used until January 1,

Proper Shipping name, Hazard Class or Division, (Subsidiary Hazard if any), UN or

NA number, Packing Group

Transport in bulk according to Annex II of MARPOL 73/78 and the IBC Code: Not

applicable

Other shipping description elements may be required for DOT compliance.

International Maritime Dangerous Goods (IMDG)

Shipping Description: If boiling point is < 20° C shipping description is:

UN1965, Hydrocarbon gas mixture, liquefied, n.o.s., ( Propane , Butane ), 2.1 If vapor pressure is <= 300 kPa (43.5 psia) at 50° C (122° F) shipping description is: UN3295, Hydrocarbons, liquid, n.o.s., 3, I or II (FP° C cc), [where FP is the material's flash

point in degrees C cc.]

[ I if BP < 95° F (35° C); II if BP > 95° F];

Non-Bulk Package Marking: Must be consistent with shipping description, either:

Hydrocarbon gas mixture, liquefied, n.o.s., (Propane, Butane), UN1965

or

Hydrocarbons, liquid, n.o.s., UN3295

Labels: For UN1965: Flammable gas

For UN3295: Flammable liquid

Placards/Marking (Bulk): For UN1965: Flammable gas / 1965

For UN3295: Flammable / 3295

Packaging - Non-Bulk: For UN1965: P200

For UN3295: P001

EMS: For UN1965: F-D, S-U

For UN3295: F-E, S-D

Note: If transported in bulk by marine vessel in international waters, product is being

carried under the scope of MARPOL Annex I.

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# International Civil Aviation Org. / International Air Transport Assoc. (ICAO/IATA)

UN/ID #:

UN1965 or UN3295

**Proper Shipping Name:** 

For UN1965: Hydrocarbon gas mixture, liquefied, n.o.s. (Propane, Butane)

For UN3295: Hydrocarbons, liquid, n.o.s.

Hazard Class/Division:

For UN1965: 2.1 For UN3295: 3

Subsidiary risk:

None

**Packing Group:** 

For UN1965: None

For UN3295: | or || [ Determined by IATA 3.3.2 ]

Non-Bulk Package Marking:

For UN1965: Hydrocarbon gas mixture, liquefied, n.o.s. (Propane, Butane), UN1965

For UN3295: Hydrocarbons, liquid, n.o.s., UN3295

Labels:

For UN1965: Flammable gas , Cargo Aircraft Only

For UN3295: Flammable liquid

**ERG Code:** 

For UN1965: 10L or For UN3295: 3H

Prokoning Instanting II	LTD. QTY	Passenger Aircraft	Cargo Aircraft Only
Packaging Instruction #:	UN1965 - Forbidden UN3295 - Forbidden - [PG I] Y341 - [PG II]	UN1965 - Forbidden UN3295 - 351 - [ PG I ] 353 - [ PG II ]	UN1965 - 200
Max. Net Qty. Per Package:	UN3295 - Forbidden - [ PG I ] 1L - [ PG II ]	UN3295 - 1L - [PG I] 5 L - [PG II]	<i>UN1965 -</i> 150 kg <i>UN3295 -</i> 30 L - <i>[ PG I ]</i> 60 L - <i>[ PG II ]</i>

## Section 15: Regulatory Information

# CERCLA/SARA - Section 302 Extremely Hazardous Substances and TPQs (in pounds):

This material contains the following chemicals subject to the reporting requirements of SARA 302 and 40 CFR 372:

Component	TPQ	EPCRA RQ
Hydrogen Sulfide	500 lb	
	00010	100 lb

## CERCLA/SARA - Section 311/312 (Title III Hazard Categories)

Acute Health:

Yes

**Chronic Health:** 

Yes

Fire Hazard:

Yes

Pressure Hazard:

No

Reactive Hazard:

No

## CERCLA/SARA - Section 313 and 40 CFR 372:

This material contains the following chemicals subject to the reporting requirements of Section 313 of SARA Title III and 40 CFR 372:

Component	Concentration <sup>1</sup>	de minimis
n-Hexane	5-25	1.0%
Toluene	1-5	
Benzene	0.1-5	1.0%
Cyclohexane		0.1%
Systemoranic	0-3	1.0%

## EPA (CERCLA) Reportable Quantity (in pounds):

EPA's Petroleum Exclusion applies to this material - (CERCLA 101(14)).

#### California Proposition 65:

Warning: This material may contain detectable quantities of the following chemicals, known to the State of California to cause cancer, birth defects or other reproductive harm, and which may be subject to the warning requirements of California Proposition 65 (CA Health & Safety Code Section 25249.5):

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Component	Type of Toxicity	
Toluene	Developmental Toxicant	
	Female Reproductive Toxicant	
Benzene	Cancer	
	Developmental Toxicant	
ernational Hazard Classification	Male Reproductive Toxicant	

#### International Hazard Classification

#### Canada:

This product has been classified in accordance with the hazard criteria of the Controlled Products Regulations (CPR) and the MSDS contains all the information required by the Regulations.

#### WHMIS Hazard Class:

B2 - Flammable Liquids

D2A

D<sub>2</sub>B

#### **National Chemical Inventories**

All components are either listed on the US TSCA Inventory, or are not regulated under TSCA All components are either on the DSL, or are exempt from DSL listing requirements

U.S. Export Control Classification Number: EAR99

#### Section 16: Other Information

Date of Issue:

SDS Number:

Status:

**Previous Issue Date:** 

Revised Sections or Basis for Revision:

1-Sep-2015

FINAL 1-Sep-2015

Identified Hazards (Section 2)

Precautionary Statement(s) (Section 2)

First Aid (Section 4)Exposure limits (Section 8)

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Shipping information (Section 14)

Regulatory information (Section 15)

786340

#### **Guide to Abbreviations:**

ACGIH = American Conference of Governmental Industrial Hygienists; CASRN = Chemical Abstracts Service Registry Number; CEILING = Ceiling Limit (15 minutes); CERCLA = The Comprehensive Environmental Response, Compensation, and Liability Act; EPA = Environmental Protection Agency; GHS = Globally Harmonized System; IARC = International Agency for Research on Cancer; INSHT = National Institute for Health and Safety at Work; IOPC = International Oil Pollution Compensation; LEL = Lower Explosive Limit; NE = Not Established; NFPA = National Fire Protection Association; NTP = National Toxicology Program; OSHA = Occupational Safety and Health Administration; PEL = Permissible Exposure Limit (OSHA); SARA = Superfund Amendments and Reauthorization Act; STEL = Short Term Exposure Limit (15 minutes); TLV = Threshold Limit Value (ACGIH); TWA = Time Weighted Average (8 hours); UEL = Upper Explosive Limit; WHMIS = Worker Hazardous Materials Information

#### Disclaimer of Expressed and implied Warranties:

The information presented in this Material Safety Data Sheet is based on data believed to be accurate as of the date this Material Safety Data Sheet was prepared. HOWEVER, NO WARRANTY OF MERCHANTABILITY, FITNESS FOR ANY PARTICULAR PURPOSE, OR ANY OTHER WARRANTY IS EXPRESSED OR IS TO BE IMPLIED REGARDING THE ACCURACY OR COMPLETENESS OF THE INFORMATION PROVIDED ABOVE, THE RESULTS TO BE OBTAINED FROM THE USE OF THIS INFORMATION OR THE PRODUCT, THE SAFETY OF THIS PRODUCT, OR THE HAZARDS RELATED TO ITS USE. No responsibility is assumed for any damage or injury resulting from abnormal use or from any failure to adhere to recommended practices. The information provided above, and the product, are furnished on the condition that the person receiving them shall make their own determination as to the suitability of the product for their particular purpose and on the condition that they assume the risk of their use. In addition, no authorization is given nor implied to practice any patented invention without a license.



## **Crude Condensate**

Safety Data Sheet

# Section 1: Identification of the substance or mixture and of the supplier

**Product Name:** 

**SDS Number:** 

Crude Condensate

730370

Synonyms/Other Means of Identification:

Natural Gas Condensates, Petroleum

Crude Oil Condensate

Gas Drips

MARPOL Annex I Category:

Intended Use:

Naphthas and Condensates

Feedstock

Manufacturer:

Ascent Resources 3501 N.W. 63rd

Oklahoma City, OK 73116

**Emergency Health and Safety Number:** 

Chemtrec: 800-424-9300 (24 Hours)

**SDS Information:** 

Phone: 800-642-3074

URL: www.ascent resources.com

## Section 2: Hazard(s) Identification

#### Classification

H224 -- Flammable liquids -- Category 1

H304 -- Aspiration Hazard -- Category 1

H315 -- Skin corrosion/irritation -- Category 2

H332 -- Acute toxicity, Inhalation -- Category 4

H336 -- Specific target organ toxicity (single exposure) -- Category 3

H350 -- Carcinogenicity -- Category 1B

H411 -- Hazardous to the aquatic environment, chronic toxicity -- Category 2

#### Hazards not Otherwise Classified

May contain or release poisonous hydrogen sulfide gas

#### Label Elements









#### **DANGER**

Extremely flammable liquid and vapor. (H224)\*
Causes skin irritation. (H315)\*
May be fatal if swallowed and enters airways. (H304)\*
Contains poisonous hydrogen sulfide gas
Harmful if inhaled. (H332)\*
May cause drowsiness or dizziness. (H336)\*
May cause cancer. (H350)\*

Toxic to aquatic life with long lasting effects. (H411)\*

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Precautionary Statement(s):

Obtain special instructions before use. (P201)\*

Do not handle until all safety precautions have been read and understood. (P202)\*

Keep away from heat/sparks/open flames/hot surfaces. - No smoking. (P210)\*

Keep container tightly closed. (P233)\*

Keep cool. (P235)\*

Ground/bond container and receiving equipment. (P240)\*

Use with explosion-proof equipment. (P241)\*

Use only non-sparking tools. (P242)\*

Take precautionary measures against static discharge. (P243)\*

Avoid breathing dust/fume/gas/mist/vapours/spray. (P261)\*

Wash thoroughly after handling. (P264)\*

Use only outdoors or in a well-ventilated area. (P271)\*

Avoid release to the environment. (P273)\*

Wear protective gloves / protective clothing / eye protection / face protection. (P280)\*

IF ON SKIN: Remove/Take off immediately all contaminated clothing. (P361)\* Wash with plenty of soap and water. (P352)\*

If skin irritation occurs: Get medical advice/attention. (P313)\*

Take off contaminated clothing and wash before reuse. (P362)\*

IF INHALED: Remove victim to fresh air and keep at rest in a position comfortable for breathing. (P340)\*

Call a POISON CENTER or doctor/physician if you feel unwell. (P312)\*

IF SWALLOWED: Immediately call a POISON CENTER or doctor/physician. (P301+P310)\*

Do NOT induce vomiting. (P331)\*

In case of fire: Use dry chemical, carbon dioxide, or foam for extinction.(P370+P378)\*

Collect spillage. (P391)\*

Store locked up. (P405)\*

Store in a well-ventilated place. Keep container tightly closed. (P403+P233)\*

Dispose of contents/container to approved disposal facility. (P501)\*

# Section 3: Composition / Information on Ingredients

Component	CASRN	Concentration <sup>1</sup>
Natural Gas CondensateC2-20	64741-47-5	100
oluene	108-88-3	1-7
Hydrogen Sulfide	7783-06-4	0.1-5
Benzene All concentrations are percent by weight upless issued in the	71-43-2	<5

All concentrations are percent by weight unless ingredient is a gas. Gas concentrations are in percent by volume.

Crude oil, natural gas and natural gas condensate can contain minor amounts of sulfur, nitrogen and oxygen containing organic compounds as well as trace amounts of heavy metals like mercury, arsenic, nickel, and vanadium. Composition can vary depending on the source of crude.

#### Section 4: First Aid Measures

Eye Contact: If irritation or redness develops from exposure, flush eyes with clean water. If symptoms persist, seek medical attention.

Skin Contact: Remove contaminated shoes and clothing, and flush affected area(s) with large amounts of water. If skin surface is damaged, apply a clean dressing and seek medical attention. If skin surface is not damaged, cleanse affected area(s) thoroughly by washing with mild soap and water or a waterless hand cleaner. If irritation or redness develops, seek medical attention. Wash contaminated clothing before reuse.

Inhalation (Breathing): Immediately move victim away from exposure and into fresh air in a position comfortable for breathing. If respiratory symptoms or other symptoms of exposure develop, seek immediate medical attention. If victim is not breathing, clear airway and immediately begin artificial respiration. If breathing difficulties develop, oxygen should be administered by qualified personnel. Seek immediate medical attention.

<sup>\* (</sup>Applicable GHS hazard code.)

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**Ingestion (Swallowing):** Aspiration hazard: Do not induce vomiting or give anything by mouth because this material can enter the lungs and cause severe lung damage. If victim is drowsy or unconscious and vomiting, place on the left side with the head down. If possible, do not leave victim unattended and observe closely for adequacy of breathing. Seek medical attention.

Most important symptoms and effects

Acute: Headache, drowsiness, dizziness, loss of coordination, disorientation and fatigue.

Delayed: Dry skin and possible irritation with repeated or prolonged exposure.

**Notes to Physician:** At high concentrations hydrogen sulfide may produce pulmonary edema, respiratory depression, and/or respiratory paralysis. The first priority in treatment should be the establishment of adequate ventilation and the administration of 100% oxygen. Animal studies suggest that nitrites are a useful antidote, however, documentation of the efficacy of nitrites in humans is lacking. If the diagnosis of hydrogen sulfide poisoning is confirmed and if the patient does not respond rapidly to supportive care, the use of nitrites may be an effective antidote if delivered within the first few minutes of exposure. For adults the dose is 10 mL of a 3% NaNO2 solution (0.5 gm NaNO2 in 15 mL water) I.V. over 2-4 minutes. The dosage should be adjusted in children or in the presence of anemia, and methemoglobin levels, arterial blood gases, and electrolytes should be monitored

Epinephrine and other sympathomimetic drugs may initiate cardiac arrhythmias in persons exposed to high concentrations of hydrocarbon solvents (e.g., in enclosed spaces or with deliberate abuse). The use of other drugs with less arrhythmogenic potential should be considered. If sympathomimetic drugs are administered, observe for the development of cardiac arrhythmias.

Federal regulations (29 CFR 1910.1028) specify medical surveillance programs for certain exposures to benzene above the action level or PEL (specified in Section (i)(1)(i) of the Standard). In addition, employees exposed in an emergency situation shall, as described in Section (i)(4)(i), provide a urine sample at the end of the shift for measurement of urine phenol.

Other Comments: Before attempting rescue, first responders should be alert to the possible presence of hydrogen sulfide, a poisonous gas with the smell of rotten eggs, and should consider the need for respiratory protection (see Section 8). Remove casualty to fresh air as quickly as possible. Immediately begin artificial respiration if breathing has ceased. Consider whether oxygen administration is needed. Obtain medical advice for further treatment.

## Section 5: Fire-Fighting Measures



#### NFPA 704 Hazard Class

Health: 2 Flammability: 4 I

Instability: 0

(0-Minimal, 1-Slight, 2-Moderate, 3-Serious, 4-Severe)

Unusual Fire & Explosion Hazards: Extremely flammable. This material can be ignited by heat, sparks, flames, or other sources of ignition (e.g., static electricity, pilot lights, mechanical/electrical equipment, and electronic devices such as cell phones, computers, calculators, and pagers which have not been certified as intrinsically safe). Vapors may travel considerable distances to a source of ignition where they can ignite, flash back, or explode. May create vapor/air explosion hazard indoors, in confined spaces, outdoors, or in sewers. This product will float and can be reignited on surface water. Vapors are heavier than air and can accumulate in low areas. If container is not properly cooled, it can rupture in the heat of a fire. Hazardous combustion/decomposition products, including hydrogen sulfide, may be released by this material when exposed to heat or fire. Use caution and wear protective clothing, including respiratory protection.

**Extinguishing Media:** Dry chemical, carbon dioxide, or foam is recommended. Water spray is recommended to cool or protect exposed materials or structures. Carbon dioxide can displace oxygen. Use caution when applying carbon dioxide in confined spaces. Simultaneous use of foam and water on the same surface is to be avoided as water destroys the foam. Water may be ineffective for extinguishment, unless used under favorable conditions by experienced fire fighters.

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**Fire Fighting Instructions:** For fires beyond the initial stage, emergency responders in the immediate hazard area should wear protective clothing. When the potential chemical hazard is unknown, in enclosed or confined spaces, a self contained breathing apparatus should be worn. In addition, wear other appropriate protective equipment as conditions warrant (see Section 8).

Isolate immediate hazard area and keep unauthorized personnel out. Stop spill/release if it can be done safely. Move undamaged containers from immediate hazard area if it can be done safely. Water spray may be useful in minimizing or dispersing vapors and to protect personnel. Cool equipment exposed to fire with water, if it can be done safely. Avoid spreading burning liquid with water used for cooling purposes.

**Hazardous Combustion Products:** Combustion may yield smoke, carbon monoxide, and other products of incomplete combustion. Hydrogen sulfide and oxides of nitrogen and sulfur may also be formed.

See Section 9 for Flammable Properties including Flash Point and Flammable (Explosive) Limits

# Section 6: Accidental Release Measures

Personal Precautions: Extremely flammable. Spillages of liquid product will create a fire hazard and may form an explosive atmosphere. Keep all sources of ignition and hot metal surfaces away from spill/release if safe to do so. The use of explosion-proof electrical equipment is recommended. Contains poisonous hydrogen sulfide gas. If the presence of dangerous amounts of H2S around the spilled product is suspected, additional or special actions may be warranted, including access restrictions and use of protective equipment. Stay upwind and away from spill/release. Avoid direct contact with material. For large spillages, notify persons down wind of the spill/release, isolate immediate hazard area and keep unauthorized personnel out. Wear appropriate protective equipment, including respiratory protection, as conditions warrant (see Section 8). See Sections 2 and 7 for additional information on hazards and precautionary measures.

**Environmental Precautions:** Stop spill/release if it can be done safely. Prevent spilled material from entering sewers, storm drains, other unauthorized drainage systems, and natural waterways. Use foam on spills to minimize vapors. Use water sparingly to minimize environmental contamination and reduce disposal requirements. If spill occurs on water notify appropriate authorities and advise shipping of any hazard. Spills into or upon navigable waters, the contiguous zone, or adjoining shorelines that cause a sheen or discoloration on the surface of the water, may require notification of the National Response Center (phone number 800-424-8802).

**Methods for Containment and Clean-Up:** Notify relevant authorities in accordance with all applicable regulations. Immediate cleanup of any spill is recommended. Dike far ahead of spill for later recovery or disposal. Absorb spill with inert material such as sand or vermiculite, and place in suitable container for disposal. If spilled on water remove with appropriate methods (e.g. skimming, booms or absorbents). In case of soil contamination, remove contaminated soil for remediation or disposal, in accordance with local regulations.

Recommended measures are based on the most likely spillage scenarios for this material; however local conditions and regulations may influence or limit the choice of appropriate actions to be taken.

# Section 7: Handling and Storage

**Precautions for safe handling:** Keep away from ignition sources such as heat/sparks/open flame – No smoking. Take precautionary measures against static discharge. Nonsparking tools should be used. Do not handle until all safety precautions have been read and understood. Obtain special instructions before use. Wear protective gloves/clothing and eye/face protection. May contain or release dangerous levels of hydrogen sulfide. Use only outdoors or in well-ventilated area. Avoid breathing vapors or mists. Wash thoroughly after handling. Use good personal hygiene practices and wear appropriate personal protective equipment (see section 8).

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Extremely Flammable. May vaporize easily at ambient temperatures. The vapor is heavier than air and may create an explosive mixture of vapor and air. Beware of accumulation in confined spaces and low lying areas. Open container slowly to relieve any pressure. Electrostatic charge may accumulate and create a hazardous condition when handling or processing this material. To avoid fire or explosion, dissipate static electricity during transfer by grounding and bonding containers and equipment before transferring material. The use of explosion-proof electrical equipment is recommended and may be required (see appropriate fire codes). Refer to NFPA-70 and/or API RP 2003 for specific bonding/grounding requirements. Do not enter confined spaces such as tanks or pits without following proper entry procedures such as ASTM D-4276 and 29CFR 1910.146. Do not wear contaminated clothing or shoes. Keep contaminated clothing away from sources of ignition such as sparks or open flames.

Mercury and other heavy metals may be present in trace quantities in crude oil, raw natural gas, and condensates. Production and processing of these materials can lead to "drop-out" of elemental mercury in enclosed vessels and pipe work, typically at the low point of any process equipment because of its density. Mercury may also occur in other process system deposits such as sludges, sands, scales, waxes, and filter media. Personnel engaged in work with equipment where mercury deposits might occur (confined space entry, sampling, opening drain valves, draining process lines, etc), may be exposed to a mercury hazard (see sections 3 and 8).

Static Accumulation Hazard: Electrostatic charge may accumulate and create a hazardous condition when handling this material. To minimize this hazard, bonding and grounding of tanks, transfer piping, and storage tank level floats are necessary but may not, by themselves, be sufficient. Review all operations which have the potential of generating and accumulating an electrostatic charge and/or a flammable atmosphere (including tank and container filling, splash filling, tank cleaning, sampling, gauging, switch loading, filtering, mixing, agitation, and vacuum truck operations) and use appropriate mitigating procedures. Special care should be given to ensure that special slow load procedures for "switch loading" are followed to avoid the static ignition hazard that can exist when higher flash point material (such as fuel oil or diesel) is loaded into tanks previously containing low flash point products (such as gasoline or naphtha). For more information, refer to OSHA Standard 29 CFR 1910.106, 'Flammable and Combustible Liquids', National Fire Protection Association (NFPA 77, 'Recommended Practice on Static Electricity', and/or the American Petroleum Institute (API) Recommended Practice 2003, 'Protection Against Ignitions Arising Out of Static, Lightning, and Stray Currents'.

Conditions for safe storage: This material may contain or release poisonous hydrogen sulfide gas. In a tank, barge, or other closed container, the vapor space above this material may accumulate hazardous concentrations of hydrogen sulfide. Check atmosphere for oxygen content, H2S, and flammability prior to entry. Keep container(s) tightly closed and properly labeled. Use and store this material in cool, dry, well-ventilated areas away from heat, direct sunlight, hot metal surfaces, and all sources of ignition. Store only in approved containers. Post area "No Smoking or Open Flame." Keep away from any incompatible material (see Section 10). Protect container(s) against physical damage. Outdoor or detached storage is preferred. Indoor storage should meet OSHA standards and appropriate fire codes.

"Empty" containers retain residue and may be dangerous. Do not pressurize, cut, weld, braze, solder, drill, grind, or expose such containers to heat, flame, sparks, or other sources of ignition. They may explode and cause injury or death. "Empty" drums should be completely drained, properly bunged, and promptly shipped to the supplier or a drum reconditioner. All containers should be disposed of in an environmentally safe manner and in accordance with governmental regulations. Before working on or in tanks which contain or have contained this material, refer to OSHA regulations, ANSI Z49.1, and other references pertaining to cleaning, repairing, welding, or other contemplated operations.

# Section 8: Exposure Controls / Personal Protection

ACGIH	OSHA	Other
TWA: 300 ppm (as Gasoline)	TWA: 400 mg/m³ TWA: 100 ppm	0.5 ppm TWA8hr (as benzene) 0.25 ppm TWA12hr (as benzene) 2.5 ppm STEL (as benzene)
TWA: 20 ppm	Ceiling: 300 ppm	(American Energy Guidelines
STEL: 5 ppm TWA: 1 ppm	Ceiling: 20 ppm	TWA: 5 ppm 8hr TWA: 2.5 ppm 12hr STEL: 15 ppm (American Energy Guidelines)
STEL: 2.5 ppm TWA: 0.5 ppm	Ceiling: 25 ppm STEL: 5 ppm	
	TWA: 300 ppm (as Gasoline)  TWA: 20 ppm  STEL: 5 ppm TWA: 1 ppm	TWA: 300 ppm (as Gasoline)  TWA: 400 mg/m³ TWA: 100 ppm  TWA: 20 ppm  Ceiling: 300 ppm TWA: 200 ppm  Ceiling: 20 ppm  TWA: 1 ppm  STEL: 5 ppm TWA: 1 ppm  Ceiling: 25 ppm

Note: State, local or other agencies or advisory groups may have established more stringent limits. Consult an industrial hygienist or similar professional, or your local agencies, for further information.

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**Engineering controls:** If current ventilation practices are not adequate to maintain airborne concentrations below the established exposure limits, additional engineering controls may be required.

**Eye/Face Protection:** The use of eye protection that meets or exceeds ANSI Z.87.1 is recommended to protect against potential eye contact, irritation, or injury. Depending on conditions of use, a face shield may be necessary.

**Skin/Hand Protection:** The use of gloves impervious to the specific material handled is advised to prevent skin contact. Users should check with manufacturers to confirm the breakthrough performance of their products. Depending on exposure and use conditions, additional protection may be necessary to prevent skin contact including use of items such as chemical resistant boots, aprons, arm covers, hoods, coveralls, or encapsulated suits. Suggested protective materials: Nitrile

**Respiratory Protection:** A NIOSH approved, self-contained breathing apparatus (SCBA) or equivalent operated in a pressure demand or other positive pressure mode should be used in situations of oxygen deficiency (oxygen content less than 19.5 percent), unknown exposure concentrations, or situations that are immediately dangerous to life or health (IDLH).

A respiratory protection program that meets or is equivalent to OSHA 29 CFR 1910.134 and ANSI Z88.2 should be followed whenever workplace conditions warrant a respirator's use.

If benzene concentrations equal or exceed applicable exposure limits, OSHA requirements for personal protective equipment, exposure monitoring, and training may apply (29CFR1910.1028 - Benzene).

Workplace monitoring plans should consider the possibility that heavy metals such as mercury may concentrate in processing vessels and equipment presenting the possibility of exposure during various sampling and maintenance operations. Implement appropriate respiratory protection and the use of other protective equipment as dictated by monitoring results (See Sections 2 and 7).

**Other Protective Equipment:** Eye wash and quick-drench shower facilities should be available in the work area. Thoroughly clean shoes and wash contaminated clothing before reuse.

Suggestions provided in this section for exposure control and specific types of protective equipment are based on readily available information. Users should consult with the specific manufacturer to confirm the performance of their protective equipment. Specific situations may require consultation with industrial hygiene, safety, or engineering professionals.

# Section 9: Physical and Chemical Properties

**Note:** Unless otherwise stated, values are determined at 20°C (68°F) and 760 mm Hg (1 atm). Data represent typical values and are not intended to be specifications.

Appearance: Amber to dark brown **Physical Form:** Liquid Odor: Rotten egg / sulfurous; Petroleum. **Odor Threshold:** No data pH: Not applicable Vapor Pressure: 5-15 psia (Reid VP) @ 100°F / 37.8°C Vapor Density (air=1): Initial Boiling Point/Range: -20 to 800 °F / -29 to 427 °C Melting/Freezing Point: No data Solubility in Water: Negligible Partition Coefficient (n-octanol/water) (Kow): No data Specific Gravity (water=1): 0.6 - 0.8 @ 60°F (15.6°C) **Bulk Density:** 6.25 lbs/gal VOC Content(%): 50 Evaporation Rate (nBuAc=1): Flash Point: -51 °F / -46 °C **Test Method:** Pensky-Martens Closed Cup (PMCC), ASTM D93, EPA 1010 Lower Explosive Limits (vol % in air): 1.1 Upper Explosive Limits (vol % in air): 6.0 **Auto-ignition Temperature:** 590 °F / 310 °C

# Section 10: Stability and Reactivity

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Stability: Stable under normal ambient and anticipated conditions of use.

Conditions to Avoid: Avoid high temperatures and all sources of ignition. Prevent vapor accumulation.

Materials to Avoid (Incompatible Materials): Avoid contact with strong oxidizing agents and strong reducing agents.

Hazardous Decomposition Products: Not anticipated under normal conditions of use.

Hazardous Polymerization: Not known to occur.

# Section 11: Toxicological Information

# Information on Toxicological Effects of Substance/Mixture

Hazard Harmful if inhaled	Additional Information Contains poisonous hydrogen sulfide gas. See Signs and Symptoms.	LC50/LD50 Data 10 mg/L (vapor, estimated)
Unlikely to be harmful		> 2 g/kg
Unlikely to be harmful		> 5 g/kg
	Harmful if inhaled Unlikely to be harmful	Harmful if inhaled  Contains poisonous hydrogen sulfide gas. See Signs and Symptoms.  Unlikely to be harmful

Aspiration Hazard: May be fatal if swallowed and enters airways.

Skin Corrosion/Irritation: Causes skin irritation. Repeated exposure may cause skin dryness or cracking.

Serious Eye Damage/Irritation: Causes mild eye irritation. .

**Signs and Symptoms:** Effects of overexposure can include slight irritation of the respiratory tract, nausea, vomiting, and signs of nervous system depression (e.g., headache, drowsiness, dizziness, loss of coordination, disorientation and fatigue). Continued exposure to high concentrations can result in vomiting, cardiac irregularities and sudden loss of consciousness.

This material contains hydrogen sulfide, a poisonous gas with the smell of rotten eggs. The smell disappears rapidly because of olfactory fatigue so odor may not be a reliable indicator of exposure. Effects of overexposure include irritation of the eyes, nose, throat and respiratory tract, blurred vision, photophobia (sensitivity to light), and pulmonary edema (fluid accumulation in the lungs). Severe exposures can result in nausea, vomiting, muscle weakness or cramps, headache, disorientation and other signs of nervous system depression, irregular heartbeats, convulsions, respiratory failure, and death.

Skin Sensitization: Not expected to be a skin sensitizer.

Respiratory Sensitization: No information available.

Specific Target Organ Toxicity (Single Exposure): May cause drowsiness and dizziness.

Specific Target Organ Toxicity (Repeated Exposure): Not expected to cause organ effects from repeated exposure.

Carcinogenicity: May cause cancer

Germ Cell Mutagenicity: Not expected to cause heritable genetic effects.

Reproductive Toxicity: Not expected to cause reproductive toxicity.

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# Information on Toxicological Effects of Components

## Natural Gas Condensate .. C2-20

Carcinogenicity: Two year inhalation studies of vaporized unleaded gasoline produced an increased incidence of kidney tumors in male rats and liver tumors in female mice. Repeated skin application of various petroleum naphthas in mice for two years resulted in an increased incidence of skin tumors but only in the presence of severe skin irritation. Follow-up mechanistic studies suggest that the occurrence of these tumors may be the consequence of promotional processes and not relevant to human risk assessment. Epidemiology data collected from a study of more than 18,000 petroleum marketing and distribution workers showed no increased risk of leukemia, multiple myeloma, or kidney cancer from gasoline exposure. Unleaded gasoline has been identified as a possible carcinogen by the International Agency for Research on Cancer.

Target Organs: Two year inhalation studies of wholly vaporized unleaded gasoline, and 90 days studies of various petroleum naphthas, did not produce significant target organ toxicity in laboratory animals. Nephropathy in male rats, characterized by the accumulation of alpha-2-u- globulin in epithelial cells of the proximal tubules was observed, however follow-up studies suggest that these changes are unique to the male rat.

Reproductive Toxicity: No evidence of developmental toxicity was found in pregnant laboratory animals (rats and mice) exposed to high vapor concentrations of unleaded gasoline and petroleum naphthas via inhalation. A two-generation reproductive toxicity study of vapor recovery gasoline did not adversely affect reproductive function or offspring survival and development.

#### **Xylenes**

Target Organs: Rats exposed to xylenes at 800, 1000 or 1200 ppm 14 hours daily for 6 weeks demonstrated high frequency hearing loss. Another study in rats exposed to 1800 ppm 8 hours daily for 5 days demonstrated middle frequency hearing loss. Reproductive Toxicity: Both mixed xylenes and the individual isomers produced limited evidence of developmental toxicity in laboratory animals. Inhalation and oral administration of xylene resulted in decreased fetal weight, increased incidences of delayed ossification, skeletal variations and resorptions, but no evidence of teratogenicity. Toluene

Carcinogenicity: Exposure of rats and mice to toluene at concentrations ranging from 120-1200 ppm for two years did not demonstrate evidence of carcinogenicity. Toluene has not been listed as a carcinogen by IARC.

Target Organs: Epidemiology studies suggest that chronic occupational overexposure to toluene may damage color vision. Subchronic and chronic inhalation studies with toluene produced kidney and liver damage, hearing loss and central nervous system (brain) damage in laboratory animals. Intentional misuse by deliberate inhalation of high concentrations of toluene has been shown to cause liver, kidney, and central nervous system damage, including hearing loss and visual disturbances. Reproductive Toxicity: Exposure to toluene during pregnancy has demonstrated limited evidence of developmental toxicity in laboratory animals. Decreased fetal body weight and increased skeletal variations in both inhalation and oral studies, but only at doses that were maternally toxic. No fetal toxicity was seen at doses that were not maternally toxic. Decreased sperm counts have been observed in male rats in the absence of a reduction in fertility. Toluene has been reported to cause mental or growth retardation in the children of solvent abusers who directly inhale toluene during pregnancy. Cyclohexane

Reproductive Toxicity: Two-generation reproduction and developmental toxicity studies using rats and rabbits exposed (whole-body) to atmospheric concentrations up to 7000 ppm cyclohexane did not detect evidence of developmental toxicity in either species.

#### **Benzene**

Carcinogenicity: Benzene is an animal carcinogen and is known to produce acute myelogenous leukemia (a form of cancer) in humans. Benzene has been identified as a human carcinogen by IARC, the US National Toxicology Program and the US-Occupational Safety and Health Administration.

Target Organs: Prolonged or repeated exposures to benzene vapors can cause damage to the blood and blood forming organs, including disorders like leukopenia, thrombocytopenia, and aplastic anemia.

Reproductive Toxicity: Some studies in occupationally exposed women have suggested benzene exposure increased risk of miscarriage and stillbirth and decreased birth weight and gestational age. The size of the effects detected in these studies was small, and ascertainment of exposure and outcome in some cases relied on self-reports, which may limit the reliability of these

Germ Cell Mutagenicity: Benzene exposure has resulted in chromosomal aberrations in human lymphocytes and animal bone marrow cells. Exposure has also been associated with chromosomal aberrations in sperm cells in human and animal studies.

#### n-Hexane

Target Organs: Excessive exposure to n-hexane can result in peripheral neuropathies. The initial symptoms are symmetrical sensory numbness and paresthesias of distal portions of the extremities. Motor weakness is typically observed in muscles of the toes and fingers but may also involve muscles of the arms, thighs and forearms. The onset of these symptoms may be delayed for several months to a year after the beginning of exposure. The neurotoxic properties of n-hexane are potentiated by exposure to methyl ethyl ketone and methyl isobutyl ketone.

Reproductive Toxicity: Prolonged exposure to high concentrations of n-hexane (>1,000 ppm) resulted in decreased sperm count and degenerative changes in the testes of rats but not those of mice.

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#### Ethyl Benzene

Carcinogenicity: Rats and mice exposed to 0, 75, 250, or 750 ppm ethyl benzene in a two year inhalation study demonstrated limited evidence of kidney, liver, and lung cancer. Ethyl benzene has been listed as a possible human carcinogen by IARC.

Target Organs: In rats and mice exposed to 0, 75, 250, or 750 ppm ethyl benzene in a two year inhalation study there was mild damage to the kidney (tubular hyperplasia), liver (eosinophilio foci, hypertrophy, necrosis), lung (alveolar epithelium metaplasia), thyroid (hyperplasia), thyroid (hyperplasia) and pituitary (hyperplasia). In animal models (particularly rats), ethyl benzene affects the auditory function mainly in the cochlear mid-frequency range and ototoxicity was observed after combined exposure to noise and ethyl benzene. There is no evidence of either ethyl benzene-induced hearing losses or ototoxicity with combined exposure to ethyl benzene and noise in workers.

# Section 12: Ecological Information

**Toxicity:** Acute aquatic toxicity studies on samples of gasoline and naphtha streams show acute toxicity values greater than 1 mg/L and mostly in the range 1-100 mg/L. These tests were carried out on water accommodated fractions, in closed systems to prevent evaporative loss. Results are consistent with the predicted aquatic toxicity of these substances based on their hydrocarbon composition. These substances should be regarded as toxic to aquatic organisms, with the potential to cause long term adverse effects in the aquatic environment. Classification: H411: Chronic Cat 2.

**Persistence and Degradability:** The hydrocarbons in this material are not readily biodegradable but are regarded as inherently biodegradable since their hydrocarbon components can be degraded by microorganisms.

**Bioaccumulative Potential:** Log Kow values measured for the hydrocarbon components of this material range from 3 to greater than 6 and therefore are regarded as having the potential to bioaccumulate. In practice, metabolic processes or physical properties may prevent this effect or limit bioavailability.

**Mobility in Soil:** On release to water, hydrocarbons will float on the surface and since they are sparingly soluble, the only significant loss is volatilization to air. In air, these hydrocarbons are photodegraded by reaction with hydroxyl radicals with half lives varying from 6.5 days for benzene to 0.5 days for n-dodecane.

Other Adverse Effects: None anticipated.

# Section 13: Disposal Considerations

The generator of a waste is always responsible for making proper hazardous waste determinations and needs to consider state and local requirements in addition to federal regulations.

This material, if discarded as produced, would not be a federally regulated RCRA "listed" hazardous waste. However, it would likely be identified as a federally regulated RCRA hazardous waste for the following characteristic(s) shown below. See Sections 7 and 8 for information on handling, storage and personal protection and Section 9 for physical/chemical properties. It is possible that the material as produced contains constituents which are not required to be listed in the MSDS but could affect the hazardous waste determination. Additionally, use which results in chemical or physical change of this material could subject it to regulation as a hazardous waste.

Container contents should be completely used and containers should be emptied prior to discard. Container residues and rinseates could be considered to be hazardous wastes.

#### **EPA Waste Number(s)**

- · D001 Ignitability characteristic
- D018 Toxicity characteristic (Benzene)

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# Section 14: Transport Information

U.S. Department of Transportation (DOT)

**Shipping Description:** 

If vapor pressure is > 300 kPa (43.5 psia) at 50° C (122° F) and H2S is > 8.8 molar %

shipping description is:

UN3160, Liquefied gas, toxic, flammable, n.o.s., ( Hydrogen sulfide; ,; Liquefied

Petroleum Gas ), 2.3,, , (2.1), Inhalation Hazard Zone X

If vapor pressure is > 300 kPa (43.5 psia) at 50° C (122° F) and H2S is < 8.8 molar %

shipping description is:

UN1965, Hydrocarbon gas mixture, liquefied, n.o.s., 2.1

If vapor pressure is <= 300 kPa (43.5 psia) at 50° C (122° F) and H2S is < 8.8 molar %

shipping description is:

UN1267, Petroleum crude oil, 3, I or II [ I if BP < 35° C (95° F); II if BP > 35° C]

Non-Bulk Package Marking:

Must be consistent with shipping description, either:

Liquefied gas, toxic, flammable, n.o.s., (Hydrogen sulfide, Liquefied petroleum gas),

UN3160 or

Hydrocarbon gas mixture, liquefied, n.o.s., UN1965

Petroleum crude oil, UN1267

Non-Bulk Package Labeling:

For UN3160: Poison gas and Flammable gas

For UN1965: Flammable gas For UN1267: Flammable liquid

**Bulk Package/Placard Marking:** 

For UN3160: Poison gas / 3160 and Flammable gas

For UN1965: Flammable gas / 1965 For UN1267: Flammable / 1267

Packaging - References:

For UN3160: None; 49 CFR 173.304; 173.314 & .315 For UN1965: 49 CFR: 173.306; 173.304; 173.314 & .315 For UN1267: 49 CFR 173.150; 173.201; 173.243 [ PG I ] -or-

49 CFR 173.150; 173.202; 173.242 [ PG II ]

(Exceptions; Non-bulk; Bulk)

**Hazardous Substance:** 

The EPA's Petroleum Exclusion applies to Section 2 and/or 15 components which are listed

in 49 CFR 172.101, Table 1 to Appendix A. UN3160 - 119; UN1965 - 115; UN1267 - 128;

**Emergency Response Guide:** Note:

Replace X in shipping description with: D if Molar % H2S is from 8.8% to 14.8% C if Molar % H2S is from 14.9% to 44.4% **B** if Molar % H2S is from 44.5% to 100.0%

Container(s) greater than 5 liters (liquids) or 5 kilograms (solids), shipped by water mode and ALL bulk shipments may require the shipping description to contain the "Marine Pollutant" notation [49 CFR 172.203(I)] and the container(s) to display the

[Marine Pollutant Mark] [49 CFR 172.322].

The following alternate shipping description order may be used until January 1,

2013:

Proper Shipping name, Hazard Class or Division, (Subsidiary Hazard if any), UN or

NA number, Packing Group

Other shipping description elements may be required for DOT compliance. Transport in bulk according to Annex II of MARPOL 73/78 and the IBC Code: Not

International Maritime Dangerous Goods (IMDG)

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**Shipping Description:** If vapor pressure is > 300 kPa (43.5 psia) at 50° C (122° F) and H2S is > 8.8 molar %

shipping description is:

UN3160, Liquefied gas, toxic, flammable, n.o.s ( Hydrogen sulphide , Liquefied Petroleum

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Gas ), 2.3,; , (2.1)

If vapor pressure is > 300 kPa (43.5 psia) at 50° C (122° F) and H2S is < 8.8 molar %

shipping description is:

UN1965, Hydrocarbon gas mixture, liquefied, n.o.s., (Hydrogen sulphide, Liquefied

petroleum gas), 2.1;

If vapor pressure is <= 300 kPa (43.5 psia) at 50° C (122° F) and H2S is < 8.8 molar %

shipping description is:

UN1267, Petroleum crude oil, 3, I *or* II [ I if IBP < 35° C (95° F); II if IBP > 35° C] (-46° C);

Non-Bulk Package Marking: Must be consistent with shipping description, either:

Liquefied gas, toxic, flammable, n.o.s., (Hydrogen sulphide, Liquefied petroleum gas),

UN3160 or

Hydrocarbon gas mixture, liquefied, n.o.s., (Hydrogen sulphide, Liquefied petroleum gas),

UN1965

Petroleum crude oil, UN1267

Labels: For UN3160: Toxic gas and Flammable gas

For UN1965: Flammable gas For UN1267: Flammable liquid

Placards/Marking (Bulk): For UN3160: Toxic gas / 3160 and Flammable gas

For UN1965: Flammable gas / 1965 For UN1267: Flammable / 1267

Packaging - Non-Bulk: For UN3160 & UN1965: P200

For UN1267: P001

EMS: For UN3160 & UN1965: F-D, S-U

For UN1267: F-E. S-E

Note: If container(s) is greater than 5 liters (liquids) or 5 kilograms (solids), shipment may

require the shipping description to contain the "Marine Pollutant" description [IMDG 5.4.1.4.3.5] and the container(s) to display the Marine Pollutant mark [IMDG 5.2.1.6]. U.S. DOT compliance requirements may apply. See 49 CFR 171.22, 23 & 25. If transported in bulk by marine vessel in international waters, product is being carried

under the scope of MARPOL Annex I.

International Civil Aviation Org. / International Air Transport Assoc. (ICAO/IATA)

UN/ID #:

UN3160 - Forbidden UN1965 or UN1267

**Proper Shipping Name:** 

For UN1965: Hydrocarbon gas mixture, liquefied, n.o.s. (Liquefied petroleum gas,

Hydrogen sulphide)

For UN1267: Petroleum crude oil

Hazard Class/Division:

For UN1965: 2.1 For UN1267: 3

Subsidiary risk:

None

Packing Group:

For UN1965: None

For UN1267: | or || [ Determined by IATA 3.3.2 ]

Non-Bulk Package Marking:

For UN1965: Hydrocarbon gas mixture, liquefied, n.o.s. (Liquefied petroleum gas,

Hydrogen sulphide), UN1965

For UN1267: Petroleum crude oil, UN1267

Labels:

For UN1965: Flammable gas , Cargo Aircraft Only

For UN1267: Flammable liquid

**ERG Code:** 

For UN1965: 10L or For UN1267: 3L

LTD. QTY

Passenger Aircraft

Cargo Aircraft Only

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UN1965 - Forbidden	UN1965 - Forbidden	UN1965 - 200
1		
	UN1207 - 351 - [PG1]	UN1267 - 361 - [PGI]
[ PG I ]	353 - <b>[ PG    1</b>	364 - <b>[ PG    1</b>
Y341 - I PG II 1		004 [1011]
<i>UN1267 -</i> None (PG I);	UN1267 - 1L - [PG]]	<b>UN1965 -</b> 150 kg
12 (1 0 11)	JL-[PGII]	UN1267 - 30 L - [PG I]
		60 L - [ PG    1
	UN1965 - Forbidden UN1267 - Forbidden - [ PG   ] Y341 - [ PG     ] UN1267 - None (PG   I); 1L (PG   II)	UN1267 - Forbidden - [PG I] Y341 - [PG II] UN1267 - None (PG I); UN1267 - 1L - [PG I]

# Section 15: Regulatory Information

CERCLA/SARA - Section 302 Extremely Hazardous Substances and TPQs (in pounds):

This material contains the following chemicals subject to the reporting requirements of SARA 302 and 40 CFR 372:

Component	TPQ	EPCRA RQ
Hydrogen Sulfide	500 lb	
	300 10	100 lb

# CERCLA/SARA - Section 311/312 (Title III Hazard Categories)

Acute Health:

Yes

**Chronic Health:** 

Yes

Fire Hazard: Pressure Hazard:

Yes No

Reactive Hazard:

No

# CERCLA/SARA - Section 313 and 40 CFR 372:

This material contains the following chemicals subject to the reporting requirements of Section 313 of SARA Title III and 40 CFR 372:

Component	Concentration <sup>1</sup>	de minimis
Xylenes	1-8	1.0%
Toluene	1-7	1.0%
Cyclohexane	1-5	
Benzene	<5	1.0%
n-Hexane	2-4	0.1%
Ethyl Benzene	1-3	1.0% 0.1%

# EPA (CERCLA) Reportable Quantity (in pounds):

EPA's Petroleum Exclusion applies to this material - (CERCLA 101(14)).

#### California Proposition 65:

Warning: This material may contain detectable quantities of the following chemicals, known to the State of California to cause cancer, birth defects or other reproductive harm, and which may be subject to the warning requirements of California Proposition 65 (CA Health & Safety Code Section 25249.5):

Component	Type of Toxicity
Toluene	Developmental Toxicant
	Female Reproductive Toxicant
Benzene	Cancer
	Developmental Toxicant
50.15	Male Reproductive Toxicant
Ethyl Benzene nternational Hazard Classification	Cancer

#### Canada:

This product has been classified in accordance with the hazard criteria of the Controlled Products Regulations (CPR) and the MSDS contains all the information required by the Regulations.

#### **WHMIS Hazard Class:**

B2 - Flammable Liquids

D2A

D2B

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# National Chemical Inventories

All components are either listed on the US TSCA Inventory, or are not regulated under TSCA All components are either on the DSL, or are exempt from DSL listing requirements

U.S. Export Control Classification Number: 1C981

# Section 16: Other Information

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1-Sep-2015

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Previous Issue Date:

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Revised Sections or Basis for Revision:

Identified Hazards (Section 2)

Precautionary Statement(s) (Section 2)

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First Aid (Section 4)
Exposure limits (Section 8)

Shipping information (Section 14) Regulatory information (Section 15)

SDS Number:

730370

#### **Guide to Abbreviations:**

ACGIH = American Conference of Governmental Industrial Hygienists; CASRN = Chemical Abstracts Service Registry Number; CEILING = Ceiling Limit (15 minutes); CERCLA = The Comprehensive Environmental Response, Compensation, and Liability Act; EPA = Environmental Protection Agency; GHS = Globally Harmonized System; IARC = International Agency for Research on Cancer; INSHT = National Institute for Health and Safety at Work; IOPC = International Oil Pollution Compensation; LEL = Lower Explosive Limit; NE = Not Established; NFPA = National Fire Protection Association; NTP = National Toxicology Program; OSHA = Occupational Safety and Health Administration; PEL = Permissible Exposure Limit (OSHA); SARA = Superfund Amendments and Reauthorization Act; STEL = Short Term Exposure Limit (15 minutes); TLV = Threshold Limit Value (ACGIH); TWA = Time Weighted Average (8 hours); UEL = Upper Explosive Limit; WHMIS = Worker Hazardous Materials Information

# Disclaimer of Expressed and implied Warranties:

The information presented in this Material Safety Data Sheet is based on data believed to be accurate as of the date this Material Safety Data Sheet was prepared. HOWEVER, NO WARRANTY OF MERCHANTABILITY, FITNESS FOR ANY PARTICULAR PURPOSE, OR ANY OTHER WARRANTY IS EXPRESSED OR IS TO BE IMPLIED REGARDING THE ACCURACY OR COMPLETENESS OF THE INFORMATION PROVIDED ABOVE, THE RESULTS TO BE OBTAINED FROM THE USE OF THIS INFORMATION OR THE PRODUCT, THE SAFETY OF THIS PRODUCT, OR THE HAZARDS RELATED TO ITS USE. No responsibility is assumed for any damage or injury resulting from abnormal use or from any failure to adhere to recommended practices. The information provided above, and the product, are furnished on the condition that the person receiving them shall make their own determination as to the suitability of the product for their particular purpose and on the condition that they assume the risk of their use. In addition, no authorization is given nor implied to practice any patented invention without a license.



# **Produced Brine Water**

Safety Data Sheet

# Section 1: Identification of the substance or mixture and of the supplier

**Product Name:** 

Produced Brine Water

SDS Number:

401320

Intended Use:

**Process Water** 

Manufacturer:

Ascent Resources 3501 N.W. 63rd

Oklahoma City, OK 73116

**Emergency Health and Safety Number:** 

Chemtrec: 800-424-9300 (24 Hours)

SDS Information:

Phone: 800-642-3074

URL: www.ascentresources.com

# Section 2: Hazard(s) Identification

## Classification

H302 - Harmful if swallowed - Category 1

H319 - Eye damage/irritation - Category 2

H316 - Causes mild skin irritation - Category 1

H332 - Harmful if inhaled - Category 1

H350 - Carcinogenicity - Category 1A

H412 -- May cause chronic harmful effects to aquatic life -- Category 2

#### **Label Elements**







#### DANGER

Causes serious eye irritation. (H319)\* Harmful if swallowed. (H302)\* Harmful if inhaled. (H332)\* May cause cancer. (H350)\*

Toxic to aquatic life with long lasting effects. (H412)\*

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#### Precautionary Statement(s):

Obtain special instructions before use. (P201)\*

Do not handle until all safety precautions have been read and understood. (P202)\*

Do not breathe dust/fume/gas/mist/vapours/spray. (P261)

Wash thoroughly after handling. (P264)\*

Do not eat, drink, or smoke when using this product. (P270)\*

Avoid release to the environment. (P273)\*

Use outdoors in a well ventelated space (P271)

Wear protective gloves / protective clothing / eye protection. (P281)\*

IF IN EYES: Rinse cautiously with water for several minutes. Remove contact lenses, if present and easy to do. Continue rinsing. (P305+P351+P338\*)

If eye irritation persists: Get medical advice/attention. (P313)\*

IF SWALLOWED: Immediately call a POISON CENTER or doctor/physician. (P301+P312)\*

IF INHALED: Remove victim to fresh air and keep at rest in a position comfortable for breathing. (P304 + P340)\*

Get medical advice/attention if you feel unwell. (P314)\*

Collect spillage. (P391)\* Store locked up. (P405)\*

Store in a well-ventilated place. Keep container tightly closed. (P403+P233)\*

Dispose of contents/container to approved disposal facility. (P501)\*

# Section 3: Composition / Information on Ingredients

Component	CAS#	Concentration <sup>1</sup>
Vater	7732-18-5	80-100%
Sodium chloride	91-20-3	<20%
Benzene	71-43-2	<2%

All concentrations are percent by weight unless ingredient is a gas. Gas concentrations are in percent by volume.

# Section 4: First Aid Measures

Eye Contact: For direct contact, remove contact lenses if present and easy to do. Immediately hold eyelids apart and flush the affected eye(s) with clean water for at least 20 minutes. Seek immediate medical attention.

**Skin Contact:** Remove contaminated shoes and clothing and cleanse affected area(s) thoroughly by washing with mild soap and water or a waterless hand cleaner. If irritation or redness develops and persists, seek medical attention.

**Inhalation (Breathing):** If respiratory symptoms develop, move victim away from source of exposure and into fresh air in a position comfortable for breathing. If breathing is difficult, oxygen or artificial respiration should be administered by qualified personnel. If symptoms persist, seek medical attention.

Ingestion (Swallowing): First aid is not normally required; however, if swallowed and symptoms develop, seek medical attention.

# Most important symptoms and effects

Acute: Headache, drowsiness, dizziness, loss of coordination, disorientation and fatigue.

Delayed: Dry skin and possible irritation with repeated or prolonged exposure.

**Notes to Physician:** Federal regulations (29 CFR 1910.1028) specify medical surveillance programs for certain exposures to benzene above the action level or PEL (specified in Section (i)(1)(i) of the Standard). In addition, employees exposed in an emergency situation shall, as described in Section (i)(4)(i), provide a urine sample at the end of the shift for measurement of urine phenol.

<sup>\* (</sup>Applicable GHS hazard code.)

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# Section 5: Fire-Fighting Measures



# NFPA 704 Hazard Class

Health: 1 Flammability: 4 Instability: 0

(0-Minimal, 1-Slight, 2-Moderate, 3-Serious, 4-Severe)

Unusual Fire & Explosion Hazards: This material may burn, but will not ignite readily. If container is not properly cooled, it can rupture in the heat of a fire.

**Extinguishing Media:** Dry chemical, carbon dioxide, foam, or water spray is recommended. Water or foam may cause frothing of materials heated above 212°F / 100°C. Carbon dioxide can displace oxygen. Use caution when applying carbon dioxide in confined spaces. Simultaneous use of foam and water on the same surface is to be avoided as water destroys the foam.

**Fire Fighting Instructions:** For fires beyond the initial stage, emergency responders in the immediate hazard area should wear protective clothing. When the potential chemical hazard is unknown, in enclosed or confined spaces, a self contained breathing apparatus should be worn. In addition, wear other appropriate protective equipment as conditions warrant (see Section 8).

Isolate immediate hazard area and keep unauthorized personnel out. Stop spill/release if it can be done safely. Move undamaged containers from immediate hazard area if it can be done safely. Water spray may be useful in minimizing or dispersing vapors and to protect personnel. Cool equipment exposed to fire with water, if it can be done safely. Avoid spreading burning liquid with water used for cooling purposes.

**Hazardous Combustion Products:** Combustion may yield smoke, carbon monoxide, and other products of incomplete combustion. Oxides of nitrogen and sulfur may also be formed.

See Section 9 for Flammable Properties including Flash Point and Flammable (Explosive) Limits

# Section 6: Accidental Release Measures

Personal Precautions: This material may burn, but will not ignite readily. Keep all sources of ignition away from spill/release. Stay upwind and away from spill/release. Avoid direct contact with material. For large spillages, notify persons down wind of the spill/release, isolate immediate hazard area and keep unauthorized personnel out. Wear appropriate protective equipment, including respiratory protection, as conditions warrant (see Section 8). See Sections 2 and 7 for additional information on hazards and precautionary measures.

**Environmental Precautions:** Stop spill/release if it can be done safely. Prevent spilled material from entering sewers, storm drains, other unauthorized drainage systems, and natural waterways. Use water sparingly to minimize environmental contamination and reduce disposal requirements. If spill occurs on water notify appropriate authorities and advise shipping of any hazard. Spills into or upon navigable waters, the contiguous zone, or adjoining shorelines that cause a sheen or discoloration on the surface of the water, may require notification of the National Response Center (phone number 800-424-8802).

**Methods for Containment and Clean-Up:** Notify relevant authorities in accordance with all applicable regulations. Immediate cleanup of any spill is recommended. Dike far ahead of spill for later recovery or disposal. Absorb spill with inert material such as sand or vermiculite, and place in suitable container for disposal. If spilled on water remove with appropriate methods (e.g. skimming, booms or absorbents). In case of soil contamination, remove contaminated soil for remediation or disposal, in accordance with local regulations.

Recommended measures are based on the most likely spillage scenarios for this material; however local conditions and regulations may influence or limit the choice of appropriate actions to be taken. See Section 13 for information on appropriate disposal.

# Section 7: Handling and Storage

**Precautions for safe handling:** Keep away from flames and hot surfaces. Obtain special instructions before use. Do not handle until all safety precautions have been read and understood. Do not breathe vapors or mists. Wear protective gloves/clothing and eye/face protection. Wash thoroughly after handling. Use good personal hygiene practices and wear appropriate personal protective equipment (see section 8).

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Do not enter confined spaces such as tanks or pits without following proper entry procedures such as ASTM D-4276 and 29CFR 1910.146. Do not wear contaminated clothing or shoes.

Conditions for safe storage: Keep container(s) tightly closed and properly labeled. This material may contain or release poisonous hydrogen sulfide gas. In a tank, barge, or other closed container, the vapor space above this material may accumulate hazardous concentrations of hydrogen sulfide. Check atmosphere for oxygen content, H2S, and flammability prior to entry. Use and store this material in cool, dry, well-ventilated area away from heat and all sources of ignition. Store only in approved containers. Keep away from any incompatible material (see Section 10). Protect container(s) against physical damage.

"Empty" containers retain residue and may be dangerous. Do not pressurize, cut, weld, braze, solder, drill, grind, or expose such containers to heat, flame, sparks, or other sources of ignition. They may explode and cause injury or death. "Empty" drums should be completely drained, properly bunged, and promptly shipped to the supplier or a drum reconditioner. All containers should be disposed of in an environmentally safe manner and in accordance with governmental regulations. Before working on or in tanks which contain or have contained this material, refer to OSHA regulations, ANSI Z49.1, and other references pertaining to cleaning, repairing, welding, or other contemplated operations.

# Section 8: Exposure Controls / Personal Protection

Component	ACGIH	OSHA	NIOSH
Water (7732-18-5)	Not established	Not established	Not established
Sodium chloride (7647-14-5)	Not established	Not established	Not established
Benzene (71-43-2)	STEL: 2.5 ppm TWA: 0.5 ppm Skin	Ceiling: 25 ppm STEL: 5 ppm TWA: 1 ppm	STEL: 5 ppm TWA: 0.1 ppm

Note: State, local or other agencies or advisory groups may have established more stringent limits. Consult an industrial hygienist or similar professional, or your local agencies, for further information.

**Engineering controls:** If current ventilation practices are not adequate to maintain airborne concentrations below the established exposure limits, additional engineering controls may be required.

**Eye/Face Protection:** The use of eye protection (such as splash goggles) that meets or exceeds ANSI Z.87.1 is recommended when there is potential liquid contact to the eye. Depending on conditions of use, a face shield may be necessary.

**Skin/Hand Protection:** The use of gloves impervious to the specific material handled is advised to prevent skin contact. Users should check with manufacturers to confirm the breakthrough performance of their products. Suggested protective materials: Nitrile

**Respiratory Protection:** Where there is potential for airborne exposure above the exposure limit a NIOSH certified air purifying respirator equipped with organic vapor cartridges/canisters may be used.

A respiratory protection program that meets or is equivalent to OSHA 29 CFR 1910.134 and ANSI Z88.2 should be followed whenever workplace conditions warrant a respirator's use. Air purifying respirators provide limited protection and cannot be used in atmospheres that exceed the maximum use concentration (as directed by regulation or the manufacturer's instructions), in oxygen deficient (less than 19.5 percent oxygen) situations, or under conditions that are immediately dangerous to life and health (IDLH).

If benzene concentrations equal or exceed applicable exposure limits, OSHA requirements for personal protective equipment, exposure monitoring, and training may apply (29CFR1910.1028 - Benzene).

Other Protective Equipment: Eye wash and quick-drench shower facilities should be available in the work area. Thoroughly clean shoes and wash contaminated clothing before reuse.

Suggestions provided in this section for exposure control and specific types of protective equipment are based on readily available information. Users should consult with the specific manufacturer to confirm the performance of their protective equipment. Specific situations may require consultation with industrial hygiene, safety, or engineering professionals.

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# Section 9: Physical and Chemical Properties

**Note:** Unless otherwise stated, values are determined at 20°C (68°F) and 760 mm Hg (1 atm). Data represent typical values and are not intended to be specifications.

Appearance:

Physical Form:

Odor Threshold:

pH:

Odor:

Vapor Pressure:

Vapor Density (air=1): Initial Boiling Point/Range:

Melting/Freezing Point:

**Pour Point:** 

Solubility in Water:

Partition Coefficient (n-octanol/water) (Kow):

Specific Gravity (water=1):

Viscosity:

Evaporation Rate (nBuAc=1):

Flash Point: Test Method:

Lower Explosive Limits (vol % in air): Upper Explosive Limits (vol % in air):

**Auto-ignition Temperature:** 

Varies (clear / amber / brown)

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Liquid Petroleum No data 4.9-8.5

No data available

>1

212 °F / 100 °C 32 °F / 0 °C

No data

Infinintely >10

1.0 -1.1 °API

No data available No data available No data available

Not applicable

1% 46%

No data available

# Section 10: Stability and Reactivity

Stability: Stable under normal ambient and anticipated conditions of use.

Conditions to Avoid: Avoid all possible sources of ignition. Prevent vapor accumulation.

Materials to Avoid (Incompatible Materials): Avoid contact with strong oxidizing and reducing agents.

Hazardous Decomposition Products: Not anticipated under normal conditions of use.

Hazardous Polymerization: Not known to occur.

# Section 11: Toxicological Information

Information on Toxicological Effects of Substance/Mixture

Acute Toxicity	Hazard	Additional Information	LC50/LD50 Data
Inhalation	Expected to have a low degree of toxicity by inhalation		No data
Skin Absorption	Unlikely to be harmful		No data
Ingestion (Swallowing)	Unlikely to be harmful		No data

Aspiration Hazard: Not expected to be an aspiration hazard.

Skin Corrosion/Irritation: Causes mild skin irritation. Repeated exposure may cause skin dryness or cracking.

Serious Eye Damage/Irritation: Causes serious eye irritation.

Status: FINAL

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**Signs and Symptoms:** Effects of overexposure may include irritation of the digestive tract, irritation of the respiratory tract, nausea, vomiting, diarrhea and signs of nervous system depression (e.g., headache, drowsiness, dizziness, loss of coordination, disorientation and fatigue).

Skin Sensitization: Not expected to be a skin sensitizer.

Respiratory Sensitization: No information available.

Specific Target Organ Toxicity (Single Exposure): May cause drowsiness and dizziness.

**Specific Target Organ Toxicity (Repeated Exposure):** May cause damage to organs through prolonged or repeated exposure. Laboratory animal studies of hydrocarpon products by the dermal and inhalation exposure routes have demonstrated toxicity to the liver, blood, spleen and thymus

Carcinogenicity: May cause cancer, based on component information.

Germ Cell Mutagenicity: Inadequate information available.

Reproductive Toxicity: Inadequate information available.

Other Comments: This material may contain varying concentrations of polycyclic aromatic hydrocarbons (PAHs) which have been known to produce a phototoxic reaction when contaminated skin is exposed to sunlight. The effect is similar in appearance to an exaggerated sunburn, and is temporary in duration if exposure is discontinued. Continued exposure to sunlight can result in more serious skin problems including pigmentation (discoloration), skin eruptions (pimples), and possible skin cancers.

# Information on Toxicological Effects of Components

#### **Water**

Carcinogenicity: No data available
Target Organs: No data available
Reproductive Toxicity: No data available
Germ Cell Mutagenicity: No data available

#### Sodium chloride

Carcinogenicity: No data available but sodium chloride has not been identified as a human carcinogen by IARC, the US National Toxicology Program and the US-Occupational Safety and Health Administration.

Target Organs: Eyes, respiratory system, central nervous system

Reproductive Toxicity: No data available Germ Cell Mutagenicity: No data available 401320 - Produced Brine Water **Date of Issue:** 1-Sep-2015

#### <u>Benzene</u>

Carcinogenicity: Benzene is an animal carcinogen and is known to produce acute myelogenous leukemia (a form of cancer) in humans. Benzene has been identified as a human carcinogen by IARC, the US National Toxicology Program and the US-Occupational Safety and Health Administration.

**Target Organs:** Prolonged or repeated exposures to benzene vapors can cause damage to the blood and blood forming organs, including disorders like leukopenia, thrombocytopenia, and aplastic anemia.

Reproductive Toxicity: Some studies in occupationally exposed women have suggested benzene exposure increased risk of miscarriage and stillbirth and decreased birth weight and gestational age. The size of the effects detected in these studies was small, and ascertainment of exposure and outcome in some cases relied on self-reports, which may limit the reliability of these results.

**Germ Cell Mutagenicity:** Benzene exposure has resulted in chromosomal aberrations in human lymphocytes and animal bone marrow cells. Exposure has also been associated with chromosomal aberrations in sperm cells in human and animal studies.

# Section 12: Ecological Information

Toxicity: Not evaluated

Persistence and Degradability: Not evaluated

Persistence per IOPC Fund definition: Not evaluated

**Bioaccumulative Potential:** Not evaluated although the solubility and log KOW would indicate it has little bioaccumulative potential.

**Mobility in Soil:** Not evaluated although the solubility properties indicate produced water would be highly mobile throughout a system.

Other Adverse Effects: None anticipated.

# Section 13: Disposal Considerations

The generator of a waste is always responsible for making proper hazardous waste determinations and needs to consider state and local requirements in addition to federal regulations.

This material, if discarded as produced, would not be a federally regulated RCRA "listed" hazardous waste. However, it would likely be identified as a federally regulated RCRA hazardous waste for the following characteristic(s) shown below. See Sections 7 and 8 for information on handling, storage and personal protection and Section 9 for physical/chemical properties. It is possible that the material as produced contains constituents which are not required to be listed in the MSDS but could affect the hazardous waste determination. Additionally, use which results in chemical or physical change of this material could subject it to regulation as a hazardous waste.

Container contents should be completely used and containers should be emptied prior to discard. Container residues and rinseates could be considered to be hazardous wastes.

#### EPA Waste Number(s)

D018 - Toxicity characteristic (Benzene)

# Section 14: Transport Information

# U.S. Department of Transportation (DOT)

Shipping name: N

Not regulated

Note: Some states may require specific shipping lables. Contact each jurisdiction for more information.

Status: FINAL

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# Section 15: Regulatory Information

# CERCLA/SARA - Section 302 Extremely Hazardous Substances and TPQs (in pounds):

This material does not contain any chemicals subject to the reporting requirements of SARA 302 and 40 CFR 372.

# CERCLA/SARA - Section 311/312 (Title III Hazard Categories)

Acute Health: Chronic Health: Yes

Yes

Fire Hazard:

No

Pressure Hazard:

No

Reactive Hazard:

No

# CERCLA/SARA - Section 313 and 40 CFR 372:

This material contains the following chemicals subject to the reporting requirements of Section 313 of SARA Title III and 40 CFR 372:

Component	Concentration¹	de minimis
Benzene	<2	0.1%

# EPA (CERCLA) Reportable Quantity (in pounds):

EPA's Petroleum Exclusion applies to this material - (CERCLA 101(14)).

Warning: This material may contain detectable quantities of the following chemicalsidentified on federal and individual state hazardouis substances list. Contact each jurisdiction for more information.

Component	Type of Toxicity
Benzene	Cancer Developmental Toxicant Male Reproductive Toxicant

#### **International Hazard Classification:**

#### Canada:

This product has been classified in accordance with the hazard criteria of the Controlled Products Regulations (CPR) and the MSDS contains all the information required by the Regulations.

#### WHMIS Hazard Class:

D<sub>2</sub>A

D2B

#### **National Chemical Inventories**

All components are either listed on the US TSCA Inventory, or are not regulated under TSCA All components are either on the DSL, or are exempt from DSL listing requirements

U.S. Export Control Classification Number: 1C981

# Section 16: Other Information

Date of Issue:

1-Sep-2015

Status:

**FINAL** 

401320 - Produced Brine Water Date of Issue: 1-Sep-2015

Status: FINAL

Revised Sections or Basis for Revision:

Identified Hazards (Section 2)
Precautionary Statement(s) (Section 2)
First Aid (Section 4)
Shipping information (Section 14)
Regulatory information (Section 15)
401320

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SDS Number:

#### **Guide to Abbreviations:**

ACGIH = American Conference of Governmental Industrial Hygienists; CASRN = Chemical Abstracts Service Registry Number; CEILING = Ceiling Limit (15 minutes); CERCLA = The Comprehensive Environmental Response, Compensation, and Liability Act; EPA = Environmental Protection Agency; GHS = Globally Harmonized System; IARC = International Agency for Research on Cancer; INSHT = National Institute for Health and Safety at Work; IOPC = International Oil Pollution Compensation; LEL = Lower Explosive Limit; NE = Not Established; NFPA = National Fire Protection Association; NTP = National Toxicology Program; OSHA = Occupational Safety and Health Administration; PEL = Permissible Exposure Limit (OSHA); SARA = Superfund Amendments and Reauthorization Act; STEL = Short Term Exposure Limit (15 minutes); TLV = Threshold Limit Value (ACGIH); TWA = Time Weighted Average (8 hours); UEL = Upper Explosive Limit; WHMIS = Worker Hazardous Materials Information

# Disclaimer of Expressed and implied Warranties:

The information presented in this Material Safety Data Sheet is based on data believed to be accurate as of the date this Material Safety Data Sheet was prepared. HOWEVER, NO WARRANTY OF MERCHANTABILITY, FITNESS FOR ANY PARTICULAR PURPOSE, OR ANY OTHER WARRANTY IS EXPRESSED OR IS TO BE IMPLIED REGARDING THE ACCURACY OR COMPLETENESS OF THE INFORMATION PROVIDED ABOVE, THE RESULTS TO BE OBTAINED FROM THE USE OF THIS INFORMATION OR THE PRODUCT, THE SAFETY OF THIS PRODUCT, OR THE HAZARDS RELATED TO ITS USE. No responsibility is assumed for any damage or injury resulting from abnormal use or from any failure to adhere to recommended practices. The information provided above, and the product, are furnished on the condition that the person receiving them shall make their own determination as to the suitability of the product for their particular purpose and on the condition that they assume the risk of their use. In addition, no authorization is given nor implied to practice any patented invention without a license.

# Attachment I: Emission Units Table

# Attachment I

# **Emission Units Table**

(includes all emission units and air pollution control devices that will be part of this permit application review, regardless of permitting status)

Emission	Emission	Emission Unit Description	Voor lestelle 1/	D- :	T	
Unit ID <sup>1</sup>	Point ID <sup>2</sup>	Zimesion offit Description	Year Installed/ Modified	Design Capacity	Type <sup>3</sup> and Date of Change	Control Device 4
FUG-1	14E	Sitewide Fugitive	2015	N/A	Mod	N/A
ENG-2	9E	Natural Gas-Fired Generator (HiPower)	2015	47 hp	Mod	N/A
GPU-1	1E	Gas Production Unit	2015	1.50 MMBtuH	Mod	N/A
GPU-2	2E	Gas Production Unit	2015	1.50 MMBtuH	Mod	N/A
GPU-3	3E	Gas Production Unit	2015	1.50 MMBtuH	Mod	N/A
HTR-1	4E	Line Heater	2015	1.50 MMBtuH	Mod	N/A
SEP-1	7E	Flash Separator Heater	2015	1.00 MMBtuH	Mod	N/A
CS-1	11E	Condensate Stabilizer Heater	2015	0.75 MMBtuH	Mod	N/A
CTK-1	15E	Tank 1 - Condensate Storage Tank	2015	400-bbl	Mod	CTRL-1
CTK-2	16E	Tank 2 - Condensate Storage Tank	2015	400-bb1	Mod	CTRL-1
CTK-3	17E	Tank 3 - Condensate Storage Tank	2015	400-bbl	Mod	CTRL-1
PTK-1	18E	Tank 4 - Prod. Water Storage Tank	2015	400-bb1	Mod	CTRL-1
PTK-2	19E	Tank 5 - Prod. Water Storage Tank	2015	400-bbl	Mod	CTRL-1
PTK-3	20E	Tank 6 - Prod. Water Storage Tank	2015	400-bbl	Mod	CTRL-1
CTRL-1	10E	Enclosed Combustor	2015	18.42 MMBtuH	Mod	N/A
TRL-1	12E	Condensate Truck Loading	2015	N/A	Mod	N/A
TRL-2	13E	Produced Water Truck Loading	2015	N/A	Mod	N/A
ROAD-1	21E	Unpaved Road Sources	2015	N/A	Mod	N/A

<sup>&</sup>lt;sup>1</sup> For Emission Units (or <u>S</u>ources) use the following numbering system:1S, 2S, 3S,... or other appropriate designation.

<sup>2</sup> For <u>E</u>mission Points use the following numbering system:1E, 2E, 3E, ... or other appropriate designation.

<sup>3</sup> New, modification, removal

<sup>4</sup>For <u>C</u>ontrol Devices use the following numbering system: 1C, 2C, 3C,... or other appropriate designation.

# Attachment J: Emission Points Data Summary Sheet

# Attachment J EMISSION POINTS DATA SUMMARY SHEET

J-				$\neg$		_			Ţ.	_		_	_	_	_		_	
	Emission Concentration 7 (ppmv or mg/m <sup>4</sup> )																	
	Est. Method Used <sup>6</sup>		EE			EE					EE	_	_	-		BE		
	Emission Form or Phase (At exit conditions,	or Gas/Vapor)	Gas/Vapor			Gas/Vapor					Gas/Vapor					Gas/Vapor		
	Maximum Potential Controlled Emissions <sup>5</sup>	ton/yr	9.27	0.04	0.64	0.54	0.05	<0.01	0.04	0.64	0.54	0.05	<0.01	0.04	0.64	0.54	0.05	<0.01
	May Pod Con Emis	lb/hr	2.13	0.01	0.15	0.12	0.01	<0.01	0.01	0.15	0.12	0.01	<0.01	0.01	0.15	0.12	0.01	<0.01
	Maximum Potential Uncontrolled Emissions 4	ton/yr	9.27	0.04	0.64	0.54	0.05	<0.01	0.04	0.64	0.54	0.05	<0.01	0.04	0.64	0.54	0.05	<0.01
) ata	Max Pote Uncor Emiss	lb/hr	2.13	0.01	0.15	0.12	0.01	<0.01	0.01	0.15	0.12	0.01	<0.01	0.01	0.15	0.12	0.01	<0.01
Table 1: Emissions Data	All Regulated Pollutants - Chemical Name/CAS <sup>3</sup> (Speciate VOCs & HAPS)		VOC	VOC	NOx	00	PM	SO2	NOC	NOx	00	PM	SO2	NOC	NOx	00	PM	SO2
Table 1:	Vent Time for Emission Unit (chemical processes only)	Max (hr/yr)	8760			8760					8760					8760		7
	Vent Emiss (che	Short Term <sup>2</sup>	Ü			ပ			_		ပ					C		
	Air Pollution Control Device (Must match Emission Units Table & Plot Plan)	Device Type	N/A			N/A					N/A					N/A	·	
	Air F Contr (Mus Emission & Pi	ID No.	N/A			N/A				_	N/A			_		N/A		
	Emission Unit Vented Through This Point (Must match Emission Units	Source	FUG-1		***	GPU-1					GPU-2					GPU-3		
	Emiss Ve. Throu P( (Must Emissi Table &	ID No.	14E			ΙΈ					2E	<u></u>				3E		
	Emission Point Type <sup>1</sup>		Fugitive		Horizontal	Stack				Horizontal	Stack				Horizontal	Stack		
	Emission Point ID No. (Must match Emission Units Table & Plot Plan)		14E			JE				Į	7E				_	3E		

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		Emission Concentration 7 (ppmv or	mg/m <sup>4</sup> )												
		Est. Method Used <sup>6</sup>						EE				_	EE		
		Emission Form or Phase	(At exit conditions, Solid, Liquid	Gas/Vapor)				Gas/Vapor					Gas/Vapor		
		Maximum Potential Controlled	EMISSIONS		ton/yr	0.04	0.64	0.54	0.05	<0.01	0.02	0.43	0.36	0.03	<0.01
		Maxi Confi	SS E E E E E E E E E E E E E E E E E E		lb/hr	0.01	0.15	0.12	0.01	<0.01	0.01	0.10	0.08	0.01	<0.01
		Maximum Potential Uncontrolled			ton/yr	0.04	0.64	0.54	0.05	<0.01	0.02	0.43	0.36	0.03	<0.01
ata		Maxi Pote	2 2 2 3 3 4 4 7 7		lb/hr	0.01	0.15	0.12	0.01	<0.01	0.01	0.10	0.08	0.01	<0.01
Table 1: Emissions Data		All Regulated Pollutants - Chemical Name/CAS3	(Speciate VOCs & HAPS)			NOC	NOx	00	PM	SO2	70V	NOx	00	PM	S02
able 1:		Vent Time for Emission Unit (chemical processes only)			Max (hr/yr)			8760	_				8760		
_		Vent   Emiss (che			Short Term <sup>2</sup>	-		ပ					C		
	: :	Alr Pollution Control Device (Must match Emission Units Table	ot Plan)		Device Type			N/A					N/A	•	
		Alr P Contr (Mu Emission	~ ~		ID No.		-	N/A					N/A	_	
	11 1 40	Vented Vented Through This	(Must match Emission Units Table & Plot Plan)		Source			HTR-1					SEP-1		
	C	Throu	(Musi Emissi Table &		Ω No.			4E					7E		
	Fmission	Point Type <sup>1</sup>	-	•			Horizontal	Stack			· .	Horizontal	Stack		
	Emission	Point ID No. (Must match Emission Units Table	& Plot Plan)				į	4E				Į	7/ -		

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			_		_				_	_												
	Emission Concentra tion <sup>7</sup> (ppmv or	mg/m <sup>4</sup> )																				
	Est. Method Used <sup>6</sup>					EE					BE			0	(Tanks 4.0.9d methodology,	Promax)	(Tanks 4.0.9d methodology,	0	(Tanks 4.0.9d	methodology, Promax)	0	(Tanks 4.0.9d methodology, Promax)
	Emission Form or Phase	Conditions, Solid, Liquid or Or			-1	Gas/Vapor					Gas/Vapor				Gas/Vapor		Gas/Vapor		Gas/Vapor			Gas/Vapor
	Maximum Potential Controlled Emissions 5		ton/yr	0.05	1.27	2.18	0.03	<0.01	0.02	0.32	0.27	0.02	<0.01		1.82		1.82		1.82			<0.01
	May Pot Con Emis		lb/hr	0.01	0.29	0.50	0.01	<0.01	<0.01	0.07	90.0	0.01	<0.01		1		1					1
	Maximum Potential Uncontrolled Emissions <sup>4</sup>		ton/yr	0.05	1.27	2.18	0.03	<0.01	0.02	0.32	0.27	0.02	<0.01	-	91.03		91.03		91.03			0.20
g	Maxi Pote Uncor Emiss		lb/hr	0.01	0.29	0.50	0.01	<0.01	<0.01	0.07	90.0	0.01	<0.01		ı		ŀ		1			-
Table 1: Emissions Data	All Regulated Pollutants - Chemical Name/CAS <sup>3</sup>	(Speciate VOCs & HAPS)		VOC	NOx	00	PM	SO2	NOC	NOx	00	PM	SO2		VOC		NOC		NOC			VOC
ble 1: E	me for on Unit nical		Max (hr/yr)		_	8760					09/8	-			0928		8760		8760			8760
Ta	Vent Time for Emission Unit (chemical processes only)		Short Term²			Ö	-		_		O				D D		ن ن		C			υ l
	Air Pollution Control Device (Must match Emission Units Table & Plot Plan)	_	Device Type			N/A					N/A			_	Flare		Flare	_	Flare			Flare
	Air I Contr (Mu Emission		ID No.			N/A				-	N/A				10E		10E		10E		-	10E
	Emission Unit Vented Through This Point (Must match	Emission Units Table & Plot Plan)	Source			ENG-2				ű	1-80			1 717	CIN-1	_	CTK-2		CIK-3		PTK 1	
	Emissi Ver Throug Pc	Emissic Table & I	ID No.			9E				7	TIE TIE			77	361	_	16E	ļ	17E		181	100
	Emission Point Type <sup>1</sup>				Vertical	Stack				Horizontal	Stack			Vent / Combustor	Vertical Stack	Vent/	Combustor Vertical Stack	Vent /	Vertical	Угаск	Vent / Combustor	Vertical Stack
	Emission Point ID No. (Must match Emission Units Table & Plot Plan)				į	7E				į	116			17	361		16E		17E		Li	

	1							
	Emission Concentrati on <sup>7</sup> (ppmv or mg/m <sup>4</sup> )							
	Est. Method Used <sup>6</sup>		O (Tanks 4.0.9d methodology,	O (Tanks 4.0.9d methodology,	Promax) EE	EE	EE	H
	Emission Form or Phase (At exit conditions, Solid	Liquid or Gas/Vapor)	Gas/Vapor	Gas/Vapor	Gas/Vapor	Gas/Vapor	Gas/Vapor	Solid
	Maximum Potential Controlled Emissions <sup>5</sup>	ton/yr	<0.01	<0.01	2.82	0.14	5.49	3.24
	Cor	lb/hr		1	58.95	0.59	1.25	0.74
	Maximum Potential Uncontrolled Emissions <sup>4</sup>	ton/yr	0.20	0.20	2.82	0.14	5.49	3.24
ata	Max Pot Unco Emisi	lb/hr	!	1	58.95	0.59	1.25	0.74
Table 1: Emissions Data	All Regulated Pollutants - Chemical Name/CAS³ (Speciate VOCs & HAPS)		VOC	VOC	NOC	NOC	NO <sub>X</sub>	PM(total)
Table 1:	Vent Time for Emission Unit (chemical processes only)	Max (hr/yr)	8760	0928	0928	8760	8760	8760
	Vent Emiss (ch proces	Short Term <sup>2</sup>	၁	C	Ü	C	Ü	C
	Air Pollution Control Device (Must match Emission Units Table & Plot Plan)	Device Type	Flare	Flare	N/A	N/A	N/A	N/A
	Air F Contr (Mu Emission & P	ID No.	10E	10E	N/A	N/A	N/A	N/A
	Emission Unit Vented Through This Point (Must match Emission Units	Source	PTK-2	PTK-3	CTK-1 CTK-2 CTK-3	PTK-1 PTK-2 PTK-3	CTRL-1	ROADS
	Emisss Ve Throu Pu (Mus) Emissi	ID No.	19E	20E	15E, 16E, 17E	18E, 19E, 20E	10E	21E
	Emission Point Type <sup>1</sup>		Vent / Combustor Vertical Stack	Vent / Combustor Vertical Stack	Truck Vent	Truck Vent	Flare	Fugitive
	Emission Point ID No. (Must match Emission Units Table & Plot Plan)		19E	20E	12E	13E	10E	21E

The EMISSION POINTS DATA SUMMARY SHEET provides a summation of emissions by emission unit. Note that uncaptured process emission unit emissions are not typically considered to be fugitive and must be accounted for on the appropriate EMISSIONS UNIT DATA SHEET and on the EMISSION POINTS DATA SUMMARY SHEET. Please note that total emissions from the source are equal to all vented emissions, all fugitive emissions, plus all other emissions (e.g. uncaptured emissions). Please complete the FUGITIVE EMISSIONS DATA SUMMARY SHEET for fugitive emission activities.

2 Indicate by "C" if venting is continuous. Otherwise, specify the average short-term venting rate with units, for intermittent venting (ie., 15 min/hr). Indicate as many rates as needed

<sup>3</sup> List all regulated air pollutants. Speciate VOCs, including all HAPs. Follow chemical name with Chemical Abstracts Service (CAS) number. **LIST** Acids, CO, CS<sub>2</sub>, VOCs, H<sub>2</sub>S, Inorganics, Lead, Organics, O<sub>3</sub>, NO, NO<sub>2</sub>, SO<sub>2</sub>, SO<sub>3</sub>, all applicable Greenhouse Gases (including CO<sub>2</sub> and methane), etc. **DO NOT LIST** H<sub>2</sub>, H<sub>2</sub>O, N<sub>2</sub>, O<sub>2</sub>, and Noble Gases.

4 Give maximum potential emission rate with no control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20

<sup>5</sup> Give maximum potential emission rate with proposed control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb

6 Indicate method used to determine emission rate as follows: MB = material balance; ST = stack test (give date of test); EE = engineering estimate;

Provide for all pollutant emissions. Typically, the units of parts per million by volume (ppmv) are used. If the emission is a mineral acid (sulfuric, nitric, hydrochloric or phosphoric) use units of miligram per dry cubic meter (mg/m³) at standard conditions (68 °F and 29.92 inches Hg) (see 45CSR7). If the pollutant is SO₂, use units of ppmv (See 45CSR10). O = other (specify).

# Attachment J EMISSION POINTS DATA SUMMARY SHEET

	se (km)	Easting		532770	532770	532770	532770	07770	0//260	3321/0	532770	532770	532770	532770	07776	532770	011776	07/75	077770	0//780	532770
	UTM Coordinates (km)		4	1	-	4,	-	, , ,	,	,	S	5	1 "	-	) "	7 4	) 4	7	0 0	, i	, , , ,
	OTMC	Northing		4384250	4384255	4384260	4384265	4384270	4384775	C/740Ct	4584280	4384285	4384290	4384295	4384300	4384305	012884310	712727	0000000	7004004	4384330
	Emission Point Elevation (ft)	Stack Height <sup>2</sup> (Release height of emissions above	ground level)	×	10	10	10	10	01		10	10	10	20	20	20	20	02	02	07	N/A
ter Data	Emission Poir	Ground Level (Height above mean sea level)	1134	+CII	1134	1134	1134	1134	1134	1137	1011	1134	1134	1134	1134	1134	1134	1134	1134	1134	1134
Release Parameter Data		Velocity (fps)	1001	100.1	N/A	N/A	N/A	N/A	N/A	N/A	4777	N/A	N/A	N/A	N/A	N/A	N/A	N/A	A/X	N/A	N/A
Table 2: Rele	Exit Gas	Volumetric Flow 1 (acfm) at operating conditions	208	000	IN/A	N/A	N/A	N/A	N/A	N/A		N/A	N/A	N/A	N/A	N/A	N/A	N/A	N/A	N/A	N/A
		Temp. (°F)	1050	4/2	17/17	N/A	N/A	N/A	N/A	N/A	NT/A	IN/A	N/A	N/A	N/A	N/A	N/A	N/A	N/A	N/A	N/A
	Inner	(ft.)	0.21	N/A	7/14	N/A	N/A	N/A	N/A	N/A	\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\	VAI	N/A	N/A	N/A	N/A	N/A	N/A	N/A	N/A	N/A
	Emission Point ID	No. (Must match Emission Units Table)	9E	1E	)F	777	3E	4E	5E	6E	7E	! ! !	111E	15E	16E	17E	18E	19E	20E	10E	12E

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632770	011700	627770	0//700	532770	0/1700
4384335		4384340	01010	4384345	5
N/A	*****	N/A	X7/AT	N/A	4 4 7 7 4
1134		1134		1134	
N/A		N/A		N/A	
N/A		N/A		N/A	
N/A		N/A		N/A	
N/A		N/A		N/A	
13E	171	14E		21E	

<sup>1</sup>Give at operating conditions. Include inerts.
<sup>2</sup> Release height of emissions above ground level.

# Attachment K: Fugitive Emissions Data Summary Sheet

#### Attachment K

# **FUGITIVE EMISSIONS DATA SUMMARY SHEET**

The FUGITIVE EMISSIONS SUMMARY SHEET provides a summation of fugitive emissions. Fugitive emissions are those emissions which could not reasonably pass through a stack, chimney, vent or other functionally equivalent opening. Note that uncaptured process emissions are not typically considered to be fugitive, and must be accounted for on the appropriate EMISSIONS UNIT DATA SHEET and on the EMISSION POINTS DATA SUMMARY SHEET.

Please note that total emissions from the source are equal to all vented emissions, all fugitive emissions, plus all other emissions (e.g. uncaptured emissions).

$\vdash$	APPLICATION FORMS CHECKLIST - FUGITIVE EMISSIONS
1.)	Will there be haul road activities?
	⊠ Yes □ No
	If YES, then complete the HAUL ROAD EMISSIONS UNIT DATA SHEET.
2.)	Will there be Storage Piles?
	☐ Yes
	☐ If YES, complete Table 1 of the NONMETALLIC MINERALS PROCESSING EMISSIONS UNIT DATA SHEET.
3.)	Will there be Liquid Loading/Unloading Operations?
	∑ Yes □ No
	☑ If YES, complete the BULK LIQUID TRANSFER OPERATIONS EMISSIONS UNIT DATA SHEET.
4.)	Will there be emissions of air pollutants from Wastewater Treatment Evaporation?
	☐ Yes          No
	☐ If YES, complete the GENERAL EMISSIONS UNIT DATA SHEET.
5.)	Will there be Equipment Leaks (e.g. leaks from pumps, compressors, in-line process valves, pressure relief devices, open-ended valves, sampling connections, flanges, agitators, cooling towers, etc.)?
	⊠ Yes □ No
	☑ If YES, complete the LEAK SOURCE DATA SHEET section of the CHEMICAL PROCESSES EMISSIONS UNIT DATA SHEET.
6.)	Will there be General Clean-up VOC Operations?
	☐ Yes
	☐ If YES, complete the GENERAL EMISSIONS UNIT DATA SHEET.
7.)	Will there be any other activities that generate fugitive emissions?
	⊠ Yes □ No
	☑ If YES, complete the GENERAL EMISSIONS UNIT DATA SHEET or the most appropriate form.
lf you Sum	answered "NO" to all of the items above, it is not necessary to complete the following table, "Fugitive Emissions mary."

FUGITIVE EMISSIONS SUMMARY	All Regulated Pollutants · Chemical Name/CAS ¹	Maximum Potential Uncontrolled Emissions <sup>2</sup>	Potential Emissions 2	Maximum Potential Controlled Emissions 3	otential nissions <sup>3</sup>	Est. Method
Haul Road/Road Dust Emissions Paved Haul Roads	N/A		S. Carlotte	10/UI	ton/yr	
Unpaved Haul Roads	N/A (Included in Attachment L)					
Storage Pile Emissions	N/A					
Loading/Unloading Operations	N/A (Included in Attachment L)					
Wastewater Treatment Evaporation & Operations	N/A					
Equipment Leaks	VOC HAPs	2.13	9.27	2.13	9.27	Ш
General Clean-up VOC Emissions	N/A					
Other	N/A (Included in Attachment L)					

<sup>1</sup>List all regulated air pollutants. Speciate VOCs, including all HAPs. Follow chemical name with Chemical Abstracts Service (CAS) number. LIST Acids, CO, CS<sub>2</sub>, VOCs, H2S, Inorganics, Lead, Organics, O<sub>3</sub>, NO, NO<sub>2</sub>, SO<sub>2</sub>, SO<sub>3</sub>, all applicable Greenhouse Gases (including CO<sub>2</sub> and methane), etc. DO NOT LIST H<sub>2</sub>, H<sub>2</sub>O, N<sub>2</sub>,

<sup>2</sup> Give rate with no control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute batch).
<sup>3</sup> Give rate with proposed control equipment operating. If emissions occur for less than 1 hr, then record emissions per batch in minutes (e.g. 5 lb VOC/20 minute

⁴ Indicate method used to determine emission rate as follows: MB = material balance; ST = stack test (give date of test); EE = engineering estimate; O = other

# Attachment L: Emissions Unit Data Sheet(s)

# Attachment L EMISSIONS UNIT DATA SHEET GENERAL

To be used for affected sources other than asphalt plants, foundries, incinerators, indirect heat exchangers, and quarries.

Identification Number (as assigned on *Equipment List Form*): 1E, 2E, 3E

TE, ZE, 3E
Name or type and model of proposed affected source:
Three (3) Gas Production Units
<ol> <li>On a separate sheet(s), furnish a sketch(es) of this affected source. If a modification is to be made to this source, clearly indicated the change(s). Provide a narrative description of al features of the affected source which may affect the production of air pollutants.</li> </ol>
3. Name(s) and maximum amount of proposed process material(s) charged per hour:
N/A
4. Name(s) and maximum amount of proposed material(s) produced per hour:
Per Unit:
0.01 lb/hr VOC 0.15 lb/hr NOx
0.13 lb/lii NOX 0.12 lb/hr CO 0.01 lb/hr PM
0.01 lb/hr PM
5. Give chemical reactions, if applicable, that will be involved in the generation of air pollutants:
N/A

<sup>\*</sup> The identification number which appears here must correspond to the air pollution control device identification number appearing on the *List Form*.

	0 1 11 11				
6.	Combustion Data (if app				
	(a) Type and amount in	appropriate units	of fuel(s) to be	burned:	
N	atural Gas: 1470.6 scf/hr				
	(b) Chemical analysis of	proposed fuel(s),	excluding coal,	including maxi	mum percent sulfur
	and ash:			_	•
	. Au 1				
56	e Attachment N, Table 20.				
	(a) Theoretical as when the		/		
	(c) Theoretical combusti	on air requirement	(ACF/unit of fu	iel):	
	@		°F and		psia.
	(d) Percent excess air:				
	(e) Type and BTU/hr of b	ourners and all other	er firing equipm	ent planned to	ho usod:
			or ming oquipm	ont planned to	be used.
					=
1.5	0 MMBtu/hr, each				
(	f) If coal is proposed as	a source of fuel, ic	lentify supplier	and seams and	dive sizing of the
	coal as it will be fired:		contact outphior	ana ocamo anc	give sizing of the
6	g) Proposed maximum de	esian hoat innut:			406 PTI I
_					× 10 <sup>6</sup> BTU/hr.
. F	rojected operating sched	ule:			
lour	s/Day 24	Days/Week	7	   Weeks/Year	52
	<del>-</del>	,	,	TY CONS/ TEAT	52

8.	Projected amount of poll devices were used:	utants that would b	e emitted fro	om this affected source if no contro
(	N/A	°F a	nd	psia
a.	NO <sub>X</sub>	0.15	lb/hr	grains/ACF
b.	SO <sub>2</sub>		lb/hr	grains/ACF
C.	СО	0.12	lb/hr	grains/ACF
d.	PM <sub>10</sub>	0.01	lb/hr	grains/ACF
e.	Hydrocarbons		lb/hr	grains/ACF
f.	VOCs	0.01	lb/hr	grains/ACF
g.	Pb		lb/hr	grains/ACF
h.	Specify other(s)	1		
	Benzene	<0.0001	lb/hr	grains/ACF
_	Formaldehyde	<0.0001	lb/hr	grains/ACF
_	n-Hexane	0.003	lb/hr	grains/ACF
_	Toluene	<0.0001	lb/hr	grains/ACF

NOTE: (1) An Air Pollution Control Device Sheet must be completed for any air pollution device(s) used to control emissions from this affected source.

<sup>(2)</sup> Complete the Emission Points Data Sheet.

compliance with the proposed emissions lin	and reporting in order to demonstrate compliance
MONITORING N/A	RECORDKEEPING N/A
REPORTING N/A	TESTING
IVA	N/A
MONITORING. PLEASE LIST AND DESCRIBE THE PROPOSED TO BE MONITORED IN ORDER TO DEMONIPROCESS EQUIPMENT OPERATION/AIR POLLUTION (	STRATE COMPLIANCE WITH THE OPERATION OF THIS
<b>RECORDKEEPING.</b> PLEASE DESCRIBE THE PROP MONITORING.	OSED RECORDKEEPING THAT WILL ACCOMPANY THE
<b>REPORTING.</b> PLEASE DESCRIBE THE PRO	POSED FREQUENCY OF REPORTING OF THE
TESTING. PLEASE DESCRIBE ANY PROPOSED EMIS POLLUTION CONTROL DEVICE.	SIONS TESTING FOR THIS PROCESS EQUIPMENT/AIR
10. Describe all operating ranges and mainten- maintain warranty	ance procedures required by Manufacturer to
N/A	

To be used for affected sources other than asphalt plants, foundries, incinerators, indirect heat exchangers, and quarries.

Identification Number (as assigned on *Equipment List Form*): 4E, 5E, 6E

Name or type and model of proposed affected source:
One (1) Line Heater
2. On a separate sheet(s) furnish a sketch(es) of this affected source. If a modification is to be
<ol> <li>On a separate sheet(s), furnish a sketch(es) of this affected source. If a modification is to be made to this source, clearly indicated the change(s). Provide a narrative description of all features of the affected source which may affect the production of air pollutants.</li> </ol>
Name(s) and maximum amount of proposed process material(s) charged per hour:
N/A
4. Name(s) and maximum amount of proposed material(s) produced per hour:
0.01 lb/hr VOC
0.15 lb/hr NOx 0.12 lb/hr CO
0.01 lb/hr PM
5. Give chemical reactions if applicable that will be involved to the
5. Give chemical reactions, if applicable, that will be involved in the generation of air pollutants:
N/A

<sup>\*</sup> The identification number which appears here must correspond to the air pollution control device identification number appearing on the *List Form*.

	Camalassatt	D / //5				
0.		n Data (if app				
	(a) Type ar	nd amount in	appropriate units	of fuel(s) to be	burned:	
N	atural Gas: 147	70.6 scf/hr				
	(b) Chemic and ash	al analysis of	proposed fuel(s),	excluding coal	, including max	imum percent sulfui
Se	ee Attachment I	N, Table 20.				
	(c) Theoreti	cal combustic	on air requiremen	t (ACF/unit of fu	ıel):	
		@		°F and		psia.
	(d) Percent	excess air:				
-	(e) Type and	d BTU/hr of b	urners and all oth	er firing equipm	nent planned to	be used:
	0 MMBtu/hr  f) If coal is properties of the coal as it	proposed as will be fired:	a source of fuel, i	dentify supplier	and seams and	d give sizing of the
		maximum de	esign heat input:			× 10 <sup>6</sup> BTU/hr.
		naung sched	uie: 		1	
our	s/Day	24	Days/Week	7	Weeks/Year	52

8.	Projected amount of pollutants that would be emitted from this affected source if no contro devices were used:			
@	N/A	°Fa	nd	psia
a.	NO <sub>X</sub>	0.15	lb/hr	grains/ACF
b.	SO <sub>2</sub>		lb/hr	grains/ACF
C.	СО	0.12	lb/hr	grains/ACF
d.	PM <sub>10</sub>	0.01	lb/hr	grains/ACF
e.	Hydrocarbons		lb/hr	grains/ACF
f.	VOCs	0.01	lb/hr	grains/ACF
g.	Pb		lb/hr	grains/ACF
h.	Specify other(s)	1		
_	Benzene	<0.0001	lb/hr	grains/ACF
_	Formaldehyde	<0.0001	lb/hr	grains/ACF
_	n-Hexane	0.003	lb/hr	grains/ACF
	Toluene	<0.0001	lb/hr	grains/ACF

NOTE: (1) An Air Pollution Control Device Sheet must be completed for any air pollution device(s) used to control emissions from this affected source.

<sup>(2)</sup> Complete the Emission Points Data Sheet.

<ol> <li>Proposed Monitoring, Recordkeeping, Rep Please propose monitoring, recordkeeping, with the proposed operating parameters. compliance with the proposed emissions line</li> </ol>	and reporting in order to demonstrate compliance.
MONITORING	RECORDKEEPING
N/A	N/A
REPORTING	TEOTING
N/A	TESTING N/A
MONITORING. PLEASE LIST AND DESCRIBE THE PROPOSED TO BE MONITORED IN ORDER TO DEMONS PROCESS EQUIPMENT OPERATION/AIR POLLUTION (	STRATE COMPLIANCE WITH THE OPERATION OF THIS
RECORDKEEPING. PLEASE DESCRIBE THE PROPMONITORING.	
<b>REPORTING.</b> PLEASE DESCRIBE THE PRORECORDKEEPING.	POSED FREQUENCY OF REPORTING OF THE
TESTING. PLEASE DESCRIBE ANY PROPOSED EMIS	SSIONS TESTING FOR THIS PROCESS FOLUDAMENT/AID
POLLOTION CONTROL DEVICE.	
10. Describe all operating ranges and maintenamentain warranty	ance procedures required by Manufacturer to
N/A	
	ľ

To be used for affected sources other than asphalt plants, foundries, incinerators, indirect heat exchangers, and quarries.

Identification Number (as assigned on Equipment List Form): 7E

1. Name or type and model of proposed affected source:

One (1) Flash Separator Heater

2. On a separate sheet(s), furnish a sketch(es) of this affected source. If a modification is to be made to this source, clearly indicated the change(s). Provide a narrative description of all features of the affected source which may affect the production of air pollutants.

3. Name(s) and maximum amount of proposed process material(s) charged per hour:

N/A

4. Name(s) and maximum amount of proposed material(s) produced per hour:

Per Unit:
0.01 lb/hr VOC
0.10 lb/hr NOx
0.08 lb/hr CO
0.01 lb/hr PM

5. Give chemical reactions, if applicable, that will be involved in the generation of air pollutants:

N/A

<sup>\*</sup> The identification number which appears here must correspond to the air pollution control device identification number appearing on the *List Form*.

<ul> <li>6. Combustion Data (if applicable): <ul> <li>(a) Type and amount in appropriate units of fuel(s) to be burned:</li> </ul> </li> <li>Natural Gas: 735.3 scf/hr</li> <li>(b) Chemical analysis of proposed fuel(s), excluding coal, including maximum percentage.</li> </ul>	ent sulfui
Natural Gas: 735.3 scf/hr  (b) Chemical analysis of proposed fuel(s), excluding coal, including maximum percentage.	ent sulfu
(b) Chemical analysis of proposed fuel(s), excluding coal, including maximum percentage.	ent sulfu
(b) Chemical analysis of proposed fuel(s), excluding coal, including maximum perceand ash:	ent sulfui
See Attachment N, Table 20.	
(c) Theoretical combustion air requirement (ACF/unit of fuel):	
© °F and	psia.
(d) Percent excess air:	
(e) Type and BTU/hr of burners and all other firing equipment planned to be used:  1.0 MMBtu/hr, each	
(f) If coal is proposed as a source of fuel, identify supplier and seams and give sizin coal as it will be fired:	g of the
(g) Proposed maximum design heat input: × 10 <sup>6</sup> BTU	J/hr.
. Projected operating schedule:	-
lours/Day 24 Days/Week 7 Weeks/Year 52	

8.	Projected amount of podevices were used:	ollutants that would be	e emitted fro	om this affected source if no contro
0	N/A	°F a	nd	psia
a.	NO <sub>X</sub>	0.10	lb/hr	grains/ACF
b.	SO <sub>2</sub>		lb/hr	grains/ACF
C.	СО	0.08	lb/hr	grains/ACF
d.	PM <sub>10</sub>	0.01	lb/hr	grains/ACF
e.	Hydrocarbons		lb/hr	grains/ACF
f.	VOCs	0.01	lb/hr	grains/ACF
g.	Pb		lb/hr	grains/ACF
h.	Specify other(s)		1	
-	Benzene	<0.0001	lb/hr	grains/ACF
_	Formaldehyde	<0.0001	lb/hr	grains/ACF
_	n-Hexane	0.002	lb/hr	grains/ACF
	Toluene	<0.0001	lb/hr	grains/ACF

NOTE: (1) An Air Pollution Control Device Sheet must be completed for any air pollution device(s) used to control emissions from this affected source.

<sup>(2)</sup> Complete the Emission Points Data Sheet.

<ol> <li>Proposed Monitoring, Recordkeeping, Rep Please propose monitoring, recordkeeping, with the proposed operating parameters. compliance with the proposed emissions lin MONITORING</li> </ol>	and reporting in order to demonstrate compliance. Please propose testing in order to demonstrate mits.
N/A	RECORDKEEPING N/A
1	
REPORTING	TESTING
N/A	N/A
MONITORING	
MONITORING. PLEASE LIST AND DESCRIBE THE PROPOSED TO BE MONITORED IN ORDER TO DEMONS PROCESS EQUIPMENT OPERATION/AIR POLLUTION (	STRATE COMPLIANCE WITH THE OPERATION OF THIS
<b>RECORDKEEPING.</b> PLEASE DESCRIBE THE PROPI MONITORING.	
<b>REPORTING.</b> PLEASE DESCRIBE THE PRORECORDKEEPING.	POSED FREQUENCY OF REPORTING OF THE
TESTING. PLEASE DESCRIBE ANY PROPOSED EMIS	SIONS TESTING FOR THIS PROCESS FOLLIPMENTALE
POLLUTION CONTROL DEVICE.	SIGNS 1231ING FOR THIS PROCESS EQUIPMENT/AIR
10. Describe all operating ranges and maintena	ance procedures required by Manufacturer to
mairitain warranty	in present to required by Marialacturer to
N/A	

To be used for affected sources other than asphalt plants, foundries, incinerators, indirect heat exchangers, and quarries.

Identification Number (as assigned on Equipment List Form): 9E

Name or type and model of proposed affected source:
One (1) HiPower PSI/GM 3.0L natural gas-fired generator (47hp)
(1) The ower 1 Shows 5.0L hattiral gas-fired generator (4/hp)
2. On a separate sheet(s), furnish a sketch(es) of this affected source. If a modification is to be
I made to this source, clearly indicated the change(s). Drovide a porretive description of
reatures of the affected source which may affect the production of air pollutants.
3. Name(s) and maximum amount of proposed process material(s) charged per hour:
27/4
N/A
4. Name(s) and maximum amount of proposed material(s) produced per hour:
Per Unit: 0.01 lb/hr VOC
0.29 lb/hr NOx
0.50 lb/hr CO
0.01 lb/hr PM
F. Characteristic at the state of the state
5. Give chemical reactions, if applicable, that will be involved in the generation of air pollutants:
N/A
IV/A

<sup>\*</sup> The identification number which appears here must correspond to the air pollution control device identification number appearing on the *List Form*.

6. Combustion Da					
(a) Type and ar	mount in	appropriate units o	f fuel(s) to be I	burned:	
Natural Gas: 8,681 B	tu/hp-hr				
(b) Chemical ar and ash:	nalysis of	proposed fuel(s), e	excluding coal,	including maxi	mum percent sulfui
See Attachment N, Ta	ible 20				
(c) Theoretical of	combustic	on air requirement	(ACF/unit of fu	el):	-
	@		°F and		psia.
(d) Percent exce	ess air:				
47 hp		urners and all othe			
(f) If coal is prop coal as it will	osed as a be fired:	a source of fuel, ide	entify supplier	and seams and	give sizing of the
(g) Proposed max	ximum de	esign heat input:			× 10 <sup>6</sup> BTU/hr.
. Projected operation	ng sched	ule:			
lours/Day 2	24	Days/Week	7	Weeks/Year	52

_	D N/A	°F a	nd	psia
a.	NO <sub>X</sub>	0.29	lb/hr	grains/ACF
b.	SO <sub>2</sub>		lb/hr	grains/ACF
C.	СО	0.50	lb/hr	grains/ACF
d.	PM <sub>10</sub>	0.01	lb/hr	grains/ACF
e.	Hydrocarbons		lb/hr	grains/ACF
f.	VOCs	0.01	lb/hr	grains/ACF
g.	Pb		lb/hr	grains/ACF
٦.	Specify other(s)			
-	Formaldehyde	0.01	lb/hr	grains/ACF
_	Acetaldehyde	0.003	lb/hr	grains/ACF
_	Acrolein	0.002	lb/hr	grains/ACF
	Methanol	0.001	lb/hr	grains/ACF

NOTE: (1) An Air Pollution Control Device Sheet must be completed for any air pollution device(s) used to control emissions from this affected source.

<sup>(2)</sup> Complete the Emission Points Data Sheet.

0.0	
<ol> <li>Proposed Monitoring, Recordkeeping, Rep Please propose monitoring, recordkeeping, with the proposed operating parameters. compliance with the proposed emissions lin MONITORING</li> </ol>	and reporting in order to demonstrate compliance Please propose testing in order to demonstrate mits.
N/A	RECORDKEEPING N/A
	N/A
PEDORTING	
REPORTING N/A	TESTING
	N/A- Engine is certified. Certificate of Conformity is included in this application.
MONITORING PLEASE LIST AND DESCRIPT	
MONITORING. PLEASE LIST AND DESCRIBE THE PROPOSED TO BE MONITORED IN ORDER TO DEMONS PROCESS EQUIPMENT OPERATION/AIR POLLUTION OF	STRATE COMPLIANCE WITH THE OPERATION OF THIS
RECORDKEEPING. PLEASE DESCRIBE THE PROPOMONITORING.	OSED RECORDKEEPING THAT WILL ACCOMPANY THE
REPORTING. PLEASE DESCRIBE THE PRO- RECORDKEEPING.	POSED FREQUENCY OF REPORTING OF THE
<b>FESTING.</b> PLEASE DESCRIBE ANY PROPOSED EMISPOLLUTION CONTROL DEVICE.	
0. Describe all operating ranges and maintena	ance procedures required by Manufacturer to
naintain warranty N/A	, ,
• • • • • • • • • • • • • • • • • • • •	
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#### **RENTAL** Gaseous Generator Set

#### Model: HRGM 30 T6

#### Specification & Application Data

#### **GM Vortec Series**



Photo may depict optional equipment.

#### Description

HIPOWER<sup>®</sup> rental generators are an efficient, reliable and versatile source of mobile electrical power. They are designed to operate in the most extreme working conditions. All HIPOWER<sup>®</sup> Gaseous Rental Generators have a unique combination of innovative design and the use of high quality materials that provide the user with the most dependable power that you can rely on for non-stop power with easy to operate controls.

The generator set is powered by a radiator-cooled, industrial GM Vortec gaseous engine, which meets current Environmental Protection Agency (EPA) non-road exhaust emission regulations, driving a single bearing, four-pole, three-phase alternator, with IP23 protection. The Prime Power kVA rating for generator set is given with a 125 degree C alternator winding temperature rise.

#### HIPOWER® Features and Benefits

**GM Vortec Engine:** Long-life, heavy-duty, 4-cycle, gaseous engine from a world renown manufacturer for economy of operation and maximum reliability and durability. Capable of full rated load acceptance in one step.

Cooling: Radiator with belt driven pusher fan.

Filtration: Heavy-duty replaceable element air-cleaner.

Alternator: Single bearing, rotating field, self-excited, self-ventilated, 12-wire re-connectable, 60Hz brushless alternator with permanent magnetic generator (PMG) for reduced service and maintenance requirements, with Class H insulation. Automatic voltage regulator (AVR) providing close voltage regulation. Has a high skVA starting capability for electric motor loads.

Arrangement: Engine and alternator units are closed coupled together and with mobile style anti-vibration isolators, mounted between the assembly and a heavy-duty steel base. The sturdy base frame has openings allowing for winching, slinging and forklift pockets for ease of handling

#### 60Hz Prime Power Ratings kW & kVA

Voltage VAC	Phase	DE	Phase PF	L	LPG		NG	
vortage vac	Filase	1,1,1	kW	kVA	kW	kVA		
120/240	1	0.8	15.6	19.5	14.3	17.9		
120/208	3	0.8	24.0	30.0	22.0	27.5		
120/240 Delta	3	0.8	N.A	N.A	N.A	N.A		
277/480	3	0.8	24.0	30.0	22.0	27.5		
347/600	3	0.8	24.0	30.0	22.0	27.5		

Rating Definitions: (N.A. = Not available for model designated)
Prime - All Rental Sets are Prime Rated - Prime rating is applicable
for supplying power to a varying load in lieu of utility for an unlimited
amount of running of amount of running time. (Max. load factor = 80%)
A 10% overload capacity is available for 1 out of every 12 hours.

#### HIPOWER® Features and Benefits

Enclosure: Fully sound attenuated enclosure, fabricated in 11-gauge steel, powder coated with finish that exceeds 1000-hr salt spray test, curved edges, minimum outside fasteners.

Ample layer of durable sound insulating material placed all around the inside of the container, doors and ducting with metal retainer frames. Can be cleaned by high-pressure water and is oil and fire resistant.

Vertical air discharge for quiet operation.

Wide steel lockable access doors with rubber seals, for easy entrance of all maintenance personnel and any necessary service by technicians, with stainless steel hinges, hardware and fasteners resistant to corrosion.

**Exhaust:** Effective low noise, steel residential-type exhaust silencer and catalytic converter with rain cap

**Controls:** Digital control panel to operate all manual and automatic start and stop features. Many programmable automatic functions for local and remote controls with LED lights, tamper proof engine hour recorder with analog meters: voltmeter & switch, three (3) ammeters, Hz meter, fuel gauge and battery charger.

#### HIPOWER® Rental Options

Voltage Selector Switch: Three-position, manual voltage selector switch. Lockable in three positions for switching set between 120/240V single phase and 120/208 and 277/480V 3-phase. - NOT AVAILABLE AT 600V CONNECTION.

**Power Distribution:** Consult HIPOWER® regarding the comprehensive range of power distribution accessoires available.

Oil field heavy duty rental skid: Heavy duty sub base

(See page 3 for additional options)





#### Application & Specification Data

LPG/NG Rental Generator Set Model: HRGM 30 T6 **PSI - GM Vortec** 

#### **Gaseous Generator Set Specification:**

Governor regulation class	ISO 8528 Part 1 Class G3	
Voltage regulation, no load to full load	plus or minus 1%	
Frequency regulation	Ischronous	
Radio frequency emissions compliance	Meets requirements of most industrial and commercial applications	
skVA at 480 volts with 30% voltage dip	76	
Main Line Circuit breaker – amps capacity	105	
ENGINE		

Manufacturer	PSI-General Motors
Model	
EPA certified	Vortec 3.0L
Crankshaft speed	Yes
	1,800rpm
Туре	LPG/NG fueled, 4-stroke
Ignition	Spark Plug
Aspiration	Natural
Number of Cylinders	4
Cylinder arrangement	In-line
Displacement CID (liters)	181 (3.0)
Bore and Stroke ins (mm)	4 x 3.6 (10.2 x 9.1)
Nominal power	LPG 48 hp NG 47 hp
Cooling	Liquid
Governor	Electronic
Starting motor & alternator	12 volt
Compression ratio	9.3:1
Air cleaner type	Dry, replacable cartridge
xhaust gas flow at full output lb/hr (kg/hr)	250 (7.1)
xhaust temperature at full load - dry exhaust °F ( °C)	1056 (569)
Maximum permitted back pressure - in. HG (kPa)	3.0 (10.2)

#### **Cooling System:**

Radiator- cooled cooling air flow - cu. ft./min. (cu. m/min.)	2500 (72)
Alternator cooling flow - cu. ft./min. (cu. m/min.)	250 (4.5)
Combustion air - cu. ft./min. (cu. m/min.)	64 (1.8)
Total cooling air flow (engine + alternator + combustion)	2814 (78.3)
Radiator system capacity, including engine - gallons (L)	5.0 (18.9)
Lubrication system:	

Oil pan capacity - quarts (L)	4.0 (3.8)
Oil pan capacity with filter - quarts (L)	4.3 (4.1)
Oil filter - quantity and type	1, Replaceable Spin-On
Recommended lubricating oil grade - above 0 ° F (below 0 ° F)	
Oil consumption at full load	Less than 0.1% of fuel consumption
Oil pressure – psi (bars)	46.0 (320.0)
Engine Flectrical System:	10.0 (020.0)

#### **Engine Electrical System:**

Starting motor voltage	12 volt	
Battery - AH	1, size BC I# 24F	
Maximum battery charge alternator output - amps	70	
Cold Cranking Amps - minimum	600	
	-	

The state of the s	11 G.	Model - AT1
Noise level - dBA at 23 feet (7 meters)	74	
Dimensions - inches	82 x 36 x 47	
Dry weight – lbs.	1,617	
Fuel System: (*Massured at any		

Fuel System: (\*Measured at gen-set fuel inlet, downstream of any dry fuel or filter accessories.)

- downstream or any dry fuel or filter accessories.)		
Fuel type	LPG or Natural Gas, vapor withdrawl	
Fuel supply line - inlet	1" NPTF	
*Natural gas and LPG fuel supply pressure - in. column H <sub>2</sub> O (kPa)	7" - 11" (1.74 - 2.74)	
Prime Rating Fuel consumentians		

Prime Rating Fuel consumption:

LPG - cu. ft./hour (kg/hour) at 100% standby rating	168 (4.8)
Natural Gas - cu. ft./hour (kg/hour) at 100% standby rating	400 (11.3)
Alternator Specification	

**Alternator Specification:** 

Manufacturer		Stamford
Alternator model, winding & AVR model	127/208; 277/480 volts	PI 144 H
	600 volts	PI 144 H
Voltages		3-phase 120/208, 277/480, 347/600
Alternator Type		4-pole, rotating field
Excitation System		Brushless with EBS/AS480 AVR
Power factor		0.8
Number of leads		12
Stator Pitch		2/3
Insulation		Class H
Windings – Temperature Rise		120° C
Enclosure (IEC-34-S)		IP 23
Bearing		Single, sealed
Coupling		Flexible disc
Amortisseur windings		Full
Voltage regulation – no load to full load with MX341 AVR		plus or minus 1%
TIF		< 50
Line harmonics		5% maximum

#### Standard Accessories: (see back-page for control panel details)

Radiator with pusher fan	All rotating components (i.e. fan) protected with metal guards	
Dry air cleaner		
<ul> <li>Heavy-duty engine start batteries in rack with cables</li> </ul>	All hot components (i.e. exhaust) protected with metal guards     Ground composition recovered to	
Emergency stop switch	Ground connection prepared for ground spike (not supplied)     Main line ARR III (to be for ground spike)	
Control Panel DSE7310 (See over for details)	Main line ABB UL listed circuit breaker for overload protection	
Two dry contacts for auto-start	Operation and installation literature     CSA certified	
<ul> <li>Steel base for mounting on firm surface such as concrete</li> </ul>		
Optional Accessories:	Control panel DSE 7310 MANUAL & AUTO START MODULE	

#### **Optional Accessories:**

Distribution power panel to	
□ DOT certified towing trailer	☐ Oil Make-up system
☐ Snow hoods for air intake and exhaust	☐ Oil fiels heavy duty rental skid
	Control patier fleater
☐ Electric actuator and louvers for air intake and exhaust	☐ Control panel heater
☐ Winterization kit for low ambient temperature	☐ Engine Block heater
[7] Winterination Lit 6 I	- Store power receptacie
☐ Alternator anti-condensation heaters	☐ Shore power receptacle
Rotary voltage selector switch (not available with 600V connection)	☐ Interior lights

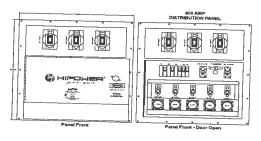
#### Distribution power panel \*See image RH back-page

Aluminum 0.090" enclosure black powder coated - covered panel NEMA 3R/IP67rated weather proof assembly - Individual Square-D QOU branch breakers - 2 x 20A 125V NEMA 5-20 GFCI duplex receptacles - 3 x 50A 125/250V CS6369 Twist -lock receptacles & Lexan covers - 50A California Style twist lock (1 $\Phi$  only) - 1 set Camlock devices rated 400A - Color coded Camlock devices 3 $\Phi$  - 5W black, red, blue, white & green - Pad lockable 1/4 turn door access with cable trap - Auxiliary bus bars with mechanical lugs - Mechanical lugs up to 250MCM cable

HIPOWER® DSE 7310 Control Panel: The DSE model 7310 digital control panel is back-lit with icon LCD text display, and is PC configurable. It works with the engine electronic governor with PLC functionality, protected front panel editing, and includes: manual, automatic and remote (input) start, PC configurable six inputs and four outputs, configurable timers and alarms, generator voltage and Hz display, battery voltage display, engine speed display, multiple engine parameters are monitored simultaneously, comprehensive shutdown or warning on fault condition, engine preheat, LED and LCD alarm indication, tamper-proof hour counter provides accurate information for monitoring and maintenance periods. The module monitors: engine speed, frequency, voltage and engine run hours and also displays the warning and shutdown status

Engine alarms included: High coolant temperature, low oil pressure, low coolant level, unexpected shutdown, low fuel level, stop failure, low battery voltage, battery charging alternator failure, over-speed, under-speed, start failure and emergency stop.





Alternator alarms included: Overload, unbalanced voltage, over voltage, under voltage, over frequency,

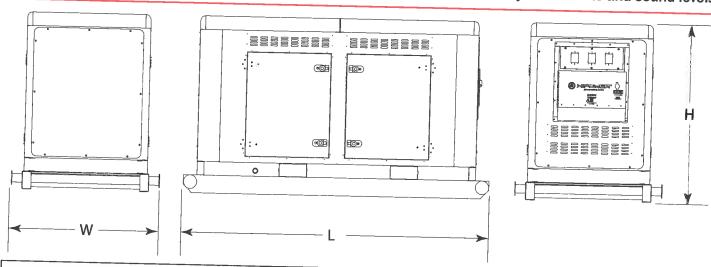
under frequency, short circuit, reverse power, and incorrect phase sequence.

Instrumentation and gauges included: 3 ammeters, frequency meter, voltmeter plus selector, hour meter, fuel gauge, battery charger gauge, oil pressure gauge, water temperature gauge, siren and emergency stop button.

Pictures of Control Panel RH and Distribution Panel LH may include optional equipment and/or accessories

#### Model HRGM 30 T6

#### key dimensions and sound levels



Generator Data (L, W & H dimensions in inches)						
Configuration	L =Length	W = Width	H = Height	Net Weight lbs	dBA	
Enclosed	82"	36"	47"	1525	73	
Enclosed (with oil field heavy dury rental skid)	90"	43.5"	52.5"	1917	73	
* All measurements are approximate and for estimation purposes only. Sound levels measured at 23ft (7m) and does not account for ambient site and the						

<sup>\*</sup> All measurements are approximate and for estimation purposes only. Sound levels measured at 23ft (7m) and does not account for ambient site conditions.

#### Codes and Standards Compliances used where applicable













NFPA 99 **NFPA 110** ISO 8528-5 ISO 1708A.5 ISO 3046

BS5514 SAE J1349 DIN6271 IEE C62.41 TESTING NEMA ICS 1

your partner for power

Ref# 777-10030R-August 2013

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# UNITED STATES ENVIRONMENTAL PROTECTION AGENCY 2015 MODEL YEAR CERTIFICATE OF CONFORMITY WITH THE CLEAN AIR ACT

OFFICE OF TRANSPORTATION AND AIR QUALITY ANN ARBOR, MICHIGAN 48105

Certificate Issued To: Power Solutions International, Inc.	(U.S. Manufacturer or Importer)	Certificate Number: FPSIB2.97GLP-001
Certificate Issued		Certificate Numb

Seturer. Dower Colutions International Inc

Expiration Date: 12/31/2015

Issue Date: 10/06/2014 Revision Date: N/A

> Byron J. Bunker, Division Director Compliance Division

> > Manufacturer: Power Solutions International, Inc. Engine Family: FPSIB2.97GLP

Certification Type: Mobile and Stationary
Fuel: Gasoline (up to and including 10% Ethanol)

Natural Gas (CNG/LNG)
LPG/Propane

Emission Standards: HC + NOx (g/kW-hr): 2.7 CO (g/kW-hr): 4.4 NMHC + NOx (g/kW-hr): 2.7CO (g/kW-hr): 4.4

NMHC + NOX (g/kW-hr): 2.7CO (HC + NOX (g/kW-hr): 2.7 NMHC + NOX (g/kW-hr): 2.7

Emergency Use Only: N

conditions prescribed in those provisions, this certificate of conformity is hereby issued with respect to the test engines which have been found to conform to applicable requirements and which represent the Pursuant to Section 213 of the Clean Air Act (42 U.S.C. section 7547) and 40 CFR Part 1048, 1065, 1068, and 60 (stationary only and combined stationary and mobile) and subject to the terms and following nonroad engines, by engine family, more fully described in the documentation required by 40 CFR Part 1048 and produced in the stated model year.

documentation required by 40 CFR Part 1048 and which are produced during the model year stated on this certificate of the said manufacturer, as defined in 40 CFR Part 1048. This certificate of conformity This certificate of conformity covers only those new nonroad spark-ignition engines which conform in all material respects to the design specifications that applied to those engines described in the does not cover nonroad engines imported prior to the effective date of the certificate.

warrant or court order may lead to revocation or suspension of this certificate for reasons specified in 40 CFR Part 1048. It is also a term of this certificate that this certificate may be revoked or suspended or It is a term of this certificate that the manufacturer shall consent to all inspections described in 40 CFR 1068.20 and authorized in a warrant or court order. Failure to comply with the requirements of such a rendered void ab initio for other reasons specified in 40 CFR Part 1048.

This certificate does not cover large nonroad engines sold, offered for sale, or introduced, or delivered for introduction, into commerce in the U.S. prior to the effective date of the certificate.

To be used for affected sources other than asphalt plants, foundries, incinerators, indirect heat exchangers, and quarries.

Identification Number (as assigned on *Equipment List Form*): 11E

Name or type and model of proposed affected source:
One (1) Condensate Stabilizer Heater
<ol> <li>On a separate sheet(s), furnish a sketch(es) of this affected source. If a modification is to be made to this source, clearly indicated the change(s). Provide a narrative description of all features of the affected source which may affect the production of air pollutants.</li> </ol>
3. Name(s) and maximum amount of proposed process material(s) charged per hour:
N/A
4. Name(s) and maximum amount of proposed material(s) produced per hour:
Per Unit:
0.004 lb/hr VOC
0.07 lb/hr NOx
0.06 lb/hr CO
0.01 lb/hr PM
5. Give chemical reactions, if applicable, that will be involved in the generation of air pollutants:
N/A
14/11

<sup>\*</sup> The identification number which appears here must correspond to the air pollution control device identification number appearing on the *List Form*.

_			="-		
6.	Combustion Data (if app	licable):			
	(a) Type and amount in	appropriate units	of fuel(s) to be b	urned:	
N	atural Gas: 735.3 scf/hr				
	(b) Chemical analysis of	proposed fuel(s),	excluding coal, i	ncluding maxin	num percent sulfur
Se	and ash: e Attachment N, Table 20.				
	(c) Theoretical combustion	on air requirement	t (ACF/unit of fue	el):	
	@		°F and		psia.
	(d) Percent excess air:				
	(e) Type and BTU/hr of b	umers and all oth	er firing equipme	ent planned to	be used:
0.7	5 MMBtu/hr				
1	f) If coal is proposed as coal as it will be fired:	a source of fuel, i	dentify supplier a	and seams and	give sizing of the
(	g) Proposed maximum d	esign heat input:			× 10 <sup>6</sup> BTU/hr.
7.	Projected operating sched	lule:			
lou	rs/Day 24	Days/Week	7	Weeks/Year	52

8.	Projected amount of pollutants that would be emitted from this affected source if no control devices were used:					
@	N/A	°F an	d	psia		
a.	NO <sub>X</sub>	0.07	lb/hr	grains/ACF		
b.	SO <sub>2</sub>		lb/hr	grains/ACF		
c.	СО	0.06	lb/hr	grains/ACF		
d.	PM <sub>10</sub>	0.01	lb/hr	grains/ACF		
e.	Hydrocarbons		lb/hr	grains/ACF		
f.	VOCs	0.004	lb/hr	grains/ACF		
g.	Pb		lb/hr	grains/ACF		
h.	Specify other(s)		ı			
	Benzene	<0.0001	lb/hr	grains/ACF		
	Formaldehyde	<0.0001	lb/hr	grains/ACF		
	n-Hexane	0.001	lb/hr	grains/ACF		
	Toluene	<0.0001	lb/hr	grains/ACF		

NOTE: (1) An Air Pollution Control Device Sheet must be completed for any air pollution device(s) used to control emissions from this affected source.

(2) Complete the Emission Points Data Sheet.

compliance with the proposed emissions lin	and reporting in order to demonstrate compliance.  Please propose testing in order to demonstrate
MONITORING N/A	RECORDKEEPING N/A
REPORTING N/A	TESTING N/A
MONITORING. PLEASE LIST AND DESCRIBE THE PROPOSED TO BE MONITORED IN ORDER TO DEMONITORESS EQUIPMENT OPERATION/AIR POLLUTION OF THE PROPERTY O	E PROCESS PARAMETERS AND RANGES THAT ARE STRATE COMPLIANCE WITH THE OPERATION OF THIS CONTROL DEVICE
<b>RECORDKEEPING.</b> PLEASE DESCRIBE THE PROP MONITORING.	
<b>REPORTING.</b> PLEASE DESCRIBE THE PRORECORDKEEPING.	POSED FREQUENCY OF REPORTING OF THE
TESTING. PLEASE DESCRIBE ANY PROPOSED EMIS POLLUTION CONTROL DEVICE.	1
10. Describe all operating ranges and mainten maintain warranty N/A	ance procedures required by Manufacturer to
	-

# Attachment L EMISSIONS UNIT DATA SHEET BULK LIQUID TRANSFER OPERATIONS

Furnish the following information for each new or modified bulk liquid transfer area or loading rack, as shown on the *Equipment List Form* and other parts of this application. This form is to be used for bulk liquid transfer operations such as to and from drums, marine vessels, rail tank cars, and tank trucks.

Identification No	umber (as assigne	ed on Equipment	List Form):	<u> </u>			
1. Loading Area Name: 12E, 13E							
2. Type of cargo as apply):	11 07						
□ Drums	☐ Marine Vesse	els 🗆 R	ail Tank Cars	☑ Tank Trucks			
3. Loading Racl	k or Transfer Poin	t Data:					
Number of pu	ımps	2					
Number of liq	luids loaded	2 - Conde	ensate, Produced Wa	ater			
Maximum number of marine 1 vessels, tank trucks, tank cars, and/or drums loading at one time							
4. Does ballasti □ Yes	ing of marine vess □ No		oading area? oes not apply				
transfer point:	aning location, cor	mpounds and pro	cedure for cargo v	essels using this			
N/A							
6. Are cargo vessels pressure tested for leaks at this or any other location?  ☐ Yes ☑ No  If YES, describe:							
7. Projected Maximum Operating Schedule (for rack or transfer point as a whole):							
Maximum	Jan Mar.	Apr June	July - Sept.	Oct Dec.			
hours/day	1	1	1	1			
days/week	7	7	7	7			

weeks/quarter	13	13	13	13	7
---------------	----	----	----	----	---

0 5 11 11							
8. Bulk Liq	uid Data (add pages as	necessar	<i>y):</i>				
Pump ID No		1	2				
Liquid Name		Condensate	Produced Water				
Max. daily th	roughput (1000 gal/day)	8,000 gal/hr	8,000 gal/hr				
Max. annual	throughput (1000 gal/yr)	766.5	3,832.5				
Loading Met	nod <sup>1</sup>	SUB	SUB				
Max. Fill Rate	e (gal/min)	133.3	133.3				
Average Fill	Time (min/loading)	60	60				
Max. Bulk Liquid Temperature (°F)		55	55				
True Vapor Pressure <sup>2</sup>		8.46	8.46				
Cargo Vessel Condition <sup>3</sup>		U	U				
Control Equip	ment or Method 4	N/A	N/A				
Minimum con	trol efficiency (%)						
Maximum Emission	Loading (lb/hr)	58.95	0.59				
Rate	Annual (lb/yr)	5,647.99	282.40				
Estimation Me	ethod <sup>5</sup>	EPA	EPA	,			
<sup>1</sup> BF = Bottom	Fill SP = Splash Fill	SUB :	= Submerg	ed Fill			
<sup>2</sup> At maximum	bulk liquid temperature				<u> </u>	<u> </u>	
		= Unclean	ed (dedica	ted servi	ico) O -	- other (	dogorih o)
<sup>3</sup> B = Ballasted Vessel, C = Cleaned, U = Uncleaned (dedicated service), O = other (describe) <sup>4</sup> List as many as apply (complete and submit appropriate <i>Air Pollution Control Device Sheets</i> ):CA = Carbon Adsorption  LOA = Lean Oil AdsorptionCO = Condensation  SC = Scrubber (Absorption)CRA = Compressor-Refrigeration-Absorption  TO = Thermal Oxidation or Incineration  CRC = Compression-Refrigeration-Condensation  VB = Dedicated Vapor Balance (closed system)  O = other (descibe)							
<sup>5</sup> EPA = EPA MB = Materia	Emission Factor as stated al Balance	in AP-42					

TM = Test Measurement based upon test data submittal O = other (describe)

#### 9. Proposed Monitoring, Recordkeeping, Reporting, and Testing

Please propose monitoring, recordkeeping, and reporting in order to demonstrate compliance with the proposed operating parameters. Please propose testing in order to demonstrate compliance with the proposed emissions limits.

RECORDKEEPING
Ascent will keep records of loading volumes to ensure emissions do not exceed those listed in this application.
TESTING
N/A

**MONITORING.** PLEASE LIST AND DESCRIBE THE PROCESS PARAMETERS AND RANGES THAT ARE PROPOSED TO BE MONITORED IN ORDER TO DEMONSTRATE COMPLIANCE WITH THE OPERATION OF THIS PROCESS EQUIPMENT OPERATION/AIR POLLUTION CONTROL DEVICE.

**RECORDKEEPING.** PLEASE DESCRIBE THE PROPOSED RECORDKEEPING THAT WILL ACCOMPANY THE MONITORING.

**REPORTING.** PLEASE DESCRIBE THE PROPOSED FREQUENCY OF REPORTING OF THE RECORDKEEPING.

**TESTING.** PLEASE DESCRIBE ANY PROPOSED EMISSIONS TESTING FOR THIS PROCESS EQUIPMENT/AIR POLLUTION CONTROL DEVICE.

10. Describe all operating ranges and maintenance procedures required by Manufacturer to maintain warranty

N/A

# Attachment L EMISSIONS UNIT DATA SHEET CHEMICAL PROCESS

Fo su	or chemical processes please fill out pplementary forms that have been	this sheet and all supplementary forms completed.	(see below) that apply. Please check all				
	Emergency Vent Summary Sheet						
1.	Chemical process area name and Sitewide Fugitives (14E)	d equipment ID number (as shown in <i>E</i>	quipment List Form)				
2.	Standard Industrial Classification 1311	Codes (SICs) for process(es)					
3.	List raw materials and ☐ attach N/A- fugitive gas emissions only	MSDSs					
4	1112 de la companya del companya de la companya del companya de la						
	List Products and Maximum Produ		1				
Des	scription and CAS Number	Maximum Hourly (lb/hr)	Maximum Annual (ton/year)				
5.	Complete the Emergency Vent St	ummary Sheet for all emergency relief of	devices.				
6.							
7.	Clearly describe below or attach to spill or release.	application Accident Procedures to be	followed in the event of an accidental				
	Ascent will repair and report any accident	dental reslease as soon as possible following	ng the incident.				

chemical entity sheet is not it teratogenicity, unknown, and 8B. Describe any I	SA. Complete the <i>Toxicology Data Sheet</i> or attach to application a toxicology report (an up-to-date material safety data sheets (MSDS) may be used) outlining the currently known acute and chronic health effects of each compound or chemical entity emitted to the air. If these compounds have already been listed in Item 3, then a duplicate MSDS sheet is not required. Include data such as the OSHA time weighted average (TWA) or mutagenicity, teratogenicity, irritation, and other known or suspected effects should be addressed. Indicate where these are unknown, and provide references.  3B. Describe any health effects testing or epidemiological studies on these compounds that are being or may be conducted by the company or required under TSCA, RCRA or other federal regulations. Discuss the persistence							
in the environn	nent of any emission (e.g. pe	esticides, etc.).						
Hazardous Wa	iste Section of WVDEP, OA		CSR25, please contact the					
	ounts of wastes to be dispos							
Carrier:	osal and location of waste d	Phone:						
		ardous Waste Landfill will be used						
10. Maximum and		Schedule for process or project as a who	ole (circle appropriate units).					
circle units:	(hrs/day) (hr/batch)	(days), (batches/day), (batches/week)	(days/yr), (weeks/year)					
10A. Maximum	24 hrs/day	7 days/week	52 weeks/year					
10B. Typical	24 hrs/day	7 days/week	52 weeks/year					
		eactor in this chemical process.						
		for each distillation column in this chem	ical process.					
13. Proposed Monitoring, Recordkeeping, Reporting, and Testing Please propose monitoring, recordkeeping, and reporting in order to demonstrate compliance with the proposed operating parameters. Please propose testing in order to demonstrate compliance with the proposed emissions limits. MONITORING Ascent staff will perform AVO walkthroughs during site visits, expected to be at least weekly. RECORDKEEPING Ascent staff will note any detected leaks and the repairs done to repair them.								
REPORTING		TESTING						
In the case of a reportable event, Ascent will contact the WV DEP and comply with any applicable requirements.								
MONITORING. Please list and describe the process parameters and ranges that are proposed to be monitored in								
order to demonstrate compliance with the operation of this process equipment operation or air pollution control device.  RECORDKEEPING. Please describe the proposed recordkeeping that will accompany the monitoring.								
REPORTING. Pleas	REPORTING. Please describe the proposed frequency of reporting of the recordkeeping.							
<b>FESTING.</b> Please describe any proposed emissions testing for this process equipment or air pollution control device.								
Describe all operating ranges and maintenance procedures required by Manufacturer to maintain warranty     N/A								

#### INFORMATION REQUIRED FOR CHEMICAL PROCESSES

The notes listed below for chemical processes are intended to help the applicant submit a complete application to the OAQ; these notes are not intended to be all inclusive. The requirements for a complete application for a permit issued under 45CSR13 are designed to provided enough information for a permit reviewer to begin a technical review. Additional information beyond that identified may be required to complete the technical review of any individual application.

#### **Process Description**

Please keep these points in mind when completing your process description as part of this permit application.

- Provide a general process overview. This brief, but complete, process description should include chemical or registered trademark names of chemical products, intermediates, and/or raw materials to be produced or consumed, and the ultimate use(s) of the product(s). A list of the various chemical compounds is helpful.
- Describe <u>each process step</u>. Include the process chemistry and stoichiometrically balanced reaction equation or material mass balance on all components.
- 3. Describe the methods and equipment used to receive, store, handle, and charge raw materials.
- 4. Describe the methods and equipment used to handle, store, or package final products and intermediates.
- 5. Provide process flow diagrams or equipment layout drawings which clearly show the process flow relationships among all pieces of process and control equipment. Identify all air emission discharge points. Discuss instrumentation and controls for the process.
- 6. Discuss the possibilities of process upsets, the duration and frequency of upsets, and consequences (including air emissions) of these upsets. Include a description of rupture discs, pressure relief valves, and secondary containment systems.
- 7. Discuss any fugitive emissions and the methods used to minimize them.
- 8. Include the following plans for the process if available:
  - a. preventative maintenance and malfunction abatement plan (recommended for all control equipment).
  - b. continuous emissions (in-stack) monitoring plan
  - c. ambient monitoring plan
  - d. emergency response plan

#### **Regulatory Discussion**

The following state and federal air pollution control regulations may be applicable to your chemical process. You should review these regulations carefully to determine if they apply to your process. Please summarize the results of your review in your permit application along with any other regulations you believe are applicable.

- Title 45 Legislative Rule Division of Environmental Protection, Office of Air Quality contains West Virginia's air pollution control regulations, including the following promulgated rules which may require emissions reductions or control technologies for your chemical process:
  - a. 45CSR27 Best Available Technology (BAT) for Toxic Air Pollutants (TAPs)
  - 45CSR21 VOC emissions controls for ozoné maintenance in Kanawha, Cabell, Putnam, Wayne, and Wood counties.
  - c. 45CSR13 (Table 45-13A) plantwide emission thresholds for permitting for certain pollutants.
- Federal Guidelines for case-by-case MACT determinations under section 112(g) of the 1990 CAAA for individual and total HAPs greater than 10 and 25 tons per year, respectively.
- There are also subparts of the federal Standards of Performance for New Stationary Sources (NSPS), 40CFR60 60, and the National Emission Standards for Hazardous Air Pollutants (NESHAP) at 40CFR61 and 40CFR63, which apply to various chemical and nonchemical processes. These subparts are too numerous to list here, but these areas of the federal regulations should be consulted carefully to determine applicability to your process.

#### **Emissions Summary and Calculations**

Please keep these points in mind when submitting your emissions calculations as part of this permit application.

- 1. For each pollutant, provide the basis for the emissions estimate and for all emission reduction(s) or control efficiency(ies) claimed.
- 2. For all batch processes provide the following
  - a. Emissions of each pollutant in pound(s) per batch, from each process step
  - b. Annual emissions based on number of batches requested per year
  - c. The total time for each process step and the duration of the emissions during the process step
  - d. Total batch time, total emissions per batch (or per day), and annual emissions based on the number of batches requested per year.

#### **EMERGENCY VENT SUMMARY SHEET**

List below all emergency relief devices, rupture disks, safety relief valves, and similar openings that will vent only under abnormal conditions.

	I	T		
Emission Point ID¹	Equipment to Relief Vent (type, ID if available) <sup>2</sup>	Relief Vents (type) & Set Pressure (psig)	Name of Chemical(s) or Pollutants Controlled	Worst Case Emission per Release Event (lbs)
N/A				
			<u> </u>	
			-	
				<u> </u>
	<u> </u>			
	]			

All routine vents (non-emergency) should be listed on the Emission Points Data Summary Sheet.

<sup>&</sup>lt;sup>1</sup> Indicate the emission point, if any, to which source equipment normally vents. Do <u>not</u> assign emission point ID numbers to each emergency relief vent or device.

<sup>&</sup>lt;sup>2</sup> List all emergency relief devices next to the piece of equipment from which they control releases.

# LEAK SOURCE DATA SHEET

Source Category	Pollutant	Number of Source Components¹	Number of Components Monitored by Frequency <sup>2</sup>	Average Time to Repair (days) <sup>3</sup>	Estimated Annual
Pumps <sup>5</sup>	light liquid VOC <sup>6,7</sup>			(26-2)	Limpolou Ivare (19/91)
	heavy liquid VOC <sup>8</sup>				
	Non-VOC9				
Valves <sup>10</sup>	Gas VOC	200	0	7	2.784
	Light Liquid VOC	200	0	7	9,636
	Heavy Liquid VOC				
	Non-VOC				
Safety Relief Valves <sup>11</sup>	Gas VOC	35	0	7	2.713
	Non VOC				
Open-ended Lines <sup>12</sup>	VOC				
	Non-VOC				
Sampling Connections <sup>13</sup>	VOC	1,300	0	7	7 577
	Non-VOC				7,724
Compressors	VOC				
	Non-VOC				
Flanges	VOC	725	0	7	808
	Non-VOC				
Other	VOC				
	Non-VOC				

1-13 See notes on the following page.

#### **Notes for Leak Source Data Sheet**

- For VOC sources include components on streams and equipment that contain greater than 10% w/w VOC, including feed streams, reaction/separation facilities, and product/by-product delivery lines. Do not include certain leakless equipment as defined below by category.
- 2. By monitoring frequency, give the number of sources routinely monitored for leaks, using a portable detection device that measures concentration in ppm. Do not include monitoring by visual or soap-bubble leak detection methods. "M/Q(M)/Q/SA/A/O" means the time period between inspections as follows:

Monthly/Quarterly, with Monthly follow-up of repaired leakers/Quarterly/Semi-annual/Annually/Other (specify time period)

If source category is not monitored, a single zero in the space will suffice. For example, if 50 gas-service valves are monitored quarterly, with monthly follow-up of those repaired, 75 are monitored semi-annually, and 50 are checked bimonthly (alternate months), with non checked at any other frequency, you would put in the category "valves, gas service:" 0/50/0/75/0/50 (bimonthly).

- 3. Give the average number of days, after a leak is discovered, that an attempt will be made to repair the leak.
- 4. Note the method used: MB material balance; EE engineering estimate; EPA emission factors established by EPA (cite document used); O other method, such as in-house emission factor (specify).
- Do not include in the equipment count sealless pumps (canned motor or diaphragm) or those with enclosed venting to a control device. (Emissions from vented equipment should be included in the estimates given in the Emission Points Data Sheet.)
- 6. Volatile organic compounds (VOC) means the term as defined in 40 CFR □51.100 (s).
- 7. A light liquid is defined as a fluid with vapor pressure equal to or greater than 0.04 psi (0.3 Kpa) at 20°C. For mixtures, if 20% w/w or more of the stream is composed of fluids with vapor pressures greater than 0.04 psi (0.3 Kpa) at 20 °C, then the fluid is defined as a light liquid.
- 8. A heavy liquid is defined as a fluid with a vapor pressure less than 0.04 psi (0.3 Kpa) at 20°C. For mixtures, if less than 20% w/w of the stream is composed of fluids with vapor pressures greater than 0.04 psi (0.3 Kpa) at 20°C, then the fluid is defined as a heavy liquid.
- 9. LIST CO, H<sub>2</sub>S, mineral acids, NO, NO<sub>2</sub>, SO<sub>3</sub>, etc. DO NOT LIST CO<sub>2</sub>, H<sub>2</sub>, H<sub>2</sub>O, N<sub>2</sub>, O<sub>2</sub>, and Noble Gases.
- 10. Include all process valves whether in-line or on an open-ended line such as sample, drain and purge valves. Do not include safety-relief valves, or leakless valves such as check, diaphragm, and bellows seal valves.
- 11. Do not include a safety-relief valve if there is a rupture disk in place upstream of the valve, or if the valve vents to a control device.
- 12 Open-ended lines include purge, drain and vent lines. Do not include sampling connections, or lines sealed by plugs, caps, blinds or second valves.
- 13. Do not include closed-purge sampling connections.

# TOXICOLOGY DATA SHEET

			£ - 7 4			
Descriptor Name/CAS	OSHA Limits <sup>2</sup>	Limits <sup>2</sup>	TCto - Animal		,	
Number	TWA	ر ا	LC <sub>LO</sub> - Animal LC <sub>50</sub> - Animal	Chronic <sup>4</sup>	rritation <sup>5</sup>	References
N/A						

<sup>&</sup>lt;sup>1</sup> Indicate by "ND" where no data exists, in company's knowledge. <sup>2</sup> Time Weighted Average, Ceiling Limit, or other, with units. <sup>3</sup> If inhalation data is not available, provide other data as available.

<sup>&</sup>lt;sup>4</sup> Relying on animal or human studies, indicate if any data suggests: C = carcinogenicity, M = mutagenicity, T = teratogenecity, O = oncogenicity, I had it there are dermal or eye irritation effects and whether they are considered to be low, moderate, or severe.

#### **REACTOR DATA SHEET**

Provide the following information for <u>each</u> piece of equipment that is a potential or actual source of emissions as shown on the *Equipment List Form* and other parts of application.

Identification Number	er (as shown o	on <i>Equipment List Fo</i>	orm):					
1. Name and type	Name and type of equipment (e.g. CSTR, plug flow, batch, etc.)							
2. Type of operation	n Ba	atch [	☐ Continuous			☐ Semi-batch		
3. Projected Actual Equipment Operating Schedule (complete appropriate line								
hrs/day		days/v	veek			weeks/	year	
hrs/batch			es/day, weeks e one)	S		day,we (Circle		
4. Feed Data	Flow in =	g	al/hr, or gal/b	patch				
Material Name & CAS No.	Phasea	Specific Gravity	Vapor Pressure <sup>b</sup>	C Normal	harge Ra Max	te Units	Fill Time (min/batch, run) <sup>c</sup>	
5. Provide all chem	s juipment is filli ical reaction y occur as wel	ing per batch or run ( s that will be involve Il as gases that may b	d (if applicab	ole), includ	ina the r	esidence t	ime and any side	

C Mandanian T				T					
6. Maximum Temperato	ıre				eximum Press ex. Set Pressu		enting		
·	°C				mm	Hg			mmHg
°F					psig		psig		
8. Output Data Flow	Out =				gal/hr or gal	/batch			
Material Name and CAS	Phase	Spe		Vapor		Hour	ly or Ba	tch Outpu	t Rate
No.	- 1000	Gra	vity   F	Pressure	Norma	ıl	Max	dimum	Units
						1			
								1	
						1		1	
Complete the following levels <u>before</u> entering	g emissi header :	on dat	a for ec	uipment fore cor	connected to	a head	der exha	aust syste	m, giving emissions
☐ Check here if not a			(		aro, oquipinoi				
Emission Point ID (exhaus			er syste	em):					
Material Name and CAS N					ential Emissio	n Rate	(lb/hr)		Method **
Method							Wicthoo		
		İ							
							ı		
		ľ							
		ı							
* MB - material balance: E	E - Engir	neering	Estima	ate: TM -	Test Measure	ement (	submit	test data):	O - other (Explain)
		-:"							` ' /

10.	additio	le the following information pertaining onal pages as necessary if more than or on Control Device Sheet if necessary.	to each condense ne condenser is us	er that may be attached to this reactor. Attached for this reactor. Complete the Condenser Air
	☐ Che	eck here if not applicable		
	10A.	Cooling material		
	10B.	Minimum and Maximum flowrate of c	ooling material (ga	al/hr)
	10C.	Inlet temperature of cooling material (	· -	•
	10D.	Outlet temperature of cooling materia	al (°F)	
	10E.	Pressure drop of gas to be condense	ed from inlet to outle	et (psig)
	10F.	Inlet temperature of gas stream (°F)		·· -/
	10G.	Outlet temperature of gas stream (°F)	)	
	10H.	Number of passes		
	101.	Cooling surface area		
11.	Provide	e the following pertaining to auxiliary eq	uipment that burns	s fuel (heaters, dryers, etc.):
	☐ Che	eck here if not applicable		
	11A.	Type of fuel and maximum fuel burn r	rata per hour:	
	117.	Type of fuel and maximum rues burn r	ate, per nour	
	11B.	Provide maximum percent sulfur (S), ε	ash content of fuel,	and the energy content using appropriate units:
		%S	% Ash	BTU/lb, std. ft³/day, gal
			• • • • • • • • • • • • • • • • • • • •	
				(circle one)
	11C.	Theoretical combustion air requiremen PSIA:	nt in SCFD per unit	of fuel (circle appropriate unit) @ 70°F and 14.7
		SCFD/lb, SCFD, g	gal (circle one)	
	11D.	Percent excess air:	%	
	11E.	Type, amount, and BTU rating of burn		ring equipment that are planned to be used:
		7,500	oro and an oaro	ing equipment that are planned to be used.
•	11F.	Total maximum design heat input:		×10 <sup>6</sup> BTU/hr.

12. Proposed Monitoring, Recordkeeping, Reporting, and Testing Please propose monitoring, recordkeeping, and reporting in order to demonstrate compliance with the proposed operating parameters. Please propose testing in order to demonstrate compliance with the proposed emissions limits.					
ONITORING   RECORDKEEPING					
REPORTING	TESTING				
MONITORING. PLEASE LIST AND DESCRIBE THE PROCESS PARAMETERS AND RANGES THAT ARE PROPOSED TO BE MONITORED IN ORDER TO DEMONSTRATE COMPLIANCE WITH THE OPERATION OF THIS PROCESS EQUIPMENT OPERATION OR AIR POLLUTION CONTROL DEVICE.					
RECORDKEEPING. PLEASE DESCRIBE THE PROPO	SED RECORDKEEPING THAT WILL ACCOMPANY THE MONITORING.				
REPORTING. PLEASE DESCRIBE THE PROPOSED FREQUENCY OF REPORTING OF THE RECORDICEPING.  TESTING. PLEASE DESCRIBE ANY PROPOSED EMISSIONS TESTING FOR THIS PROCESS FOLLOWERS OF A REPORT OF A PROPOSED FOR THE PROPOSED FOR THE PROCESS FOLLOWERS.					
<b>TESTING.</b> PLEASE DESCRIBE ANY PROPOSED EMISSIONS TESTING FOR THIS PROCESS EQUIPMENT OR AIR POLLUTION CONTROL DEVICE.					
13. Describe all operating ranges and maintenance procedures required by Manufacturer to maintain warranty					
The state of the s	o processing required by managed or to maintain warranty				

NOTE: An AIR POLLUTION CONTROL DEVICE SHEET must be completed for any air pollution device(s) (except emergency relief devices) used to control emissions from this reactor.

### **DISTILLATION COLUMN DATA SHEET**

Id	entification Number (as assigned on <i>Eq</i>	uipment List Form):	
1.	Name and type of equipment		
#.	Projected actual equipment operating	schedule (complete appropriate lines):	
	hrs/day	days/week	weeks/year
	hrs/batch	batches/day, batches/week (circle one)	days/yr, weeks/yr (circle one)
2.	Number of stages (plates), excluding	condenser	
3.	Number of feed plates and stage loca	tion	
4.	Specify details of any reheating, recyc	ling, or stage conditioning along with the stage lo	ocations
5.	Specify reflux ratio, R (where R is defin R=L/D, where L = liquid down column,	ned as the ratio of the reflux to the overhead produ D = distillation product)	uct, given symbolically as
6.	Specify the fraction of feed which is var continuously as vapor).	porized, f (where f is the molal fraction of the feed	that leaves the feed plate
	Type of condenser used:	☐ partial ☐ multiple perating details including all inlet and outlet tempe	☐ other eratures, pressures, and
8.	Feed Characteristics  A. Molar composition  B. Individual vapor pressure of each of the composition of the c		
9.	Overhead Product  A. Molar composition of components  B. Vapor pressure of components  C. Total mass flow rate of all streams	leaving the system as overhead products	
10.	Bottom Product  A. Molar composition of all componer  B. Total mass flow rate of all steams in	nts leaving the system as bottom products	

General Information     A. Distillation column diameter	_
B. Distillation column height	
C. Type of plates	
D. Plate spacing     E. Murphree plate efficiency	
F. Any other information necessary of describe the	operation of this distillation column.
12. Proposed Monitoring, Recordkeeping, Reporting	, and Testing
Please propose monitoring, recordkeeping, and report operating parameters. Please propose testing in order limits.	rting in order to demonstrate compliance with the proposed er to demonstrate compliance with the proposed emissions
MONITORING	RECORDKEEPING
REPORTING	TESTING
MONITORING DI EASE LIST AND DESCRIBETUE DECCESS DA	
MONITORING. PLEASE LIST AND DESCRIBE THE PROCESS PAR IN ORDER TO DEMONSTRATE COMPLIANCE WITH THE OP POLLUTION CONTROL DEVICE.	RAMETERS AND RANGES THAT ARE PROPOSED TO BE MONITORED PERATION OF THIS PROCESS EQUIPMENT OPERATION OR AIR
RECORDKEEPING. PLEASE DESCRIBE THE PROPOSED REC	ORDKEEPING THAT WILL ACCOMPANY THE MONITORING.
REPORTING. PLEASE DESCRIBE THE PROPOSED FREQUENC	
<b>TESTING.</b> PLEASE DESCRIBE ANY PROPOSED EMISSIONS TEST DEVICE.	
13. Describe all operating ranges and maintenance proce	dures required by Manufacturer to maintain warranty

NOTE: An AIR POLLUTION CONTROL DEVICE SHEET must be completed for any air pollution device(s) (except emergency relief devices) used to control emissions from this distillation column.

Provide the following information for <u>each</u> new or modified bulk liquid storage tank as shown on the *Equipment List Form* and other parts of this application. A tank is considered modified if the material to be stored in the tank is different from the existing stored liquid.

IF USING US EPA'S TANKS EMISSION ESTIMATION PROGRAM (AVAILABLE AT <a href="https://www.epa.gov/tnn/tanks.html">www.epa.gov/tnn/tanks.html</a>), APPLICANT MAY ATTACH THE SUMMARY SHEETS IN LIEU OF COMPLETING SECTIONS III, IV, & V OF THIS FORM. HOWEVER, SECTIONS I, II, AND VI OF THIS FORM MUST BE COMPLETED. US EPA'S AP-42, SECTION 7.1, "ORGANIC LIQUID STORAGE TANKS," MAY ALSO BE USED TO ESTIMATE VOC AND HAP EMISSIONS (<a href="https://www.epa.gov/tnn/chief/">http://www.epa.gov/tnn/chief/</a>).

### I. GENERAL INFORMATION (required)

2. Tank Name

1. Bulk Storage Area Name

	Condensate Storage Tank			
3. Tank Equipment Identification No. (as assigned on Equipment List Form)	4. Emission Point Identification No. (as assigned on Equipment List Form)			
CTK-1	15E			
5. Date of Commencement of Construction (for existing	tanks) 2015			
	New Stored Material			
7. Description of Tank Modification (if applicable) Updated production				
7A. Does the tank have more than one mode of operation (e.g. Is there more than one product stored in the tan	k?)			
7B. If YES, explain and identify which mode is covere completed for each mode).	ed by this application (Note: A separate form must be			
7C. Provide any limitations on source operation affecting variation, etc.):	emissions, any work practice standards (e.g. production			
II. TANK INFORMATION (required)				
height.	the internal cross-sectional area multiplied by internal			
	00-bbl			
9A. Tank Internal Diameter (ft)	9B. Tank Internal Height (or Length) (ft)			
10A. Maximum Liquid Height (ft)	20 10B. Average Liquid Height (ft)			
19	14			
11A. Maximum Vapor Space Height (ft)	11B. Average Vapor Space Height (ft)			
1	6.57			
<ol> <li>Nominal Capacity (specify barrels or gallons). This is liquid levels and overflow valve heights.</li> </ol>	s also known as "working volume" and considers design			

13A. Maximum annual throughput (gal/yr)	13B. Maximum daily throughput (gal/day)	
255,500	13B. Maximum daily throughput (gal/day) 700	
14. Number of Turnovers per year (annual net throughpu		
1	5.89	
15. Maximum tank fill rate (gal/min) N/A		
	Splash Bottom Loading	
17. Complete 17A and 17B for Variable Vapor Space Tar		
17A. Volume Expansion Capacity of System (gal)	17B. Number of transfers into system per year	
18. Type of tank (check all that apply):  ☐ Fixed Roof x vertical horizontal  ☐ other (describe)  ☐ External Floating Roof pontoon roof  ☐ Domed External (or Covered) Floating Roof	flat roof dome roof dome roof double deck roof	
☐ Internal Floating Roof vertical column sup ☐ Variable Vapor Space lifter roof ☐ Pressurized spherical cylindrical ☐ Underground ☐ Other (describe)	_ diaphragm	
III. TANK CONSTRUCTION & OPERATION INFORMA	TION (optional if providing TANKS Summary Sheets)	
19. Tank Shell Construction:  ☑ Riveted ☐ Gunite lined ☐ Epoxy-coated	_	
20A. Shell Color White 20B. Roof Color		
21. Shell Condition (if metal and unlined):	Todi Edot i dilitod	
☑ No Rust ☐ Light Rust ☐ Dense Rus	st	
22A. Is the tank heated? ☐ YES ☒ NO		
22B. If YES, provide the operating temperature (°F)		
22C. If YES, please describe how heat is provided to tar	nk.	
23. Operating Pressure Range (psig): 14.7 to 14.7		
24. Complete the following section for Vertical Fixed Room	f Tanks	
24A. For dome roof, provide roof radius (ft)		
24B. For cone roof, provide slope (ft/ft) 0.06		
25. Complete the following section for Floating Roof Tank	Some Does Not Apply	
25A. Year Internal Floaters Installed:		
25B. Primary Seal Type: ☐ Metallic (Mechanical) S (check one) ☐ Vapor Mounted Resilie		
25C. Is the Floating Roof equipped with a Secondary Se	al?	
25D. If YES, how is the secondary seal mounted? (check	k one) Shoe Rim Other (describe):	
25E. Is the Floating Roof equipped with a weather shield	d? ☐ YES ☐ NO	

25F. Describe deck fittings; indica	te the number of ea	ach type of fitting:				
ACCESS HATCH						
BOLT COVER, GASKETED:		ER, GASKETED:	UNBOLTED COVER, UNGASKETED:			
	AUTOMATIC GAI	JGE FLOAT WELL				
BOLT COVER, GASKETED:	UNBOLTED COV		UNBOLTED COVER, UNGASKETED:			
	COLUM	IN WELL				
BUILT-UP COLUMN – SLIDING COVER, GASKETED:		JMN - SLIDING	PIPE COLUMN - FLEXIBLE FABRIC SLEEVE SEAL:			
	LADDE	R WELL				
PIP COLUMN – SLIDING COVER, G		1	SLIDING COVER, UNGASKETED:			
	GAUGE-HATCH	//SAMPLE PORT				
SLIDING COVER, GASKETED:		SLIDING COVER,	UNGASKETED:			
	ROOF LEG OR	HANGER WELL				
WEIGHTED MECHANICAL ACTUATION, GASKETED:		MECHANICAL	SAMPLE WELL-SLIT FABRIC SEAL (10% OPEN AREA)			
	VACUUM	BREAKER				
WEIGHTED MECHANICAL ACTUATI			NICAL ACTUATION, UNGASKETED:			
	RIM \	/ENT				
WEIGHTED MECHANICAL ACTUATI			NICAL ACTUATION, UNGASKETED:			
	DECK DRAIN (3-II	NCH DIAMETER				
OPEN:	DECK DIVAIN (3-III	90% CLOSED:				
	CTID I	DAIN!				
1-INCH DIAMETER:	STUB	JKAIN				
OTHER (DESCR	IRE ATTACH ADD	ITIONAL PAGES IF	NECESCADA)			
OTHER (BESON	BL, ATTACH ADD	ITIONAL PAGES IF	- NECESSARY)			

26. Complete the following section for Internal Floating F	Roof Tanks 🛛 Does Not Apply
26A. Deck Type:	
26B. For Bolted decks, provide deck construction:	
26C. Deck seam:	
Continuous sheet construction 5 feet wide Continuous sheet construction 6 feet wide	
Continuous sheet construction 7 feet wide	
☐ Continuous sheet construction 5 × 7.5 feet wide ☐ Continuous sheet construction 5 × 12 feet wide	
Other (describe)	
CCD Dark and the (f)	
26D. Deck seam length (ft)  For column supported tanks:	26E. Area of deck (ft²)
26F. Number of columns:	26G. Diameter of each column:
	f providing TANKS Summary Sheets)
27. Provide the city and state on which the data in this se	
Charleston, WV	
28. Daily Average Ambient Temperature (°F)	
29. Annual Average Maximum Temperature (°F)	
30. Annual Average Minimum Temperature (°F)	
31. Average Wind Speed (miles/hr)	
32. Annual Average Solar Insulation Factor (BTU/(ft²-day	7))
33. Atmospheric Pressure (psia)	
V. LIQUID INFORMATION (optional i	f providing TANKS Summary Sheets)
34. Average daily temperature range of bulk liquid:	
34A. Minimum (°F)	34B. Maximum (°F)
35. Average operating pressure range of tank:	
35A. Minimum (psig)	35B. Maximum (psig)
36A. Minimum Liquid Surface Temperature (°F)	36B. Corresponding Vapor Pressure (psia)
37A. Average Liquid Surface Temperature (°F)	37B. Corresponding Vapor Pressure (psia)
	tapan nasaana (pala)
38A. Maximum Liquid Surface Temperature (°F)	38B. Corresponding Vapor Pressure (psia)
39. Provide the following for <u>each</u> liquid or gas to be store	ed in tank. Add additional pages if necessary
39A. Material Name or Composition	
39B. CAS Number	
39C. Liquid Density (lb/gal)	
39D. Liquid Molecular Weight (lb/lb-mole)	
39E. Vapor Molecular Weight (lb/lb-mole)	

Marches M. D.				
Maximum Vapor Pres 39F. True (psia)	ssure			
39G. Reid (psia)				
Months Storage per Y	/ear			
39H. From				
39I. To				
	VI. EMISSIONS	AND CONTROL D	EVICE DATA (required	<u> </u>
40. Emission Control	Devices (check as mar			·/
☐ Carbon Adsorp		., do appi,) Do	oo Not Apply	
☐ Condenser <sup>1</sup>	0.1011			
☐ Conservation \	Vent (neig)			
Vacuum S		Droop	ura Cattina	
	elief Valve (psig)	riess	ure Setting	
☐ Inert Gas Blan				
☐ Insulation of Ta				
· ·	ion (scrubber) <sup>1</sup>			
Refrigeration o				
Rupture Disc (				
☐ Vent to Inciner				
Other¹ (describ	e): Flare			
41. Expected Emission	n Rate (submit Test Da	ata or Calculations	here or elsewhere in th	e application)
				o application).
Material Name &	Breathing Loss	1	_ 1	.
Material Name & CAS No.	Breathing Loss (lb/hr)	Working Los	s Annual Loss	1
		Working Los	s Annual Loss	.
	(lb/hr)	Working Los	s Annual Loss	.
	(lb/hr) See Attachment N,	Working Los	s Annual Loss	.
	(lb/hr) See Attachment N,	Working Los	s Annual Loss	.
	(lb/hr) See Attachment N,	Working Los	s Annual Loss	.
	(lb/hr) See Attachment N,	Working Los	s Annual Loss	.
	(lb/hr) See Attachment N,	Working Los	s Annual Loss	.
	(lb/hr) See Attachment N,	Working Los	s Annual Loss	.
	(lb/hr) See Attachment N,	Working Los	s Annual Loss	.
	(lb/hr) See Attachment N,	Working Los	s Annual Loss	.
	(lb/hr) See Attachment N,	Working Los	s Annual Loss	.
	(lb/hr) See Attachment N,	Working Los	s Annual Loss	.
	(lb/hr) See Attachment N,	Working Los	s Annual Loss	.
	(lb/hr) See Attachment N,	Working Los	s Annual Loss	.

 $<sup>^{1}</sup>$  EPA = EPA Emission Factor, MB = Material Balance, SS = Similar Source, ST = Similar Source Test, Throughput Data, O = Other (specify)

Remember to attach emissions calculations, including TANKS Summary Sheets if applicable.

Provide the following information for <u>each</u> new or modified bulk liquid storage tank as shown on the *Equipment List Form* and other parts of this application. A tank is considered modified if the material to be stored in the tank is different from the existing stored liquid.

IF USING US EPA'S TANKS EMISSION ESTIMATION PROGRAM (AVAILABLE AT <a href="https://www.epa.gov/tnn/tanks.html">www.epa.gov/tnn/tanks.html</a>), APPLICANT MAY ATTACH THE SUMMARY SHEETS IN LIEU OF COMPLETING SECTIONS III, IV, & V OF THIS FORM. HOWEVER, SECTIONS I, II, AND VI OF THIS FORM MUST BE COMPLETED. US EPA'S AP-42, SECTION 7.1, "ORGANIC LIQUID STORAGE TANKS," MAY ALSO BE USED TO ESTIMATE VOC AND HAP EMISSIONS (<a href="https://www.epa.gov/tnn/chief/">http://www.epa.gov/tnn/chief/</a>).

1 Dulle Changes A. N.					
Bulk Storage Area Name	2. Tank Name				
	Condensate Storage Tank				
3. Tank Equipment Identification No. (as assigned on	4. Emission Point Identification No. (as assigned on				
Equipment List Form)	Equipment List Form)				
CTK-2	16E				
5. Date of Commencement of Construction (for existing	tanks) 2015				
	New Stored Material				
Description of Tank Modification (if applicable)					
Updated production					
7A. Does the tank have more than one mode of operation (e.g. Is there more than one product stored in the tan	k?)				
7B. If YES, explain and identify which mode is covered	ed by this application (Note: A separate form must be				
completed for each mode).	, , , , , , , , , , , , , , , , , , , ,				
7C. Provide any limitations on source operation affecting	emissions any work practice standards (a.g. production				
7C. Provide any limitations on source operation affecting emissions, any work practice standards (e.g. production variation, etc.):					
II. TANK INFORM					
8. Design Capacity (specify barrels or gallons). Use	the internal cross-sectional area multiplied by internal				
neight.					
	00-bbl				
9A. Tank Internal Diameter (ft)	9B. Tank Internal Height (or Length) (ft)				
12	20				
10A. Maximum Liquid Height (ft)	10B. Average Liquid Height (ft)				
19	14				
11A. Maximum Vapor Space Height (ft)	11B. Average Vapor Space Height (ft)				
1	6.57				
12. Nominal Capacity (specify barrels or gallons). This is	also known as "working volume" and considers design				
liquid levels and overflow valve heights.	The second design with the second considers design				
	074 gal				

13A. Maximum annual throughput (gal/yr) 255,500	13B. Maximum daily throughput (gal/day) 700	
14. Number of Turnovers per year (annual net throughpu		
	5.89	
15. Maximum tank fill rate (gal/min) N/A		
16. Tank fill method Submerged	☐ Splash ☐ Bottom Loading	
17. Complete 17A and 17B for Variable Vapor Space Tar	nk Systems Does Not Apply	
17A. Volume Expansion Capacity of System (gal)	17B. Number of transfers into system per year	
18. Type of tank (check all that apply):  ☐ Fixed Roof x vertical horizontal  — other (describe)  ☐ External Floating Roof pontoon roof  ☐ Domed External (or Covered) Floating Roof  ☐ Internal Floating Roof vertical column sup  ☐ Variable Vapor Space lifter roof  ☐ Pressurized spherical cylindrical  ☐ Underground  ☐ Other (describe)	double deck roof  pport self-supporting	
III. TANK CONSTRUCTION & OPERATION INFORMA	ATION (optional if providing TANKS Summary Sheets)	
Tank Shell Construction:     ⊠ Riveted ☐ Gunite lined ☐ Epoxy-coated		
20A. Shell Color White 20B. Roof Color		
21. Shell Condition (if metal and unlined):		
☑ No Rust ☐ Light Rust ☐ Dense Ru	st  Not applicable	
22A. Is the tank heated? YES NO		
22B. If YES, provide the operating temperature (°F)		
22C. If YES, please describe how heat is provided to ta	nk.	
23. Operating Pressure Range (psig): 14.7 to 14.7		
24. Complete the following section for Vertical Fixed Roo	f Tanks	
24A. For dome roof, provide roof radius (ft)		
24B. For cone roof, provide slope (ft/ft) 0.06		
25. Complete the following section for Floating Roof Tank	ks 🛛 Does Not Apply	
25A. Year Internal Floaters Installed:		
25B. Primary Seal Type:	<u> </u>	
25C. Is the Floating Roof equipped with a Secondary Se	eal? YES NO	
25D. If YES, how is the secondary seal mounted? (chec	ck one)	
25E. Is the Floating Roof equipped with a weather shiel	d? YES NO	

25F. Describe deck fittings; indicate the number of each type of fitting:						
ACCESS HATCH						
BOLT COVER, GASKETED:		ER, GASKETED:	UNBOLTED COVER, UNGASKETED:			
	AUTOMATIC GAI	JGE FLOAT WELL	1			
BOLT COVER, GASKETED:	UNBOLTED COV		UNBOLTED COVER, UNGASKETED:			
	COLUM	IN WELL	1			
BUILT-UP COLUMN ~ SLIDING COVER, GASKETED:		JMN - SLIDING	PIPE COLUMN - FLEXIBLE FABRIC SLEEVE SEAL:			
	LADDE	R WELL				
PIP COLUMN – SLIDING COVER, G			SLIDING COVER, UNGASKETED:			
	GAUGE-HATCH	/SAMPLE PORT				
SLIDING COVER, GASKETED:	SAGGE HATON	SLIDING COVER,	UNGASKETED:			
	ROOF LEG OR	HANGER WELL				
WEIGHTED MECHANICAL ACTUATION, GASKETED:		MECHANICAL	SAMPLE WELL-SLIT FABRIC SEAL (10% OPEN AREA)			
	VACUUM	BREAKER				
WEIGHTED MECHANICAL ACTUATI			NICAL ACTUATION, UNGASKETED:			
	RIM \	/ENT				
WEIGHTED MECHANICAL ACTUATION			NICAL ACTUATION, UNGASKETED:			
	DECK DRAIN (3-II	NCH DIAMETER)				
OPEN:	DEOR DIVANA (3-1)	90% CLOSED:				
	STUB I	ORAIN				
1-INCH DIAMETER:	31081	21 VAII V				
OTHER (DESCR	IBE, ATTACH ADD	ITIONAL PAGES IF	NECESSARY)			
			·			

26. Complete the following section for Internal Float	ting Roof Tanks
26A. Deck Type: Bolted Welded	
26B. For Bolted decks, provide deck construction	1:
26C. Deck seam:	
Continuous sheet construction 5 feet wide	
Continuous sheet construction 6 feet wide Continuous sheet construction 7 feet wide	
Continuous sheet construction 5 × 7.5 feet w	
☐ Continuous sheet construction 5 × 12 feet wi☐ Other (describe)	de
26D. Deck seam length (ft)	26E. Area of deck (ft²)
For column supported tanks:	26G. Diameter of each column:
26F. Number of columns:	
	onal if providing TANKS Summary Sheets)
<ol> <li>Provide the city and state on which the data in the Charleston, WV</li> </ol>	his section are based.
28. Daily Average Ambient Temperature (°F)	
29. Annual Average Maximum Temperature (°F)	
30. Annual Average Minimum Temperature (°F)	
31. Average Wind Speed (miles/hr)	
32. Annual Average Solar Insulation Factor (BTU/(ft	2·dav))
33. Atmospheric Pressure (psia)	
	onal if providing TANKS Summary Sheets)
34. Average daily temperature range of bulk liquid:	
34A. Minimum (°F)	34B. Maximum (°F)
35. Average operating pressure range of tank:	
35A. Minimum (psig)	35B. Maximum (psig)
36A. Minimum Liquid Surface Temperature (°F)	36B. Corresponding Vapor Pressure (psia)
37A. Average Liquid Surface Temperature (°F)	37B. Corresponding Vapor Pressure (psia)
38A. Maximum Liquid Surface Temperature (°F)	38B. Corresponding Vapor Pressure (psia)
39. Provide the following for each liquid or gas to be	stored in tank. Add additional pages if necessary
39A. Material Name or Composition	l l
39B. CAS Number	
39C. Liquid Density (lb/gal)	
39D. Liquid Molecular Weight (lb/lb-mole)	
39E. Vapor Molecular Weight (lb/lb-mole)	

I Maximi im Manor Pressi				1	
Maximum Vapor Pressu 39F. True (psia)	ıre				
39G. Reid (psia)					
Months Storage per Yea	ar			-	
39H. From					
39I. To					
	VI. EMISSIONS A	AND CONTR	ROL DEVICI	E DATA (required)	
40. Emission Control De			_:		
☐ Carbon Adsorpti			_	11.7	
Condenser <sup>1</sup>					
☐ Conservation Ve	ent (psia)				
Vacuum Se			Pressure Se	etting	
☐ Emergency Relie	•		. 1000010 01	otting	
☐ Inert Gas Blanke	,				
☐ Insulation of Tan					
Liquid Absorption					
Refrigeration of	,				
Rupture Disc (ps					
☐ Vent to Incinerate	• /				
☐ Verit to inclinerate ☐ Other¹ (describe)					
Other (describe)	). Frare				
				<del></del>	
41. Expected Emission	Rate (submit Test Da	ita or Calcula	ations here	or elsewhere in the ap	pplication).
Material Name &	<b>Breathing Loss</b>	Workin	g Loss	<b>Annual Loss</b>	Estimation Method <sup>1</sup>
CAS No.	(lb/hr)	Amount	Units	(lb/yr)	Estimation Method
	See Attachment N,				
	Table 14			<u> </u>	

<sup>&</sup>lt;sup>1</sup> EPA = EPA Emission Factor, MB = Material Balance, SS = Similar Source, ST = Similar Source Test, Throughput Data, O = Other (specify)

Remember to attach emissions calculations, including TANKS Summary Sheets if applicable.

Provide the following information for <u>each</u> new or modified bulk liquid storage tank as shown on the *Equipment List Form* and other parts of this application. A tank is considered modified if the material to be stored in the tank is different from the existing stored liquid.

IF USING US EPA'S TANKS EMISSION ESTIMATION PROGRAM (AVAILABLE AT <a href="https://www.epa.gov/tnn/tanks.html">www.epa.gov/tnn/tanks.html</a>), APPLICANT MAY ATTACH THE SUMMARY SHEETS IN LIEU OF COMPLETING SECTIONS III, IV, & V OF THIS FORM. HOWEVER, SECTIONS I, II, AND VI OF THIS FORM MUST BE COMPLETED. US EPA'S AP-42, SECTION 7.1, "ORGANIC LIQUID STORAGE TANKS," MAY ALSO BE USED TO ESTIMATE VOC AND HAP EMISSIONS (<a href="https://www.epa.gov/tnn/chief/">http://www.epa.gov/tnn/chief/</a>).

### I. GENERAL INFORMATION (required)

2. Tank Name

Condensate Storage Tank

1. Bulk Storage Area Name

<ol> <li>Tank Equipment Identification No. (as assigned or Equipment List Form)</li> <li>CTK-3</li> </ol>	<ol> <li>Emission Point Identification No. (as assigned on Equipment List Form)</li> <li>17E</li> </ol>	
Date of Commencement of Construction (for existing		
	New Stored Material	
7. Description of Tank Modification (if applicable)	Source Tank Wouldcatton	
Updated production		
7A. Does the tank have more than one mode of operatio (e.g. Is there more than one product stored in the tar	nk?)	
7B. If YES, explain and identify which mode is cover completed for each mode).	ed by this application (Note: A separate form must be	
completed for each mode).		
7C. Provide any limitations on source operation affecting variation, etc.):	g emissions, any work practice standards (e.g. production	
	IATION (required)	
<ol><li>Design Capacity (specify barrels or gallons). Use height.</li></ol>	the internal cross-sectional area multiplied by internal	
	00-bb1	
9A. Tank Internal Diameter (ft)	9B. Tank Internal Height (or Length) (ft)	
12 10A. Maximum Liquid Height (ft)	20	
10A. Maximum Liquid Height (ft)	10B. Average Liquid Height (ft)	
11A. Maximum Vapor Space Height (ft)	14 11B. Average Vapor Space Height (ft)	
1	6.57	
12. Nominal Capacity (specify barrels or gallons). This is also known as "working volume" and considers design liquid levels and overflow valve heights.		
16.	074 gal	

13A. Maximum annual throughput (gal/yr)	13B. Maximum daily throughput (gal/day)	
255,500  14. Number of Turnovers per year (annual net throughpu	t/maximum tank liquid volume)	
15.89		
15. Maximum tank fill rate (gal/min) N/A		
16. Tank fill method Submerged	☐ Splash ☐ Bottom Loading	
17. Complete 17A and 17B for Variable Vapor Space Tar		
17A. Volume Expansion Capacity of System (gal)	17B. Number of transfers into system per year	
18. Type of tank (check all that apply):    Fixed Roof	pport self-supporting	
III. TANK CONSTRUCTION & OPERATION INFORMA	ATION (optional if providing TANKS Summary Sheets)	
Tank Shell Construction:     ⊠ Riveted ☐ Gunite lined ☐ Epoxy-coated	14	
20A. Shell Color White 20B. Roof Color		
21. Shell Condition (if metal and unlined):  ☑ No Rust ☐ Light Rust ☐ Dense Ru	ıst ☐ Not applicable	
22A. Is the tank heated? YES NO	Tvot applicable	
22B. If YES, provide the operating temperature (°F)		
22C. If YES, please describe how heat is provided to tank.		
23. Operating Pressure Range (psig): 14.7 to 14.7		
24. Complete the following section for Vertical Fixed Roo	of Tanks Does Not Apply	
24A. For dome roof, provide roof radius (ft)		
24B. For cone roof, provide slope (ft/ft) 0.06		
25. Complete the following section for Floating Roof Tan	ks Does Not Apply	
25A. Year Internal Floaters Installed:		
25B. Primary Seal Type:	_ ,	
25C. Is the Floating Roof equipped with a Secondary Se	eal? YES NO	
25D. If YES, how is the secondary seal mounted? (check	ck one)	
25E. Is the Floating Roof equipped with a weather shiel	d? YES NO	

25F. Describe deck fittings; indicate the number of each type of fitting:			
ACCESS HATCH			
BOLT COVER, GASKETED:	UNBOLTED COVER, GASKETED: UNBOLTED COVER, UNGASKETED:		
	AUTOMATIC GAI	JGE FLOAT WELL	
BOLT COVER, GASKETED:	1	AUTOMATIC GAUGE FLOAT WELL UNBOLTED COVER, GASKETED: UNBOLTED COVER, UNGASKETED:	
	COLUM	IN WELL	
BUILT-UP COLUMN – SLIDING COVER, GASKETED:		JMN - SLIDING	PIPE COLUMN – FLEXIBLE FABRIC SLEEVE SEAL:
	LADDE	R WELL	
PIP COLUMN – SLIDING COVER, G			SLIDING COVER, UNGASKETED:
	GAUGE-HATCH	I/SAMPLE PORT	
SLIDING COVER, GASKETED:		SLIDING COVER,	UNGASKETED:
	ROOF LEG OR	HANGER WELL	
WEIGHTED MECHANICAL ACTUATION, GASKETED:		MECHANICAL	SAMPLE WELL-SLIT FABRIC SEAL (10% OPEN AREA)
	VACUUM	BREAKER	
WEIGHTED MECHANICAL ACTUATION, GASKETED:   WEIGHTED MECHANICAL ACTUATION, UNGASKETED:			
	DIM	/ENT	
RIM VENT WEIGHTED MECHANICAL ACTUATION GASKETED: WEIGHTED MECHANICAL ACTUATION, UNGASKETED:			
DECK DRAIN (3-INCH DIAMETER)			
OPEN: 90% CLOSED:			
STUB DRAIN			
1-INCH DIAMETER:			
OTHER (DESCRIBE, ATTACH ADDITIONAL PAGES IF NECESSARY)			

26. Complete the following section for Internal Floating	Roof Tanks Does Not Apply
26A. Deck Type:	N
26B. For Bolted decks, provide deck construction:	
26C. Deck seam:	
26C. Deck seam:  Continuous sheet construction 5 feet wide	
Continuous sheet construction 6 feet wide	
Continuous sheet construction 7 feet wide Continuous sheet construction 5 × 7.5 feet wide	
Continuous sheet construction 5 × 12 feet wide	
Other (describe)	
26D. Deck seam length (ft)	26E. Area of deck (ft²)
For column supported tanks:	26G. Diameter of each column:
26F. Number of columns:	
	if providing TANKS Summary Sheets)
27. Provide the city and state on which the data in this s Charleston, WV	section are based.
28. Daily Average Ambient Temperature (°F)	
29. Annual Average Maximum Temperature (°F)	
30. Annual Average Minimum Temperature (°F)	
31. Average Wind Speed (miles/hr)	
32. Annual Average Solar Insulation Factor (BTU/(ft²-da	ay))
33. Atmospheric Pressure (psia)	
V. LIQUID INFORMATION (optional	l if providing TANKS Summary Sheets)
34. Average daily temperature range of bulk liquid:	
34A. Minimum (°F)	34B. Maximum (°F)
35. Average operating pressure range of tank:	
35A. Minimum (psig)	35B. Maximum (psig)
36A. Minimum Liquid Surface Temperature (°F)	36B. Corresponding Vapor Pressure (psia)
37A. Average Liquid Surface Temperature (°F)	37B. Corresponding Vapor Pressure (psia)
38A. Maximum Liquid Surface Temperature (°F)	38B. Corresponding Vapor Pressure (psia)
39. Provide the following for each liquid or gas to be sto	red in tank. Add additional pages if necessary.
39A. Material Name or Composition	
39B. CAS Number	
39C. Liquid Density (lb/gal)	
39D. Liquid Molecular Weight (lb/lb-mole)	
39E. Vapor Molecular Weight (lb/lb-mole)	

				T	
Maximum Vapor Pres 39F. True (psia)	sure				
39F. True (psia) 39G. Reid (psia)					
Months Storage per Y	'ear				
39H. From					
39I. To					
	VI. EMISSIONS A	ND CONTROL	DEVICE	DATA (required)	
40. Emission Control	Devices (check as mar	y as apply): 🔲 l	Does No	t Apply	
☐ Carbon Adsorp		–			
☐ Condenser¹					
☐ Conservation \	/ent (psig)				
Vacuum S		Pre	ssure Se	ettina	
1	elief Valve (psig)			3	
☐ Inert Gas Blan	•				
☐ Insulation of Ta					
Liquid Absorpti					
☐ Refrigeration o	•				
Rupture Disc (					
☐ Vent to Inciner					
☐ Other¹ (describ					
Z Other (describ	oj. Trare				
44 5 ( 15 1 1	D 1 / 1 17 / D				
				and a language of the Alama and	
	l ·	F	1	or elsewhere in the a	pplication).
Material Name &	Breathing Loss	Working L	oss	Annual Loss	pplication).
	Breathing Loss (lb/hr)	Working L	1		
Material Name &	Breathing Loss (lb/hr) See Attachment N,	Working L	oss	Annual Loss	
Material Name &	Breathing Loss (lb/hr)	Working L	oss	Annual Loss	
Material Name &	Breathing Loss (lb/hr) See Attachment N,	Working L	oss	Annual Loss	
Material Name &	Breathing Loss (lb/hr) See Attachment N,	Working L	oss	Annual Loss	
Material Name &	Breathing Loss (lb/hr) See Attachment N,	Working L	oss	Annual Loss	
Material Name &	Breathing Loss (lb/hr) See Attachment N,	Working L	oss	Annual Loss	
Material Name &	Breathing Loss (lb/hr) See Attachment N,	Working L	oss	Annual Loss	
Material Name &	Breathing Loss (lb/hr) See Attachment N,	Working L	oss	Annual Loss	
Material Name &	Breathing Loss (lb/hr) See Attachment N,	Working L	oss	Annual Loss	
Material Name &	Breathing Loss (lb/hr) See Attachment N,	Working L	oss	Annual Loss	
Material Name &	Breathing Loss (lb/hr) See Attachment N,	Working L	oss	Annual Loss	
Material Name &	Breathing Loss (lb/hr) See Attachment N,	Working L	oss	Annual Loss	
Material Name &	Breathing Loss (lb/hr) See Attachment N,	Working L	oss	Annual Loss	
Material Name &	Breathing Loss (lb/hr) See Attachment N,	Working L	oss	Annual Loss	
Material Name &	Breathing Loss (lb/hr) See Attachment N,	Working L	oss	Annual Loss	
Material Name &	Breathing Loss (lb/hr) See Attachment N,	Working L	oss	Annual Loss	
Material Name &	Breathing Loss (lb/hr) See Attachment N,	Working L	oss	Annual Loss	
Material Name &	Breathing Loss (lb/hr) See Attachment N,	Working L	oss	Annual Loss	

<sup>&</sup>lt;sup>1</sup> EPA = EPA Emission Factor, MB = Material Balance, SS = Similar Source, ST = Similar Source Test, Throughput Data, O = Other (specify)

<sup>⊠</sup> Remember to attach emissions calculations, including TANKS Summary Sheets if applicable.

Provide the following information for <u>each</u> new or modified bulk liquid storage tank as shown on the *Equipment List Form* and other parts of this application. A tank is considered modified if the material to be stored in the tank is different from the existing stored liquid.

IF USING US EPA'S TANKS EMISSION ESTIMATION PROGRAM (AVAILABLE AT <a href="https://www.epa.gov/tnn/tanks.html">www.epa.gov/tnn/tanks.html</a>), APPLICANT MAY ATTACH THE SUMMARY SHEETS IN LIEU OF COMPLETING SECTIONS III, IV, & V OF THIS FORM. HOWEVER, SECTIONS I, II, AND VI OF THIS FORM MUST BE COMPLETED. US EPA'S AP-42, SECTION 7.1, "ORGANIC LIQUID STORAGE TANKS," MAY ALSO BE USED TO ESTIMATE VOC AND HAP EMISSIONS (<a href="https://www.epa.gov/tnn/chief/">http://www.epa.gov/tnn/chief/</a>).

Bulk Storage Area Name	2. Tank Name		
	Produced Water Storage Tank		
Tank Equipment Identification No. (as assigned on Equipment List Form)  PTK-1			
5. Date of Commencement of Construction (for existing	tanks) 2015		
6. Type of change	New Stored Material		
7. Description of Tank Modification (if applicable) Updated production			
7A. Does the tank have more than one mode of operatio (e.g. Is there more than one product stored in the tar	nk?)		
7B. If YES, explain and identify which mode is covered by this application (Note: A separate form must be completed for each mode).			
7C. Provide any limitations on source operation affecting variation, etc.):	emissions, any work practice standards (e.g. production		
II. TANK INFORM	IATION (required)		
height.	the internal cross-sectional area multiplied by internal 00-bbl		
9A. Tank Internal Diameter (ft)	9B. Tank Internal Height (or Length) (ft)		
12	20		
10A. Maximum Liquid Height (ft)	10B. Average Liquid Height (ft)		
19	14		
11A. Maximum Vapor Space Height (ft)	11B. Average Vapor Space Height (ft)		
1	6.57		
liquid levels and overflow valve heights.	is also known as "working volume" and considers design 074 gal		

13A. Maximum annual throughput (gal/yr)	13B. Maximum daily throughput (gal/day)
1,277,500	3,500
14. Number of Turnovers per year (annual net throughp	ut/maximum tank liquid volume) 79.47
15. Maximum tank fill rate (gal/min) N/A	
16. Tank fill method Submerged	☐ Splash ☐ Bottom Loading
17. Complete 17A and 17B for Variable Vapor Space Ta	
17A. Volume Expansion Capacity of System (gal)	17B. Number of transfers into system per year
other (describe)  External Floating Roof pontoon roof Domed External (or Covered) Floating Roof Internal Floating Roof vertical column so	upport self-supporting
<ul><li>☐ Variable Vapor Space lifter roof</li><li>☐ Pressurized spherical cylindrica</li><li>☐ Underground</li><li>☐ Other (describe)</li></ul>	
	ATION (optional if providing TANKS Summary Sheets)
<ul><li>19. Tank Shell Construction:</li><li></li></ul>	d rivets
20A. Shell Color White 20B. Roof Colo	
21. Shell Condition (if metal and unlined):  ☑ No Rust ☐ Light Rust ☐ Dense R	tust
22A. Is the tank heated?   YES   NO	
22B. If YES, provide the operating temperature (°F)	
22C. If YES, please describe how heat is provided to t	ank.
23. Operating Pressure Range (psig): 14.7 to 14.7	
24. Complete the following section for Vertical Fixed Ro	of Tanks Does Not Apply
24A. For dome roof, provide roof radius (ft)	
24B. For cone roof, provide slope (ft/ft) 0.06	
25. Complete the following section for Floating Roof Tai	nks Does Not Apply
25A. Year Internal Floaters Installed:	
25B. Primary Seal Type: ☐ Metallic (Mechanical) (check one) ☐ Vapor Mounted Resil	<b>— ·</b>
25C. Is the Floating Roof equipped with a Secondary S	Seal? YES NO
25D. If YES, how is the secondary seal mounted? (che	eck one) Shoe Rim Other (describe):
25E. Is the Floating Roof equipped with a weather shie	eld? YES NO

25F. Describe deck fittings; indicate the number of each type of fitting:			
BOLT COVER, GASKETED:	ACCESS HATCH UNBOLTED COVER, GASKETED: UNBOLTED COVER, UNGASKETED:		
	AUTOMATIC GAL	JGE FLOAT WELL	
BOLT COVER, GASKETED:	UNBOLTED COV		UNBOLTED COVER, UNGASKETED:
	COLUM	IN WELL	1
BUILT-UP COLUMN – SLIDING COVER, GASKETED:		JMN - SLIDING	PIPE COLUMN – FLEXIBLE FABRIC SLEEVE SEAL:
	LADDE	R WELL	
PIP COLUMN – SLIDING COVER, G			SLIDING COVER, UNGASKETED:
	GAUGE-HATCH	I/SAMPLE PORT	
SLIDING COVER, GASKETED:		SLIDING COVER,	UNGASKETED:
	ROOF LEG OR	HANGER WELL	
WEIGHTED MECHANICAL ACTUATION, GASKETED:		MECHANICAL	SAMPLE WELL-SLIT FABRIC SEAL (10% OPEN AREA)
	VACHUM	DDE A KED	
VACUUM BREAKER WEIGHTED MECHANICAL ACTUATION, GASKETED:   WEIGHTED MECHANICAL ACTUATION, UNGASKETED:			
	DIM	  /ENT	
RIM VENT WEIGHTED MECHANICAL ACTUATION GASKETED: WEIGHTED MECHANICAL ACTUATION, UNGASKETED:			
	DECK DRAIN (3-I	NCH DIAMETER)	
OPEN:	DEGREDIVIN (0-1	90% CLOSED:	
STUB DRAIN			
1-INCH DIAMETER:			
OTHER (DESCRIBE, ATTACH ADDITIONAL PAGES IF NECESSARY)			
OTHER (BEGGRIBE, ATTAGITABBITIONAL PAGES II NEGESSART)			

26. Complete the following section for Internal Floating I	Roof Tanks Does Not Apply
26A. Deck Type:   Bolted   Welded	
26B. For Bolted decks, provide deck construction:	
26C. Deck seam:  Continuous sheet construction 5 feet wide Continuous sheet construction 6 feet wide Continuous sheet construction 7 feet wide Continuous sheet construction 5 × 7.5 feet wide Continuous sheet construction 5 × 12 feet wide Other (describe)	
26D. Deck seam length (ft)	26E. Area of deck (ft²)
For column supported tanks:	26G. Diameter of each column:
26F. Number of columns:	if and idia a TANKO Common Objects
27. Provide the city and state on which the data in this so	if providing TANKS Summary Sheets)
Charleston, WV	Solion are based.
28. Daily Average Ambient Temperature (°F)	
29. Annual Average Maximum Temperature (°F)	
30. Annual Average Minimum Temperature (°F)	-
31. Average Wind Speed (miles/hr)	
32. Annual Average Solar Insulation Factor (BTU/(ft²-day	())
33. Atmospheric Pressure (psia)	
V. LIQUID INFORMATION (optional	f providing TANKS Summary Sheets)
34. Average daily temperature range of bulk liquid:	
34A. Minimum (°F)	34B. Maximum (°F)
35. Average operating pressure range of tank:	
35A. Minimum (psig)	35B. Maximum (psig)
36A. Minimum Liquid Surface Temperature (°F)	36B. Corresponding Vapor Pressure (psia)
37A. Average Liquid Surface Temperature (°F)	37B. Corresponding Vapor Pressure (psia)
38A. Maximum Liquid Surface Temperature (°F)	38B. Corresponding Vapor Pressure (psia)
39. Provide the following for each liquid or gas to be store	ed in tank. Add additional pages if necessary.
39A. Material Name or Composition	
39B. CAS Number	
39C. Liquid Density (lb/gal)	
39D. Liquid Molecular Weight (lb/lb-mole)	
39E. Vapor Molecular Weight (lb/lb-mole)	

Maximum Vapor Press 39F. True (psia)	sure				
39G. Reid (psia)					
Months Storage per Y	ear	+			
39H. From	Cai				
39I. To					
	VI. EMISSIONS A	ND CONTR	OL DEVICE	DATA (required)	
40 Emission Control I	Devices (check as man				
☐ Carbon Adsorp	•	j do appij/.			
☐ Condenser¹	70011				
_	(ont (noig)				
☐ Conservation \			Dragging C	ottina	
Vacuum S	•		Pressure Se	etung	
	lief Valve (psig)				
☐ Inert Gas Blank					
☐ Insulation of Ta					
Liquid Absorpti					
Refrigeration o					
Rupture Disc (p					
☐ Vent to Incinera	ator <sup>1</sup>				
Other¹ (describ	e): Flare				
<sup>1</sup> Complete approp	oriate Air Pollution Cont	rol Device S	Sheet.		
41 Expected Emission	D ( ( ) "T (D				
TT. Expedica Ellission	n Rate (submit Test Da	ta or Calcula	ations here	or elsewhere in the a	oplication).
		ı	1		
Material Name & CAS No.	Breathing Loss (lb/hr)	ta or Calcula  Workin  Amount	1	or elsewhere in the a Annual Loss (lb/yr)	Estimation Method <sup>1</sup>
Material Name &	Breathing Loss (lb/hr) See Attachment N,	Workin	g Loss	Annual Loss	
Material Name &	Breathing Loss (lb/hr)	Workin	g Loss	Annual Loss	
Material Name &	Breathing Loss (lb/hr) See Attachment N,	Workin	g Loss	Annual Loss	
Material Name &	Breathing Loss (lb/hr) See Attachment N,	Workin	g Loss	Annual Loss	
Material Name &	Breathing Loss (lb/hr) See Attachment N,	Workin	g Loss	Annual Loss	
Material Name &	Breathing Loss (lb/hr) See Attachment N,	Workin	g Loss	Annual Loss	
Material Name &	Breathing Loss (lb/hr) See Attachment N,	Workin	g Loss	Annual Loss	
Material Name &	Breathing Loss (lb/hr) See Attachment N,	Workin	g Loss	Annual Loss	
Material Name &	Breathing Loss (lb/hr) See Attachment N,	Workin	g Loss	Annual Loss	
Material Name &	Breathing Loss (lb/hr) See Attachment N,	Workin	g Loss	Annual Loss	
Material Name &	Breathing Loss (lb/hr) See Attachment N,	Workin	g Loss	Annual Loss	
Material Name &	Breathing Loss (lb/hr) See Attachment N,	Workin	g Loss	Annual Loss	
Material Name &	Breathing Loss (lb/hr) See Attachment N,	Workin	g Loss	Annual Loss	
Material Name &	Breathing Loss (lb/hr) See Attachment N,	Workin	g Loss	Annual Loss	

 $<sup>^1</sup>$  EPA = EPA Emission Factor, MB = Material Balance, SS = Similar Source, ST = Similar Source Test, Throughput Data, O = Other (specify)

 $<sup>\</sup>boxtimes$  Remember to attach emissions calculations, including TANKS Summary Sheets if applicable.

Provide the following information for <u>each</u> new or modified bulk liquid storage tank as shown on the *Equipment List Form* and other parts of this application. A tank is considered modified if the material to be stored in the tank is different from the existing stored liquid.

IF USING US EPA'S TANKS EMISSION ESTIMATION PROGRAM (AVAILABLE AT <a href="https://www.epa.gov/tnn/tanks.html">www.epa.gov/tnn/tanks.html</a>), APPLICANT MAY ATTACH THE SUMMARY SHEETS IN LIEU OF COMPLETING SECTIONS III, IV, & V OF THIS FORM. HOWEVER, SECTIONS I, II, AND VI OF THIS FORM MUST BE COMPLETED. US EPA'S AP-42, SECTION 7.1, "ORGANIC LIQUID STORAGE TANKS," MAY ALSO BE USED TO ESTIMATE VOC AND HAP EMISSIONS (<a href="https://www.epa.gov/tnn/chief/">http://www.epa.gov/tnn/chief/</a>).

Bulk Storage Area Name	2. Tank Name
	Produced Water Storage Tank
3. Tank Equipment Identification No. (as assigned on	
Equipment List Form)	Equipment List Form)
PTK-2	19E
5. Date of Commencement of Construction (for existing	tanks) 2015
6. Type of change ☐ New Construction ☐ N	New Stored Material
7. Description of Tank Modification (if applicable)	
Updated production	
7A. Does the tank have more than one mode of operation	n? ☐ Yes ☒ No
(e.g. Is there more than one product stored in the tan	
	ed by this application (Note: A separate form must be
completed for each mode).	
7C. Provide any limitations on source operation affecting	emissions, any work practice standards (e.g. production
variation, etc.):	
II. TANK INFORM	ATION (required)
	the internal cross-sectional area multiplied by internal
height.	20.111
9A. Tank Internal Diameter (ft)	00-bbl
` ,	9B. Tank Internal Height (or Length) (ft)
12 10A. Maximum Liquid Height (ft)	20 10B. Average Liquid Height (ft)
19	10B. Average Liquid Height (ft)  14
11A. Maximum Vapor Space Height (ft)	11B. Average Vapor Space Height (ft)
1	6.57
12. Nominal Capacity (specify barrels or gallons). This i	
liquid levels and overflow valve heights.	a disc known as working volune and considers design
	074 gal

13A. Maximum annual throughput (gal/yr)	13B. Maximum daily throughput (gal/day)	
1,277,500	3,500	
14. Number of Turnovers per year (annual net throughpu	ut/maximum tank liquid volume) 79.47	
15. Maximum tank fill rate (gal/min) N/A		
16. Tank fill method ⊠ Submerged	☐ Splash ☐ Bottom Loading	
17. Complete 17A and 17B for Variable Vapor Space Ta	nk Systems	
17A. Volume Expansion Capacity of System (gal)	17B. Number of transfers into system per year	
18. Type of tank (check all that apply):  ☐ Fixed Roof x vertical horizontal  other (describe)  ☐ External Floating Roof pontoon roof  ☐ Domed External (or Covered) Floating Roof  ☐ Internal Floating Roof vertical column su	double deck roof	
<ul><li>☐ Variable Vapor Space lifter roof</li><li>☐ Pressurized spherical cylindrical</li><li>☐ Underground</li><li>☐ Other (describe)</li></ul>		
III. TANK CONSTRUCTION & OPERATION INFORM	ATION (optional if providing TANKS Summary Sheets)	
19. Tank Shell Construction:  ☐ Riveted ☐ Gunite lined ☐ Epoxy-coated	d rivets	
20A. Shell Color White 20B. Roof Color	White 20C. Year Last Painted	
21. Shell Condition (if metal and unlined):  ☑ No Rust ☐ Light Rust ☐ Dense R	ust	
22A. Is the tank heated? ☐ YES ☒ NO		
22B. If YES, provide the operating temperature (°F)		
22C. If YES, please describe how heat is provided to tank.		
23. Operating Pressure Range (psig): 14.7 to 14.7		
24. Complete the following section for Vertical Fixed Ro	of Tanks Does Not Apply	
24A. For dome roof, provide roof radius (ft)		
24B. For cone roof, provide slope (ft/ft) 0.06		
25. Complete the following section for Floating Roof Tar	nks Does Not Apply	
25A. Year Internal Floaters Installed:		
25B. Primary Seal Type:		
25C. Is the Floating Roof equipped with a Secondary S	Seal? YES NO	
25D. If YES, how is the secondary seal mounted? (che	eck one) Shoe Rim Other (describe):	
25E. Is the Floating Roof equipped with a weather shie	eld? YES NO	

25F. Describe deck fittings; indica	te the number of ea	ch type of fitting:	
2 october dook manage, manage		S HATCH	
BOLT COVER, GASKETED:	UNBOLTED COV		UNBOLTED COVER, UNGASKETED:
	ALITOMATIC CAL	JGE FLOAT WELL	
BOLT COVER, GASKETED:	UNBOLTED COV		UNBOLTED COVER, UNGASKETED:
	6011114	IN WELL	1
BUILT-UP COLUMN – SLIDING COVER, GASKETED:		JMN - SLIDING	PIPE COLUMN – FLEXIBLE FABRIC SLEEVE SEAL:
	LADDE	R WELL	-
PIP COLUMN – SLIDING COVER, G			SLIDING COVER, UNGASKETED:
	GAUGE-HATCH	I/SAMPLE PORT	
SLIDING COVER, GASKETED:	6/100E 11/110I	SLIDING COVER,	UNGASKETED:
	POOF LEG OP	HANGER WELL	
WEIGHTED MECHANICAL ACTUATION, GASKETED:	· ·	MECHANICAL	SAMPLE WELL-SLIT FABRIC SEAL (10% OPEN AREA)
	VACUUM	BREAKER	
WEIGHTED MECHANICAL ACTUAT			ANICAL ACTUATION, UNGASKETED:
	DIM \	⊹ VENT	
WEIGHTED MECHANICAL ACTUAT			ANICAL ACTUATION, UNGASKETED:
	DECK DRAIN (3-I	NCH DIAMETER)	
OPEN:	DECK DIVAIN (5-1	90% CLOSED:	
	STUB	DRAIN	
1-INCH DIAMETER:	3108	DIVAIN	
OTHER (DESC	RIBE, ATTACH ADD	DITIONAL PAGES I	F NECESSARY)
OTTLIN (BEOOF	NDE, ATTAOTTADE	THORAL FACES F	T NEGEOGANT)

26. Complete the following section for Internal Floating F	Roof Tanks
26A. Deck Type: ☐ Bolted ☐ Welded	
26B. For Bolted decks, provide deck construction:	
26C. Deck seam:	
Continuous sheet construction 5 feet wide Continuous sheet construction 6 feet wide	
Continuous sheet construction 7 feet wide	
☐ Continuous sheet construction 5 × 7.5 feet wide ☐ Continuous sheet construction 5 × 12 feet wide	
Other (describe)	
26D. Deck seam length (ft)	26E. Area of deck (ft²)
For column supported tanks:	26G. Diameter of each column:
26F. Number of columns:	I f providing TANKS Summary Sheets)
27. Provide the city and state on which the data in this se	
Charleston, WV	
28. Daily Average Ambient Temperature (°F)	
29. Annual Average Maximum Temperature (°F)	
30. Annual Average Minimum Temperature (°F)	
31. Average Wind Speed (miles/hr)	
32. Annual Average Solar Insulation Factor (BTU/(ft²-day	())
33. Atmospheric Pressure (psia)	
V. LIQUID INFORMATION (optional	f providing TANKS Summary Sheets)
34. Average daily temperature range of bulk liquid:	
34A. Minimum (°F)	34B. Maximum (°F)
35. Average operating pressure range of tank:	
35A. Minimum (psig)	35B. Maximum (psig)
36A. Minimum Liquid Surface Temperature (°F)	36B. Corresponding Vapor Pressure (psia)
37A. Average Liquid Surface Temperature (°F)	37B. Corresponding Vapor Pressure (psia)
38A. Maximum Liquid Surface Temperature (°F)	38B. Corresponding Vapor Pressure (psia)
ook. Waximum Elquid ourlace Temperature ( 1 )	Concesponding vapor resource (polar)
39. Provide the following for <u>each</u> liquid or gas to be store	ed in tank. Add additional pages if necessary.
39A. Material Name or Composition	
39B. CAS Number	
39C. Liquid Density (lb/gal)	
39D. Liquid Molecular Weight (lb/lb-mole)	
39E. Vapor Molecular Weight (lb/lb-mole)	

Maximum Vapor Pres	sure								
39F. True (psia)									
39G. Reid (psia)  Months Storage per Y	'ear								
39H. From	Cai								
39I. To									
	VI. EMISSIONS A	ND CONTE	ROL DEVIC	E DATA (required)					
40 Emission Control	Devices (check as man								
☐ Carbon Adsorp		y as apply).		лстрріу					
☐ Condenser¹	50011								
☐ Conservation \	/ent (neig)								
Vacuum S			Dragouna C	n Addison ou					
1	elief Valve (psig)		Pressure S	etting					
☐ Inert Gas Blanl									
☐ Insulation of Ta									
Liquid Absorpti	` '								
Refrigeration o									
Rupture Disc (									
☐ Vent to Inciner									
Other¹ (describ	,								
<sup>1</sup> Complete approp	oriate Air Pollution Cont	rol Device S	Sheet.						
41. Expected Emission	n Rate (submit Test Da	1 Complete appropriate Air Pollution Control Device Sheet.  41. Expected Emission Rate (submit Test Data or Coloulations here as also where in the small is the small in the							
41. Expected Emission Rate (submit Test Data or Calculations here or elsewhere in the application).									
Material Name &	1	Workin	1						
	Breathing Loss (lb/hr)	1	1	or elsewhere in the ap Annual Loss (lb/yr)	Estimation Method <sup>1</sup>				
Material Name &	Breathing Loss (lb/hr)	Workin	g Loss	Annual Loss					
Material Name &	Breathing Loss	Workin	g Loss	Annual Loss					
Material Name &	Breathing Loss (lb/hr) See Attachment N,	Workin	g Loss	Annual Loss					
Material Name &	Breathing Loss (lb/hr) See Attachment N,	Workin	g Loss	Annual Loss					
Material Name &	Breathing Loss (lb/hr) See Attachment N,	Workin	g Loss	Annual Loss					
Material Name &	Breathing Loss (lb/hr) See Attachment N,	Workin	g Loss	Annual Loss					
Material Name &	Breathing Loss (lb/hr) See Attachment N,	Workin	g Loss	Annual Loss					
Material Name &	Breathing Loss (lb/hr) See Attachment N,	Workin	g Loss	Annual Loss					
Material Name &	Breathing Loss (lb/hr) See Attachment N,	Workin	g Loss	Annual Loss					
Material Name &	Breathing Loss (lb/hr) See Attachment N,	Workin	g Loss	Annual Loss					
Material Name &	Breathing Loss (lb/hr) See Attachment N,	Workin	g Loss	Annual Loss					
Material Name &	Breathing Loss (lb/hr) See Attachment N,	Workin	g Loss	Annual Loss					
Material Name &	Breathing Loss (lb/hr) See Attachment N,	Workin	g Loss	Annual Loss					
Material Name &	Breathing Loss (lb/hr) See Attachment N,	Workin	g Loss	Annual Loss					

<sup>&</sup>lt;sup>1</sup> EPA = EPA Emission Factor, MB = Material Balance, SS = Similar Source, ST = Similar Source Test, Throughput Data, O = Other (specify)

 $<sup>{</sup>f igstyle Z}$  Remember to attach emissions calculations, including TANKS Summary Sheets if applicable.

Provide the following information for <u>each</u> new or modified bulk liquid storage tank as shown on the *Equipment List Form* and other parts of this application. A tank is considered modified if the material to be stored in the tank is different from the existing stored liquid.

IF USING US EPA'S TANKS EMISSION ESTIMATION PROGRAM (AVAILABLE AT <a href="https://www.epa.gov/tnn/tanks.html">www.epa.gov/tnn/tanks.html</a>), APPLICANT MAY ATTACH THE SUMMARY SHEETS IN LIEU OF COMPLETING SECTIONS III, IV, & V OF THIS FORM. HOWEVER, SECTIONS I, II, AND VI OF THIS FORM MUST BE COMPLETED. US EPA'S AP-42, SECTION 7.1, "ORGANIC LIQUID STORAGE TANKS," MAY ALSO BE USED TO ESTIMATE VOC AND HAP EMISSIONS (<a href="https://www.epa.gov/tnn/chief/">http://www.epa.gov/tnn/chief/</a>).

1.	Bulk Storage Area Name	2.	Tank Name					
			Produced Water Storage Tank					
3.	Tank Equipment Identification No. (as assigned on Equipment List Form)	4.	Emission Point Identification No. (as assigned on Equipment List Form)					
	PTK-3	20E						
5.	Date of Commencement of Construction (for existing	tank	(s) 2015					
6.	Type of change    New Construction	lew	Stored Material					
7.	Description of Tank Modification (if applicable)							
l	Updated production							
7A.	Does the tank have more than one mode of operation	1?	☐ Yes         No					
	(e.g. Is there more than one product stored in the tan	,	<del>-</del>					
7B.	If YES, explain and identify which mode is covere completed for each mode).	d b	y this application (Note: A separate form must be					
	completed for each mode).		i					
			!					
70	Provide any limitations on source energian effection	:						
/ 0.	Provide any limitations on source operation affecting variation, etc.):	emi	ssions, any work practice standards (e.g. production					
	II. TANK INFORM	ATIC	ON (required)					
8.	Design Capacity (specify barrels or gallons). Use							
	height.	0	mornar cross sectional area manipled by internal					
		0-bb						
9A.	Tank Internal Diameter (ft)	9B.	Tank Internal Height (or Length) (ft)					
40.4	12		20					
10A		10B	5 1 1 1 3 1 1 3 1 1 1 1 1					
444	19		14					
11A	. Maximum Vapor Space Height (ft)	11B	3   1   1   1   1   1   1   1   1   1					
10	Newinal Constitutes with the self-self-self-self-self-self-self-self-		6.57					
12.	Nominal Capacity (specify barrels or gallons). This is liquid levels and overflow valve heights.	s als	o known as "working volume" and considers design					
	•	)74 g	gal					

13A. Maximum annual throughput (gal/yr)	13B. Maximum daily throughput (gal/day)			
1,277,500	3,500			
14. Number of Turnovers per year (annual net throughp	79.47			
15. Maximum tank fill rate (gal/min) N/A				
16. Tank fill method Submerged	Splash Bottom Loading			
17. Complete 17A and 17B for Variable Vapor Space Ta				
17A. Volume Expansion Capacity of System (gal)	17B. Number of transfers into system per year			
18. Type of tank (check all that apply):  ☐ Fixed Roof x vertical horizontal	double deck roof upport self-supporting diaphragm			
III. TANK CONSTRUCTION & OPERATION INFORM	MATION (optional if providing TANKS Summary Sheets)			
19. Tank Shell Construction:  ☐ Riveted ☐ Gunite lined ☐ Epoxy-coate				
20A. Shell Color White 20B. Roof Colo				
21. Shell Condition (if metal and unlined):  ☑ No Rust ☐ Light Rust ☐ Dense R	Rust			
22A. Is the tank heated? ☐ YES ☒ NO				
22B. If YES, provide the operating temperature (°F)				
22C. If YES, please describe how heat is provided to	tank.			
23. Operating Pressure Range (psig): 14.7 to 14.7				
24. Complete the following section for Vertical Fixed Ro	Does Not Apply			
24A. For dome roof, provide roof radius (ft)				
24B. For cone roof, provide slope (ft/ft) 0.06				
25. Complete the following section for Floating Roof Ta	nks Does Not Apply			
25A. Year Internal Floaters Installed:				
25B. Primary Seal Type:				
25C. Is the Floating Roof equipped with a Secondary	Seal? YES NO			
25D. If YES, how is the secondary seal mounted? (che	eck one) Shoe Rim Other (describe):			
25E. Is the Floating Roof equipped with a weather shi	eld? YES NO			

25F. Describe deck fittings; indicate	te the number of ea	ch type of fitting:	· · · · · · · · · · · · · · · · · · ·
20. 1 Booth a door mange, malea		S HATCH	
BOLT COVER, GASKETED:	UNBOLTED COV		UNBOLTED COVER, UNGASKETED:
	AUTOMATIC GAL	JGE FLOAT WELL	<u> </u>
BOLT COVER, GASKETED:	UNBOLTED COV		UNBOLTED COVER, UNGASKETED:
	COLUM	N WELL	i
BUILT-UP COLUMN – SLIDING COVER, GASKETED:		JMN - SLIDING	PIPE COLUMN – FLEXIBLE FABRIC SLEEVE SEAL:
	LADDE	R WELL	
PIP COLUMN ~ SLIDING COVER, G		·	SLIDING COVER, UNGASKETED:
	GAUGE-HATCH	/SAMPLE PORT	
SLIDING COVER, GASKETED:	G, (GGE 11), (1 G).	SLIDING COVER,	UNGASKETED:
	ROOF LEG OR	HANGER WELL	·
WEIGHTED MECHANICAL ACTUATION, GASKETED:		MECHANICAL	SAMPLE WELL-SLIT FABRIC SEAL (10% OPEN AREA)
WEIGHTED MECHANICAL ACTUATI	VACUUM ION, GASKETED:		NICAL ACTUATION, UNGASKETED:
	RIM \	/ENT	
WEIGHTED MECHANICAL ACTUATI			NICAL ACTUATION, UNGASKETED:
	DECK DRAIN (3-I	NCH DIAMETER\	
OPEN:		90% CLOSED:	
	STUB I	DRAIN	
1-INCH DIAMETER:	01051	STO (III)	
OTHER (DESCR	RIBE, ATTACH ADD	DITIONAL PAGES II	F NECESSARY)

26A. Deck Type:  Bolited  Welded 26B. For Bolted decks, provide deck construction:  26C. Deck seam:  Continuous sheet construction 5 feet wide  Continuous sheet construction 6 feet wide  Continuous sheet construction 5 × 7.5 feet wide  Continuous sheet construction 5 × 7.5 feet wide  Continuous sheet construction 5 × 7.5 feet wide  Continuous sheet construction 5 × 12 feet wide  Continuous sheet construction 5	26. Complete the following section for Internal Floating	g Roof Tanks 🔲 Does Not Apply
26C. Deck seam:    Continuous sheet construction 5 feet wide		
Continuous sheet construction 5 feet wide Continuous sheet construction 6 feet wide Continuous sheet construction 7 feet wide Continuous sheet construction 7 feet wide Continuous sheet construction 5 × 7.5 feet wide Continuous sheet construction 5 × 7.5 feet wide Continuous sheet construction 5 × 12 feet wide Continuous sheet columns: Chall providing TANKS Summary Sheets  Charleston, W Charleston,	71	
Continuous sheet construction 5 feet wide Continuous sheet construction 6 feet wide Continuous sheet construction 7 feet wide Continuous sheet construction 7 feet wide Continuous sheet construction 5 × 7.5 feet wide Continuous sheet construction 5 × 7.5 feet wide Continuous sheet construction 5 × 12 feet wide Continuous sheet columns: Chall providing TANKS Summary Sheets  Charleston, W Charleston,		
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Continuous sheet construction 7 feet wide Continuous sheet construction 5 × 7.5 feet wide Continuous sheet construction 5 × 12 feet wide Cother (describe)  26E. Area of deck (ft²) For column supported tanks: 26F. Number of columns:  V. SITE INFORMANTION (optional if providing TANKS Summary Sheets)  27. Provide the city and state on which the data in this section are based. Charleston, WV  28. Daily Average Ambient Temperature (°F) 29. Annual Average Maximum Temperature (°F) 30. Annual Average Minimum Temperature (°F) 31. Average Wind Speed (miles/hr) 32. Annual Average Solar Insulation Factor (BTU/(ft²-day)) 33. Atmospheric Pressure (psia)  V. LIQUID INFORMATION (optional if providing TANKS Summary Sheets)  44. Average daily temperature range of bulk liquid: 34A. Minimum (°F) 34B. Maximum (°F) 35. Average operating pressure range of tank: 35A. Minimum (psig) 36A. Minimum (psig) 37A. Average Liquid Surface Temperature (°F) 37B. Corresponding Vapor Pressure (psia) 37A. Average Liquid Surface Temperature (°F) 38B. Corresponding Vapor Pressure (psia) 39. Provide the following for each liquid or gas to be stored in tank. Add additional pages if necessary. 39A. Material Name or Composition 39B. CAS Number 39C. Liquid Density (lb/gal) 39D. Liquid Molecular Weight (lb/lb-mole)	_	
Continuous sheet construction 5 × 7.5 feet wide Continuous sheet construction 5 × 12 feet wide Other (describe)  26B. Area of deck (ft²)  26G. Diameter of each column:  IV. SITE INFORMANTION (optional if providing TANKS Summary Sheets)  27. Provide the city and state on which the data in this section are based. Charleston, WV  28. Daily Average Ambient Temperature (°F)  29. Annual Average Maximum Temperature (°F)  30. Annual Average Minimum Temperature (°F)  31. Average Wind Speed (miles/hr)  32. Annual Average Solar Insulation Factor (BTU/(ft²-day))  33. Atmospheric Pressure (psia)  V. LIQUID INFORMATION (optional if providing TANKS Summary Sheets)  34. Average daily temperature range of bulk liquid:  34A. Minimum (°F)  35. Average operating pressure range of tank:  35A. Minimum (psig)  36A. Minimum (psig)  36B. Corresponding Vapor Pressure (psia)  37A. Average Liquid Surface Temperature (°F)  38B. Corresponding Vapor Pressure (psia)  39B. CAS Number  39C. Liquid Density (lb/gal)  39D. Liquid Molecular Weight (lb/lb-mole)	I =	
Continuous sheet construction 5 × 12 feet wide Other (describe)  26E. Area of deck (ft²)  For column supported tanks: 26F. Number of columns:  IV. SITE INFORMANTION (optional if providing TANKS Summary Sheets)  27. Provide the city and state on which the data in this section are based. Charleston, WV  28. Daily Average Ambient Temperature (°F)  29. Annual Average Maximum Temperature (°F)  30. Annual Average Minimum Temperature (°F)  31. Average Wind Speed (miles/hr)  32. Annual Average Solar Insulation Factor (BTU/(ft²-day))  33. Atmospheric Pressure (psia)  V. LIQUID INFORMATION (optional if providing TANKS Summary Sheets)  34. Average daily temperature range of bulk liquid:  35A. Minimum (°F)  34B. Maximum (°F)  35. Average operating pressure range of tank:  35A. Minimum (psig)  36A. Minimum Liquid Surface Temperature (°F)  37B. Corresponding Vapor Pressure (psia)  37A. Average Liquid Surface Temperature (°F)  38B. Corresponding Vapor Pressure (psia)  39. Provide the following for each liquid or gas to be stored in tank. Add additional pages if necessary.  39A. Material Name or Composition  39B. CAS Number  39C. Liquid Density (lb/gal)  39D. Liquid Molecular Weight (lb/lb-mole)		Δ
26D. Deck seam length (ft) 26E. Area of deck (ft²) For column supported tanks: 26F. Number of columns:  IV. SITE INFORMANTION (optional if providing TANKS Summary Sheets)  27. Provide the city and state on which the data in this section are based. Charleston, WV  28. Daily Average Ambient Temperature (°F) 29. Annual Average Maximum Temperature (°F) 30. Annual Average Minimum Temperature (°F) 31. Average Wind Speed (miles/hr) 32. Annual Average Solar Insulation Factor (BTU/(ft²-day)) 33. Atmospheric Pressure (psia)  V. LIQUID INFORMATION (optional if providing TANKS Summary Sheets)  34. Average daily temperature range of bulk liquid: 34A. Minimum (°F) 35. Average operating pressure range of tank: 35A. Minimum (psig) 35B. Maximum (psig) 36A. Minimum Liquid Surface Temperature (°F) 37B. Corresponding Vapor Pressure (psia) 37A. Average Liquid Surface Temperature (°F) 38B. Corresponding Vapor Pressure (psia) 39B. Provide the following for each liquid or gas to be stored in tank. Add additional pages if necessary. 39A. Material Name or Composition 39B. CAS Number 39C. Liquid Density (lb/gal) 39D. Liquid Molecular Weight (lb/lb-mole)	_	
For column supported tanks: 26F. Number of columns:  IV. SITE INFORMANTION (optional if providing TANKS Summary Sheets)  27. Provide the city and state on which the data in this section are based. Charleston, WV  28. Daily Average Ambient Temperature (°F)  29. Annual Average Maximum Temperature (°F)  30. Annual Average Minimum Temperature (°F)  31. Average Wind Speed (miles/hr)  32. Annual Average Solar Insulation Factor (BTU/(ft²-day))  33. Atmospheric Pressure (psia)  V. LIQUID INFORMATION (optional if providing TANKS Summary Sheets)  34. Average daily temperature range of bulk liquid:  34A. Minimum (°F)  34B. Maximum (°F)  35. Average operating pressure range of tank:  35A. Minimum (psig)  36A. Minimum Liquid Surface Temperature (°F)  37B. Corresponding Vapor Pressure (psia)  37A. Average Liquid Surface Temperature (°F)  38B. Corresponding Vapor Pressure (psia)  39. Provide the following for each liquid or gas to be stored in tank. Add additional pages if necessary.  39A. Material Name or Composition  39B. CAS Number  39C. Liquid Density (lb/gal)  39D. Liquid Molecular Weight (lb/lb-mole)	Other (describe)	
For column supported tanks: 26F. Number of columns:  IV. SITE INFORMANTION (optional if providing TANKS Summary Sheets)  27. Provide the city and state on which the data in this section are based. Charleston, WV  28. Daily Average Ambient Temperature (°F)  29. Annual Average Maximum Temperature (°F)  30. Annual Average Minimum Temperature (°F)  31. Average Wind Speed (miles/hr)  32. Annual Average Solar Insulation Factor (BTU/(ft²-day))  33. Atmospheric Pressure (psia)  V. LIQUID INFORMATION (optional if providing TANKS Summary Sheets)  34. Average daily temperature range of bulk liquid:  34A. Minimum (°F)  34B. Maximum (°F)  35. Average operating pressure range of tank:  35A. Minimum (psig)  36A. Minimum Liquid Surface Temperature (°F)  37B. Corresponding Vapor Pressure (psia)  37A. Average Liquid Surface Temperature (°F)  38B. Corresponding Vapor Pressure (psia)  39. Provide the following for each liquid or gas to be stored in tank. Add additional pages if necessary.  39A. Material Name or Composition  39B. CAS Number  39C. Liquid Density (lb/gal)  39D. Liquid Molecular Weight (lb/lb-mole)	26D. Deck seam length (ft)	26E. Area of deck (ft²)
IV. SITE INFORMANTION (optional if providing TANKS Summary Sheets)  27. Provide the city and state on which the data in this section are based. Charleston, WV  28. Daily Average Ambient Temperature (°F)  29. Annual Average Maximum Temperature (°F)  30. Annual Average Minimum Temperature (°F)  31. Average Wind Speed (miles/hr)  32. Annual Average Solar Insulation Factor (BTU/(ft²-day))  33. Atmospheric Pressure (psia)  V. LIQUID INFORMATION (optional if providing TANKS Summary Sheets)  34. Average daily temperature range of bulk liquid:  34A. Minimum (°F)  35. Average operating pressure range of tank:  35A. Minimum (psig)  36A. Minimum (psig)  37B. Corresponding Vapor Pressure (psia)  37A. Average Liquid Surface Temperature (°F)  37B. Corresponding Vapor Pressure (psia)  38A. Maximum Liquid Surface Temperature (°F)  38B. Corresponding Vapor Pressure (psia)  39. Provide the following for each liquid or gas to be stored in tank. Add additional pages if necessary.  39A. Material Name or Composition  39B. CAS Number  39C. Liquid Density (lb/gal)  39D. Liquid Molecular Weight (lb/lb-mole)	For column supported tanks:	26G. Diameter of each column:
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Charleston, WV  28. Daily Average Ambient Temperature (°F)  29. Annual Average Maximum Temperature (°F)  30. Annual Average Minimum Temperature (°F)  31. Average Wind Speed (miles/hr)  32. Annual Average Solar Insulation Factor (BTU/(ft²-day))  33. Atmospheric Pressure (psia)  V. LIQUID INFORMATION (optional if providing TANKS Summary Sheets)  34. Average daily temperature range of bulk liquid:  34A. Minimum (°F)  35B. Maximum (°F)  36B. Corresponding Vapor Pressure (psia)  37A. Average Liquid Surface Temperature (°F)  37B. Corresponding Vapor Pressure (psia)  37A. Average Liquid Surface Temperature (°F)  38B. Corresponding Vapor Pressure (psia)  39B. Provide the following for each liquid or gas to be stored in tank. Add additional pages if necessary.  39A. Material Name or Composition  39B. CAS Number  39C. Liquid Density (lb/gal)  39D. Liquid Molecular Weight (lb/lb-mole)	IV. SITE INFORMANTION (options	al if providing TANKS Summary Sheets)
28. Daily Average Ambient Temperature (°F)  29. Annual Average Maximum Temperature (°F)  30. Annual Average Minimum Temperature (°F)  31. Average Wind Speed (miles/hr)  32. Annual Average Solar Insulation Factor (BTU/(ft²-day))  33. Atmospheric Pressure (psia)  V. LIQUID INFORMATION (optional if providing TANKS Summary Sheets)  34. Average daily temperature range of bulk liquid:  34A. Minimum (°F)  35. Average operating pressure range of tank:  35A. Minimum (psig)  36A. Minimum Liquid Surface Temperature (°F)  36B. Corresponding Vapor Pressure (psia)  37A. Average Liquid Surface Temperature (°F)  38B. Corresponding Vapor Pressure (psia)  39B. Corresponding Vapor Pressure (psia)  39Provide the following for each liquid or gas to be stored in tank. Add additional pages if necessary.  39A. Material Name or Composition  39B. CAS Number  39C. Liquid Density (lb/gal)  39D. Liquid Molecular Weight (lb/lb-mole)	•	section are based.
29. Annual Average Maximum Temperature (°F) 30. Annual Average Minimum Temperature (°F) 31. Average Wind Speed (miles/hr) 32. Annual Average Solar Insulation Factor (BTU/(ft²-day)) 33. Atmospheric Pressure (psia)  V. LIQUID INFORMATION (optional if providing TANKS Summary Sheets)  34. Average daily temperature range of bulk liquid: 34A. Minimum (°F) 35. Average operating pressure range of tank: 35A. Minimum (psig) 35B. Maximum (psig) 36A. Minimum Liquid Surface Temperature (°F) 36B. Corresponding Vapor Pressure (psia) 37A. Average Liquid Surface Temperature (°F) 37B. Corresponding Vapor Pressure (psia) 38A. Maximum Liquid Surface Temperature (°F) 38B. Corresponding Vapor Pressure (psia) 39. Provide the following for each liquid or gas to be stored in tank. Add additional pages if necessary. 39A. Material Name or Composition 39B. CAS Number 39C. Liquid Density (lb/gal) 39D. Liquid Molecular Weight (lb/lb-mole)		
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39D. Liquid Molecular Weight (lb/lb-mole)	39B. CAS Number	
	39C. Liquid Density (lb/gal)	
	39D. Liquid Molecular Weight (lb/lb-mole)	
39E. Vapor Molecular Weight (Ib/Ib-mole)	39E. Vapor Molecular Weight (lb/lb-mole)	

Marriage Van de Duna				1			
Maximum Vapor Pres 39F. True (psia)	sure						
39G. Reid (psia)							
Months Storage per Y	ear						
39H. From							
39I. To							
	VI. EMISSIONS A	ND CONTR	OL DEVIC	E DATA (required)			
40. Emission Control	Devices (check as mar	ny as apply):	☐ Does No	ot Apply			
☐ Carbon Adsorp				.,,,			
☐ Condenser <sup>1</sup>							
☐ Conservation \	/ent (psia)						
Vacuum S			Pressure S	ettina			
l	lief Valve (psig)		. 10000010 0	oung			
☐ Inert Gas Blant	•,						
☐ Insulation of Ta							
☐ Liquid Absorpti							
Refrigeration o	,						
Rupture Disc (							
☐ Vent to Inciner							
_							
Other¹ (describ	•	haal Dandar O	NL 4				
	priate Air Pollution Conf						
41. Expected Emission Rate (submit Test Data or Calculations here or elsewhere in the application).							
Material Name &	Breathing Loss	Working		or elsewhere in the a			
	1	I .		I	Estimation Method <sup>1</sup>		
Material Name &	Breathing Loss (lb/hr)  See Attachment N,	Workin	g Loss	Annual Loss			
Material Name &	Breathing Loss (lb/hr)	Workin	g Loss	Annual Loss			
Material Name &	Breathing Loss (lb/hr)  See Attachment N,	Workin	g Loss	Annual Loss			
Material Name &	Breathing Loss (lb/hr)  See Attachment N,	Workin	g Loss	Annual Loss			
Material Name &	Breathing Loss (lb/hr)  See Attachment N,	Workin	g Loss	Annual Loss			
Material Name &	Breathing Loss (lb/hr)  See Attachment N,	Workin	g Loss	Annual Loss			
Material Name &	Breathing Loss (lb/hr)  See Attachment N,	Workin	g Loss	Annual Loss			
Material Name &	Breathing Loss (lb/hr)  See Attachment N,	Workin	g Loss	Annual Loss			
Material Name &	Breathing Loss (lb/hr)  See Attachment N,	Workin	g Loss	Annual Loss			
Material Name &	Breathing Loss (lb/hr)  See Attachment N,	Workin	g Loss	Annual Loss			
Material Name &	Breathing Loss (lb/hr)  See Attachment N,	Workin	g Loss	Annual Loss			

<sup>&</sup>lt;sup>1</sup> EPA = EPA Emission Factor, MB = Material Balance, SS = Similar Source, ST = Similar Source Test, Throughput Data, O = Other (specify)

Remember to attach emissions calculations, including TANKS Summary Sheets if applicable.

### Attachment L FUGITIVE EMISSIONS FROM UNPAVED HAULROADS

UNPAVED HAULROADS (including all equipment traffic involved in process, haul trucks, endloaders, etc.)

		PIVI	PM-10
k =	Particle size multiplier	0.80	0.36
s =	Silt content of road surface material (%)	10	10
p =	Number of days per year with precipitation >0.01 in.	150	150

Item Number	Description	Number of Wheels	Mean Vehicle Weight (tons)	Mean Vehicle Speed (mph)	Miles per Trip	Maximum Trips per Hour	Maximum Trips per Year	Control Device ID Number	Control Efficiency (%)
1	Light Vehicles	4	2.5	10	2	1	730	1	55
2	Heavy Trucks	18	23.7	10	2	1	730	1	55
3									
4									
5									
6									_
7									
8									

Source: AP-42 Fifth Edition - 13.2.2 Unpaved Roads

 $E = k \times 5.9 \times (s \div 12) \times (S \div 30) \times (W \div 3)^{0.7} \times (w \div 4)^{0.5} \times ((365 - p) \div 365) =$  lb/Vehicle Mile Traveled (VMT)

Where:

	<u>.                                    </u>	PM	PM-10
k =	Particle size multiplier	0.80	0.36
s =	Silt content of road surface material (%)	10	10
S=	Mean vehicle speed (mph)	10	10
W =	Mean vehicle weight (tons)	13	13
w =	Mean number of wheels per vehicle	11	11
p =	Number of days per year with precipitation >0.01 in.	150	150

For lb/hr:  $[lb \div VMT] \times [VMT \div trip] \times [Trips \div Hour] =$ lb/hr

For TPY:  $[lb \div VMT] \times [VMT \div trip] \times [Trips \div Hour] \times [Ton \div 2000 lb] =$ Tons/year

### SUMMARY OF UNPAVED HAULROAD EMISSIONS

		P	M		PM-10			
Item No.	Uncontrolled Controlled			rolled	Uncor	ntrolled	Controlled	
	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY	lb/hr	TPY
1	1.64	7.20	0.74	3.24	0.49	2.13	0.22	0.96
2			,					
3								
4								
5								
6								
7	-							
8								
TOTALS	1.64	7.20	0.74	3.24	0.49	2.13	0.22	0.96

Page 1 of 2

Revision 03/2007

#### **FUGITIVE EMISSIONS FROM PAVED HAULROADS**

INDUSTRIAL PAVED HAULROADS (including all equipment traffic involved in process, haul trucks, endloaders, etc.)

=	Industrial augmentation factor (dimensionless)	N/A
n =	Number of traffic lanes	
s =	Surface material silt content (%)	
L=	Surface dust loading (lb/mile)	<del>1</del> 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1

Item Number	Description	Mean Vehicle Weight (tons)	Miles per Trip	Maximum Trips per Hour	Maximum Trips per Year	Control Device ID Number	Control Efficiency (%)
1							
2							
3							
4	***						
5							
6							
7							
8							

Source: AP-42 Fifth Edition - 11.2.6 Industrial Paved Roads

 $E = 0.077 \times I \times (4 \div n) \times (s \div 10) \times (L \div 1000) \times (W \div 3)^{0.7} =$ 

Ib/Vehicle Mile Traveled (VMT)

#### Where:

=	Industrial augmentation factor (dimensionless)				
n =	Number of traffic lanes				
s =	Surface meterial silt content (%)				
L=	Surface dust loading (lb/mile)				
W =	Average vehicle weight (tons)				

For lb/hr:  $[lb \div VMT] \times [VMT \div trip] \times [Trips \div Hour] = lb/hr$ 

For TPY: [lb ÷ VMT] × [VMT ÷ trip] × [Trips ÷ Hour] × [Ton ÷ 2000 lb] = Tons/year

#### SUMMARY OF PAVED HAULROAD EMISSIONS

Item No.	Uncon	trolled	Controlled		
item No.	lb/hr	TPY	lb/hr	TPY	
1					
2					
3		·			
4					
5					
6		1			
7					
8					
TOTALS					

### Attachment M: Air Pollution Control Device Sheet(s)

### Attachment M Air Pollution Control Device Sheet

(FLARE SYSTEM)

Control Device ID No. (must match Emission Units Table): CTRL-1 **Equipment Information** 

_				
1.	Manufacturer: NOV	2. Method:		
	Model No. MEVC200	◯ Other Describe		
		Enclosed Vapor Combustor		
		•		
3.	Provide diagram(s) of unit describing capture syste capacity, horsepower of movers. If applicable, state	em with duct arrangement and size of duct, air volume, hood face velocity and hood collection efficiency.		
4.	Method of system used:			
_	☐ Steam-assisted ☐ Air-assisted	☐ Pressure-assisted ☐ Non-assisted		
5.	Maximum capacity of flare:	6. Dimensions of stack:		
	scf/min	Diameter 4 ft.		
	scf/hr	Height 20 ft.		
7.	Estimated combustion efficiency:	8. Fuel used in burners:		
	(Waste gas destruction efficiency)	⊠ Natural Gas		
	Estimated: 98 %	☐ Fuel Oil, Number		
_	Minimum guaranteed: 98 %	Other, Specify:		
9.	Number of burners:	11. Describe method of controlling flame: Two flame arrestors		
	Rating: 18.42 MM BTU/hr	1 wo frame arrestors		
10.	. Will preheat be used? ☐ Yes ☐ No			
12.	Flare height: 25 ft	14. Natural gas flow rate to flare pilot flame per pilot light: scf/min		
13.	Flare tip inside diameter: 0.75 ft	49.01961 scf/hr		
15.	Number of pilot lights:	16. Will automatic re-ignition be used?		
	Total 0.05 MM BTU/hr	⊠ Yes □ No		
17.	If automatic re-ignition will be used, describe the met The flare pilot switches shall automatically trig pilot.	hod: gger the ignition transformers to ignite the flare tip		
18.	Is pilot flame equipped with a monitor?  If yes, what type?  Ultra Violet  Other, Describe:	☐ No -Red era with monitoring control room		
19.	Hours of unit operation per year: 8,760			

# **Steam Injection**

20.	Will steam injection be used	d? ☐ Yes	⊠ No	21.	Steam pressure Minimum Expected:	PSIG				
_				_	Dasias Marineros					
22.	Total Steam flow rate:		LB/hr		Temperature:	°F				
24.	Velocity		ft/sec		Number of jet streams					
26.	Diameter of steam jets:		in	27.	Design basis for steam in	ijected: B steam/LB hvdrocarbon				
28.	How will steam flow be con	trolled if steam	injection is	suse		B Steam/LB HV0Tocarbon				
_	Cha	aracteristics of	the Wast	te G	as Stream to be Burned					
29.	Name	Quan Grains of H			<b>Quantity</b> (LB/hr, ft³/hr, etc)	Source of Material				
	Tank Vapor	N/A	4		61.23 lb/hr	CTK1-3, PTK1-3				
		-								
30	Estimate total combustible	to flare	61.23 lb	h/hr	l B/hr	or ACF/hr				
00.	(Maximum mass flow rate of		01,2010	0,111	scfm					
31.	Estimated total flow rate to	flare including r	naterials to	o be	burned, carrier gases, au	xiliary fuel, etc.:				
61.23 lb/hr LB/hr or ACF/hr										
32. Give composition of carrier gases:										
	See Promax									
33.	Temperature of emission st	ream:		34.	Identify and describe all a	l auxiliary fuels to be burned.				
		°F				BTU/scf				
	Heating value of emission s 1020	stream: BTU/ft³				BTU/scf				
	Mean molecular weight of e		ı: l			BTU/scf				
	MW = lb/lb-m					BTU/scf				
35.	Temperature of flare gas:	N/A °F		36. Flare gas flow rate: 50 scf/min						
37.	Flare gas heat content: 10	20 BTU/ft³		38.	Flare gas exit velocity:	N/A scf/min				
39.	Maximum rate during emerg	gency for one m	najor piece	of e	equipment or process unit:	N/A scf/min				
	Maximum rate during emerg									
41.	Describe any air pollution reheating, gas humidification $N/A$		nlet and o	outle	t gas conditioning proces	ses (e.g., gas cooling, gas				
12	Describe the collection mat	erial disposal s	vstem.			<u> </u>				
42.	Tanks are routed to comb	, ,	yəl <del>c</del> iii.							
43	Have you included Flare Co	ontrol Device i	n the Emis	ssion	ns Points Data Summary S	sheet? Yes				

Please propose m proposed operating proposed emissions MONITORING:	g parameters. Please propose	and Testing  porting in order to demonstrate compliance with the testing in order to demonstrate compliance with the RECORDKEEPING:  Operator will keep records if combustor is found
•		non-operational.
REPORTING:		TESTING:
Notifications will be	made as required.	Testing will be conducted as required.
MONITORING:		ocess parameters and ranges that are proposed to be trate compliance with the operation of this process
RECORDKEEPING: REPORTING:	Please describe the proposed rec	cordkeeping that will accompany the monitoring. emissions testing for this process equipment on air
TESTING:		emissions testing for this process equipment on air
45. Manufacturer's Gua 98% VOC	aranteed Capture Efficiency for eac	ch air pollutant.
46. Manufacturer's Gua 98% VOC	aranteed Control Efficiency for each	h air pollutant.
47. Describe all operati N/A	ng ranges and maintenance proce	dures required by Manufacturer to maintain warranty.



# **QUOTATION**

**CLIENT: American Energy Partners, LP** 

**SUBJECT: Mission Enclosed Vapor Combustor (MEVC200)** 

NOV PROPOSAL: H-14100-14-200 Rev.2

			<u> </u>		
0	5/19/14	TW	RC	PM	Quotation
REV	DATE	BY	CHECKED	APPROVED	COMMENTS

NOV

10011 MEADOWGLEN LANE, 2<sup>ND</sup> FLOOR HOUSTON, TX 77042

TEL: 1-713-395-5000 FAX: 1-713-395-5001



# **CONTENTS**

1	CO	MMERCIAL AND TECHNICAL	. 3
	1.1	Introduction	3
	1.2	Prices	5
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## 1 COMMERCIAL AND TECHNICAL

## 1.1 Introduction

In response to your inquiry, NOV is pleased to offer the following proposal for a NOV Mission Enclosed Vapor Combustor (MEVC). The model MEVC200 is capable of 18.42 MMBTU/HR, Medium Temperature Flares (MTF). NOV Mission offers a full line of reliable enclosed combustors for the ever changing requirements of today's regulation filled oil and gas industry. Mission's MEVC design incorporates years of experience with tank vapors with a combustor design which is highly effective, tested and certified "99%" for destruction of vent emissions from oil and condensate tank batteries, loading operations and storage facilities. NOV's stainless steel enclosed flare design is capable of meeting industry regulations while offering significant cost savings. Scalable to customer application, this flare is proven throughout the world. The following items will show the advantages and benefits to incorporating this equipment into the Storage Tank facility:

## **APPLICATIONS**

- Associated gas
- Dehydrators
- Pipeline blow down
- Oil and condensate loading facilities
- Equipment maintenance
- Oil and condensate storage tanks

## **FEATURES AND BENEFITS:**

- Meets EPA 40 CFR 60.00 regulations
- Remote location solar panel option available
- 98%+ destruction efficiency (independent 3rd party tested)
- Flexible & fully automated and programmable system (additional parameters optional)
- Quad O compliant ready
- Special custom application larger units available
- Low capital and operating costs
- Very high turndown ratio
- Scalable flow rates
- Field proven design
- Only requires 300 btu/ft3 gas to maintain combustion
- High Temperature Flares (HTF) with 99.99% DRE are also available



Thank you for this opportunity to quote on your combustor needs. Should you have any questions or concerns regarding the commercial terms, the scope of supply offered, or any technical points which may need clarification, please feel free to contact NOV at:

Contact : Pete Magnani

Email : <u>pete.magnani@nov.com</u>

Telephone : 1-713-395-5000 Fax : 1-713-395-5001

Address : 10011 Meadowglen Lane, 2<sup>nd</sup> Floor

Houston, TX 77042

USA



## Flare Gas Stream: 5.4 MW MTF:

- o Type: Enclosed Tank Battery Flare
- o Composition: 2200 btu/ft3 gas
- o Temperature: Ambient to 100°F +/- 20 deg°F
- o Flow Rate: up to 200,000 scfd (based on 2200 BTU /ft3 gas) or 139.6 scfm
- o Auxiliary Fuel Requirements N/A
- o Burner Size 18.42 million BTU/hr (5.4 MW)
- o Inlet Pressure Requirements 2-4 oz/in2 (3.5-7.0 "w.c.)
- o Turndown Ratio 5:1
- Data points recorded include combustion temperature, operation pressure, and run time

## • Mechanical:

- o Design Wind Speed 100 mph
- o Ambient Temperature -20 deg F up to 110 deg F
- o Electrical Area Classification General Area Classification (non-hazardous)
- o Elevation Up to 3,000 ft ASL please advise if higher elevation

# Process:

- o Smokeless Capacity 100% Sdf
- o Operating Temperature 1400 deg F to 2100 deg F (1500 deg F Nominal); Retention Time 0.3 sec.
- o Flare Inlet Pressure 2-4 oz/in2 (3.5-7.0 "w.c.)

## Utilities:

- o Pilot Gas Process Gas
- o Electricity 24VDC Panel/ 10A (Solar Option) Auxiliary Fuel N/A
- o Instrument air/gas 80 psig for valve actuation.

# • Emissions:

o Destruction Efficiency: 98% DRE

## 1.4 Delivery

The delivery for the Equipment listed in NOV Scope of Supply is as follows:

- Delivery:
  - o 2-3 weeks ARO, Ex-Works Chattanooga, TN

# 1.5 Commercial Clarifications/Exceptions

- 1.5.1 Terms are net 30 days:
  - 100% Upon notice of readiness to ship.
- 1.5.2 Quoted prices exclude all taxes, import duties, freight and/or insurance charges.
- 1.5.3 Delivery to be confirmed upon acceptance of purchase order.
- 1.5.4 NOV Worldwide Terms and Conditions shall apply.



1.5.7 NOV standard documentation will apply.

# 1.6 Quotation Validity

Validity is 30 days from the date of this proposal.

# 1.7 Service

Available upon request.

# 2 ATTACHMENTS

# 2.1 NOV Documents

NOV Terms and Conditions

# **Attachment N: Supporting Emissions Calculations**

TABLE 1

# FACILITY-WIDE POTENTIAL CRITERIA POLLUTANT EMISSIONS SUMMARY WJ CRISWELL 405 FACILITY ASCENT RESOURCES - MARCELLUS, LLC

	Emission				Criteria Po	Criteria Pollutants 1					
	Point	N	NOx	NOC	2	Ö	8	PM	5	Total	Total HAPS
Emissions Source	Identification	(lb/hr)	(T/yr)	(lb/hr)	(T/yr)	(lb/hr)	(T/yr)	(lb/hr)	(T/yr)	(ib/hr)	(T/vr)
HiPower PSI/GM 3.0L Generator (47 Hp)	9E <sup>(2)</sup>	0.29	1.27	0.01	0.05	0.50	2.18	0.01	0.03	0.02	0.07
Gas Production Unit (1.50 MMBtu/hr)	1E (3)	0.15	0.64	0.01	0.04	0.12	0.54	0.01	0.05	0.003	0.01
Gas Production Unit (1.50 MMBtu/hr)	2E (3)	0.15	0.64	0.01	0.04	0.12	0.54	0.01	0.05	0.003	0.01
Gas Production Unit (1.50 MMBtu/hr)	3E (3)	0.15	0.64	0.01	0.04	0.12	0.54	0.01	0.05	0.003	0.01
Line Heater (1.50 MMBtu/hr)	4E (3)	0.15	0.64	0.01	0.04	0.12	0.54	0.01	0.05	0.003	0.01
Flash Separator Heater (1.00 MIMBtu/hr)	7E (3)	0.10	0.43	0.01	0.02	0.08	0.36	0.01	0.03	0.002	0.01
Condensate Stabilizer Heater (0.75 MMBtu/hr)	11E (3)	0.07	0.32	0.01	0.02	90:0	0.27	0.01	0.02	0.002	0.01
Condensate Storage Tank (400-bbl)	15E (4)	I	-		1.82	I	I	1	i	-	0.001
Condensate Storage Tank (400-bbl)	16E (4)	1	1	ı	1.82	I	i	l	l	1	0.001
Condensate Storage Tank (400-bbl)	17E (4)	1	1	ı	1.82	I	1	ı	-	-	0.001
Produced Water Storage Tank (400-bbl)		I	1	ı	0.01	I	ı	i	****	1	0.001
Produced Water Storage Tank (400-bbl)		1	1	1	0.01	ı	ı	ł	1	I	0.001
Produced Water Storage Tank (400-bbt)	20E (4)		1	į	0.01	ı		ŀ	1	I	0.001
Enclosed Combustor (18.42 MMBtu/hr)		1.25	5.49	1.22	5.36	6.82	29.82	i	ı	I	1
Condensate Truck Loading			!	58.95	2.82	ı	ı	ı	1	0.02	0.001
Produced Water Truck Loading		1	ı	0.59	0.14	ı	ı	ŀ	I	0.001	0.001
Fugitive VOC Emissions	14E (8)	1	!	2.13	9.27	-	1	1	!	0.01	0.03
Total Facility Emissions		2.31	10.07	62.96	23.33	7.94	34.82	0.07	0.28	90.0	0.17

- 1. Emissions of SO2 are assumed to be negligible since pipeline-quality natural gas is used as fuel. Refer to Table 2 for HAP emissions, Table 3 for road emissions, and Table 4 for GHG emissions.
  - 2 . Refer to Table 5 for engine(s) potential emissions calculations.
- 3 . Refer to Tables 6-11 for heater(s) potential emissions calculations.
- 4 . Refer to Tables 12-14 for storage tank(s) potential emissions calculations.
  - 5. Refer to Table 15 for combustor(s) potential emissions calculations.
- 6 . Refer to Table 16 for condensate truck loading potential emissions calculations.
- 7 . Refer to Table 17 for produced water truck loading potential emissions calculations.
- 8 Refer to Tables 18-19 for process piping fugitives potential emissions calculations.

# FACILITY-WIDE POTENTIAL HAP EMISSIONS SUMMARY WJ CRISWELL 405 FACILITY ASCENT RESOURCES - MARCELLUS, LLC

	Emission									Hazaı	Hazardous Air Pollutants	Pollutants									Г
	Point	Formaldehyde	lehyde	Acetaldehyde	ehyde	Acrolein	nie	Methanol	lou	n-Hexane	ıne	Benzene	ne ne	Toluene	] a	Ethyl-Benzene	zene	Xylene		Total HAPS	PS
Emissions Source	Identification	(Ib/hr)	(T/yr)	(lb/hr)	(T/yr)	(Ib/hr)	(T/yr)	(lb/hr)	(T/yr)	(lb/hr)	(T/yr)	(lb/hr)	(T/yr)	(lb/hr)	(T/yr) Hi	Hide this Hide this	ide this	(lb/hr)	(T/vr)	(lb/hr)	(T/vr)
HiPower PSI/GM 3.0L Generator (47 Hp)	9E (2)	0.01	0.04	0.003	0.01	0.002	0.01	0.001	0.005	0.001	0.002	0.0002	0.001	0.0002		0.0001		+	-	0.02	0.07
Gas Production Unit (1.50 MMBtu/hr)	1E (3)	0.0001	0.001	i	!	ı	i	1	!	0.003	0.01	0.0001	0.0001	0.0001	0.0001	_		-	_	0.003	0.01
Gas Production Unit (1.50 MMBtu/hr)	2E (3)	0.0001	0.001	ı	1	ı	i	!	!	0.003	0.01	0.0001	0.0001	0.0001	0.0001	-	1		!	0.003	0.01
Gas Production Unit (1.50 MMBtu/hr)	3E	0.0001	0.001	i	ļ	ı	i	1	1	0.003	0.01	0.0001	0.0001	0.0001	0.0001	1	-	ı	ı	0.003	0.01
Line Heater (1.50 MMBtu/hr)	4E (3)	0.0001	0.001	i		1	ı	!	!	0.003	0.01	0.0001	0.0001	0.0001	0.0001	!	1	1	1	0.003	0.01
Flash Separator Heater (1.00 MMBtu/hr)	7E (5)	0.0001	0.0003	i	ı	ı	ì	1	!	0.002	0.01	0.0001	0.0001	0.0001	0.0001	!	ļ	i	1	0.002	0.01
Condensate Stabilizer Heater (0.75 MMBtu/hr)	116	0.0001	0.0002	1	i	1	ı	1	į	0.001	0.01	0.0001	0.0001	0.0001	0.0001	1	1	!	1	0.002	0.01
Condensate Storage Tank (400-bbl)	15E (#)	ì		ı	i	i	ŀ	1	1		0.0004	1	0.0001	1	0.0001		0.0001	1	0.0001	i	0.001
Condensate Storage Tank (400-bbl)	16E (#)	i	1	ı	i	i	ļ	1	1		0.0004	1	0.0001	-	0.0001	<u> </u>	0.0001	1	0.0001	i	0.001
Condensate Storage Tank (400-bbl)	17E (*)	í	ł	ı	i	i	ļ	1	1		0.0004	1	0.0001	-	0.0001	<u> </u>	0.0001	1	0.0001	1	0.001
Produced Water Storage Tank (400-bbl)	18E	ı	!	1	i	i	ŧ	!	1		0.0001	1	0.0001		0.0001	1	0.0001	ı	0.0001	-	0.001
Produced Water Storage Tank (400-bbl)	19E	ı	!	1	i	ı	ļ	ı	1	1	0.0001	1	0.0001	1	0.0001	1	0.0001	1	0.0001	i	0.001
Produced Water Storage Tank (400-bbl)	20E (*)	i	l	1	i	ì	ŀ	ı	ı		0.0001	1	0.0001	1	0.0001	1	0.0001	1	0.0001	í	0.001
Enclosed Combustor (18.42 MMBtu/hr)	10E	i	!	ı	i	i	ŧ	ı	ı	!	ı	i	1	!	ı	ı	1	1	1	-	i
Condensate Truck Loading	12E (6)	i	1	ı	í	i	1	ı	ı	0.01	0.001	0.002	0.0001	0.001	0.0001	0.0001	0.0001	0.0001	0.0001	0.02	0.001
Produced Water Truck Loading		i	ı	1	ı	i		i	1	0.0001	0.0001	0.0001	0.000.0	0.0001 0	0.0001	0.0001	0.0001	0.0001	0.0001	0.001	0.001
Fugitive VOC Emissions	14E (6)	i	1	ı	1	i	-	ł	ı	0.003	0.01	0.001	0.003	0.003	0.01	0.0001	0.001	0.001	0.002	0.01	0.03
Total Facility Emissions		0.01	0.04	0.003	0.01	0.002	0.01	0.001	0.005	0.03	0.08	0.003	0.004	0.004	0.01	0.00	0.001	0.001	0.002	90.0	0.17

To be convservative, emissions less than 0.0001 for each HAP were rounded up to 0.0001 lb/hr and 0.0001 TPY.
 Refer to Table 5 for engine(s) potential emissions calculations.
 Refer to Tables 6-13 for heater(s) potential emissions calculations.
 Refer to Tables 14-15 for storage tank(s) potential emissions calculations.

**TABLE 3** 

# FACILITY-WIDE POTENTIAL ROAD EMISSIONS SUMMARY WJ CRISWELL 405 FACILITY ASCENT RESOURCES -- MARCELLUS, LLC

	Emission		Pollutants	tants			
	Point	PN	PM <sub>2.5</sub>	M	PM <sub>10</sub>	PM	PMTOT
Emissions Source	Identification	(lb/hr)	(T/yr)	(lb/hr)	(T/yr)	(lb/hr)	(T/vr)
Unpaved Roads	21E 1	0.02	0.10	0.22	96.0	0.74	3.24
Total Facility Emissions	issions	0.02	0.10	0.22	96.0	0.74	3.24

# Notes:

1. Refer to Table 19 for unpaved road source(s) potential emissions calculations.

# ESTIMATION OF FACILITY-WIDE GHG EMISSIONS WJ CRISWELL 405 FACILITY ASCENT RESOURCES – MARCELLUS, LLC

	Total GHG	Emissions
GHG Emission Source	(m t. CO <sub>2</sub> e)	(tons CO <sub>2</sub> e)
Natural Gas Combustion	3,796	4,184
Tanks	263	290
Fugitives	366	403
Flares	11,725	12,925
Total Estimated Facility Emissions:	16,151	17,803

Conversion	on Factors	Global Warm	ing Potential
1.10231	ton/m.t.	CO2	1
0.001	m.t./kg	CH.	25
8,760	Hrs/yr	N₂O	298

(mol %)	CH <sub>e</sub>	G <sub>2</sub> H <sub>3</sub>	C <sub>2</sub> H <sub>8</sub>	C <sub>a</sub> H <sub>13</sub>	C5+
	(mol %)	(mol %)	(mol %)	(mol %)	(mol %
0.17%	79.70%	13.72%	3.69%	1.44%	0.64%

Note:

Carbon Dioxide Equivalent (CQs) emissions are calculated in the tables below by multiplying emissions by global warming potentials for each polutant.

Emissions estimates converted to short torus in this tables below using convention factor from 40 CFR 96 Subpert A.

Global Warming Potentials obtained from 40 CFR 98 Subpert A, Table A-1,

Mol % values obtained from the gas analysis from a representative facility.

	Emission					En	nissions Factor	1		Emissions			Emissions		Total Emis	ssione
Emissions Source	Point Identification	Rated	(MMBtu/hr)	(Btu/hp-hr)	Operation (hrlyr)	(kg/MMBtu)	CH <sub>4</sub> (kg/MMBtu)	N <sub>2</sub> O (kg/MMBtu)	co,	(m.t.) CH <sub>4</sub>	N <sub>2</sub> O	co.	(m.t. CO <sub>2</sub> e) CH <sub>4</sub>	N,O	(m.t. CO <sub>z</sub> e)	CO,e
HiPower PSI/GM 3.0L Generator (47 Hp)	9E	47	0.41	8,681	8,760	53.06	0.001	0.0001	189.64	0.004	0.0004	189.64				
Gas Production Unit (1.50 MMBtu/hr)	1E	"	1,50	0,001	8,760	53.06	0.001	0.0001	697.21	0.004	0.0004	189.64 697.21	0.09	0.107	190 698	209 789
Gas Production Unit (1.50 MMBtu/hr)	2E	_	1.50	_	8,760	53.06	0.001	0.0001	697.21	0.013	0.0013	697.21	0.33	0.392	698	769
Gas Production Unit (1.50 MMBtu/hr)	3E	_	1.50		8,760	53.06	0.001	0.0001	697.21	0.013	0.0013	697.21	0.329	0,3916	698	769
Line Heater (1.50 MMBtu/hr)	4E		1.50	_	6,760	53.06	0,001	0.0001	697.21	0.013	0.0013	697.21	0.33	0.39	698	769
Flash Separator Heater (1.00 MMBtwhr)	7E	-	1.00	_	8,760	53.06	0.001	0.0001	464.81	0.000	0.0009	464.81	0.22	0.26	465	513
Condensate Stabilizer Heater (0.75 MMBtu/hr)	11E	-	0.75		8,760	63.06	0.001	0.0001	348.60	0.007	0.0007	348.60	0.16	0.196	349	385

Notes:
1. Emission factors for GHG obtained from 40 CFR 98 Subpart C, Tables C-1 and C-2.

## Tenk Sources

Emissions Source	Emission Point Identification	Annual Condensate Production	Annual Condensate Production	Default Liquid CH <sub>4</sub> Content <sup>5</sup>	Average API Gravity	Average Separator Pressure	Separator Temperature	Dissolved Gas Grevity	Actual VOC Gas/Oil Ratio	Emissions <sup>2</sup>	Total E	missions	Control Efficiency		ontrolled selons
		(bbl/yr)	(1,000 gallyr)	(mol %)		(pelg)	(°F)	(8G <sub>x</sub> )	(sct/bbl oil)	(m.t.)	(m.t. CO <sub>2</sub> e)	(tons COze)	(%)	(m.t. CO <sub>z</sub> e)	(tons CO <sub>2</sub> s)
Condensate Storage Tank (400-bbl)	CTK-1	6,083	256	27.4	63	100	80	0.90	00.688	28.32	708.02	780.46	98%	14.16	15.61
Condensate Storage Tank (400-bbl)	CTK-2	6,083	256	27.4	63	100	80	0.90	888.00	28.32	708.02	780,46	98%	14.16	15.61
Condensate Storage Trank (400-bbl)	СТК-З	6,083	256	27.4	63	100	80	0.90	888.00	28.32	708.02	780,46	96%	14.16	15.61
Produced Water Storage Tunk (400-bbl)	PTK-1	30,417	1,278	27.4	63	100	80	0.90	888.00	1.42	35,40	39.02	98%	0.71	0.78
Produced Water Storage Tank (400-bbl)	PTK-2	30,417	1.278	27.4	63	100	80	0.90	00.888	1.42	35.40	39.02	98%	0.71	0.78
Produced Water Storage Tank (400-bbl)	PTK-3	30,417	1,278	27.4	63	100	80	0.90	888.00	1.42	35.40	39.02	98%	0.71	0.78
													Total Tanks	45	40

- Notes:

  1. Default CH4 content for crude oil per API compandium Section 5.4 and Appendix B.

  2. Emissions estimated using API Compandium, Section 5.4.

## Truck Loading

	Emission	Annual Condensate	Annuel Condensate	Default Liquid CH <sub>4</sub>	Emission Factor	Emis	elons	Emissions 2	Total Er	ntealons
Emissions Source	Point Identification	Production (bbl/yr)	Production (1,000 gal/yr)	Content 1 (mol %)	VOC (lb/1,000 gal)	VOC (tons)	VOC (m.t.)	CH <sub>4</sub> (m.t.)	(m.t CO <sub>2</sub> e)	(tons CO <sub>2</sub> e)
Condensate Truck Loading	12E	18,250	767	27.4	65.00	21.08	19.12	5.24	131	144
Produced Water Truck Loading	13E	91,250	3,633	27.4	7.37	14.12	12.81	3.51	88	97
								Total Loading:	219	241

- Notes:

  1. Default CH4 content for cnude oil per API compendium Section 5.4 and Appendix B.

  2. Emissions estimated using API Compendium, Section 5.5.

		Maximum			Emlesion Factor CH,	Emiss	one 2	Emia	alons	Total Er	missions
Source Type/Service 1	Number of Sources	Hours of Operation	CO <sub>2</sub> (mol %)	CH, (mol %)	(m.t./hr/ component)	CO <sub>2</sub> (m·t.)	CH <sub>4</sub> (m.t.)	CO <sub>2</sub> (m t CO <sub>2</sub> e)	CH <sub>4</sub> (m t CO <sub>2</sub> e)	(m.t. CO <sub>2</sub> e)	(tons CO <sub>2</sub> e)
Valves - Gas/Vapor	200	8,760	0.0017	0.7970	0.0000045	0.0358	6.28	0.0358	157.09	167,13	173.20
Flanges - Gas/Vapor	700	8,760	0.0017	0.7970	0.00000039	0.0109	1.91	0.0109	47.65	47.66	52.54
Compressor Seals - Gas/Vapor	0	8,760	0.0017	0.7970	0.0000024	0.0000	0.00	0.0000	0.00	0.00	0.00
Relief Valves - Gas/Vapor	20	8,760	0.0017	0.7970	0.000017	0.0135	2.37	0.0135	59.35	59,36	65.43
Valves - Light Liquid	200	8,760	0.0017	0.7970	0.0000025	0.0199	3.49	0.0199	87.27	87.29	96.22
Flanges - Light Liquid	25	8,760	0.0017	0.7970	0.00000011	0.00011	0.02	0.00011	0.48	0.48	0.53
Pump Seels - Light Liquid	0	6,760	0.0017	0.7970	0.000013	0.0000	0.00	0.0000	0.00	0.00	0.00
Relief Valves - Light Liquid	15	8,760	0.0017	0.7970	0.00000539	0.0032	0.68	0.0032	14.11	14.12	15.56
								7.	otal Fugitives:	386	403

- Number of each component and type of service estimated based on a similar station
   Emission estimated using API Compendium, Section 6.0, Tables 6-12 and 6-21.

Emissions Source	Emiesion Point Identification	Burner Rating (MREsturn)	Annual Gas Usage 1 (schyr)	CO <sub>2</sub> (mol %)	CH <sub>4</sub> (mol %)	Emission Feator N <sub>2</sub> O (m.t./MMsct)	CO <sub>2</sub> (m.t.)	Emissions <sup>2</sup> CH <sub>4</sub> (m-t.)	N <sub>2</sub> O (m.t.)	CO <sub>2</sub> (m.t CO <sub>2</sub> e)	Emissions CH <sub>4</sub> (m.t. CO <sub>2</sub> e)	N <sub>z</sub> O (m.t CO <sub>z</sub> e)	Total E	missions (tons CO <sub>2</sub> s)
Enclosed Combustor (18.42 MMBtu/hr)	10E	18,4	158,195,294	0.0017	0.7970	5.90E-07	10,519	48	0.00009	10,519	1,206	0.026	11,725	12,925
											Total Fla	re Emissions:	11,725	12,925

- 1. Annual gas usage calculated using the gas heating visue of 1,020 Btu/scf.
  2. Emissions estimated using API Compendium, Section 4.6 for Flare Emissions.

# POTENTIAL EMISSIONS SUMMARY HIPOWER PSI/GM 3.0L GENERATOR (ENG2) WJ CRISWELL 405 FACILITY ASCENT RESOURCES – MARCELLUS, LLC

			Potential En	nission Rate <sup>3</sup>
Pollutant <sup>1</sup>	Horsepower	Emission Factors <sup>2</sup>	(lb/hr)	(T/yr)
NO <sub>X</sub>	47	2.80	0.29	1.27
voc	47	0.0296	0.01	0.05
co	47	4.80	0.50	2.18
PM	47	0.01941	0.01	0.03
FORMALDEHYDE	47	0.0205	0.01	0.04
ACETALDEHYDE	47	0.00836	0.003	0.01
ACROLEIN	47	0.00514	0.002	0.01
METHANOL	47	0.0025	0.001	0.004
n-HEXANE	47	0.00111	0.0005	0.002
BENZENE	47	0.00044	0.0002	0.001
TOLUENE	47	0.000408	0.0002	0.001
ETHYL-BENZENE	47	0.0000397	<0.0001	0.0001
XYLENES	47	0.000184	0.0001	0.0003

## Notes:

- 1. Emissions of SO2 are assumed to be negligible and not reportable.
- 2. Emission Factors obtained from NSPS Subpart JJJJ and AP-42.

NO <sub>X</sub> =	2.80	g/hp-hr NSPS Subpart JJJJ preamble Table 3, January 18, 2008.
VOC =	0.0296	lb/MMBtu AP-42 Table 3.2-2.
CO =	4.80	g/hp-hr NSPS Subpart JJJJ preamble Table 3, January 18, 2008.
PM =	0.01941	lb/MMBtu AP-42 Table 3.2-2.
formaldehyde =	0.0205	ib/MMBtu AP-42 Table 3.2-2.
Acetaldehyde =	0.00836	lb/MMBtu AP-42 Table 3.2-2
Acrolein =	0.00514	lb/MMBtu AP-42 Table 3.2-2
Methanol =	0.0025	Ib/MMBtu AP-42 Table 3.2-2
N-Hexane =	0.00111	lb/MMBtu AP-42 Table 3.2-2
Benzene =	0.00044	lb/MMBtu AP-42 Table 3.2-2
Toluene =	0.000408	lb/MMBtu AP-42 Table 3.2-2
Ethyl-Benzene =	0.0000397	lb/MMBtu AP-42 Table 3.2-2
Xylenes =	0.000184	lb/MMBtu AP-42 Table 3.2-2

3. Potential emissions based on emission factors, maximum horsepower, a brake specific fuel consumption of 8,681 btu/hp-hr, and 8,760 hours of operation per year.

# ASCENT RESOURCES - MARCELLUS, LLC POTENTIAL EMISSIONS SUMMARY GAS PRODUCTION UNIT (GPU-1) **WJ CRISWELL 405 FACILITY**

Pollutant 1	Emission Factors <sup>2</sup>	Potential Em	Potential Emission Rates <sup>3</sup>
	(Ib/MMSCF)	(lb/hr)	(T/yr)
NOX	100.0	0.15	0.64
VOC	5.5	0.01	0.04
00	84.0	0.12	0.54
PM	7.6	0.01	0.05
Benzene	0.0021	<0.0001	<0.0001
Formaldehyde	0.075	<0.0001	0.0005
n-Hexane	1.8	0.003	0.01
Toluene	0.0034	<0.0001	<0.0001

# Notes:

- 1. HAP emissions include Benzene, Formaldehyde, n-Hexane, and Toluene.
- 2. Emission factors obtained from AP-42 Section 1.4 (7/98), Table 1.4-1 through 1.4-3 for commercial boilers. 3. Potential emissions based on AP-42 emission factors, maximum firing rate of 1.50 MMBtu/hr,

1,020 Btu/scf fuel heating value, and 8,760 hours of operation per year.

# POTENTIAL EMISSIONS SUMMARY GAS PRODUCTION UNIT (GPU-2) WJ CRISWELL 405 FACILITY ASCENT RESOURCES – MARCELLUS, LLC

Pollutant '	Emission Factors <sup>2</sup>	Potential Em	Potential Emission Rates <sup>3</sup>
	(Ib/MMSCF)	(lb/hr)	(T/yr)
NOX	100.0	0.15	0.64
VOC	5.5	0.01	0.04
8	84.0	0.12	0.54
Md	7.6	0.01	0.05
Benzene	0.0021	<0.0001	<0.0001
Formaldehyde	0.075	<0.0001	0.0005
n-Hexane	1.8	0.003	0.01
Toluene	0.0034	<0.0001	<0.0001

- 1. HAP emissions include Benzene, Formaldehyde, n-Hexane, and Toluene.
- 2. Emission factors obtained from AP-42 Section 1.4 (7/98), Table 1.4-1 through 1.4-3 for commercial boilers.
  - 3. Potential emissions based on AP-42 emission factors, maximum firing rate of 1.50 MMBtu/hr,
    - 1,020 Btu/scf fuel heating value, and 8,760 hours of operation per year.

# POTENTIAL EMISSIONS SUMMARY GAS PRODUCTION UNIT (GPU-3) WJ CRISWELL 405 FACILITY ASCENT RESOURCES – MARCELLUS, LLC

Pollutant 1	Emission Factors <sup>2</sup>	Potential Em	Potential Emission Rates <sup>3</sup>
	(Ib/MMSCF)	(lb/hr)	(T/yr)
NOx	100.0	0.15	0.64
VOC	5.5	0.01	0.04
00	84.0	0.12	0.54
PM	7.6	0.01	0.05
Benzene	0.0021	<0.0001	<0.0001
Formaldehyde	0.075	<0.0001	0.0005
n-Hexane	1.8	0.003	0.01
Toluene	0.0034	<0.0001	<0.0001

- 1. HAP emissions include Benzene, Formaldehyde, n-Hexane, and Toluene.
- 2. Emission factors obtained from AP-42 Section 1.4 (7/98), Table 1.4-1 through 1.4-3 for commercial boilers.
  - 3. Potential emissions based on AP-42 emission factors, maximum firing rate of 1.50 MMBtu/hr,
    - 1,020 Btu/scf fuel heating value, and 8,760 hours of operation per year.

# POTENTIAL EMISSIONS SUMMARY LINE HEATER (HTR-1) WJ CRISWELL 405 FACILITY ASCENT RESOURCES – MARCELLUS, LLC

Dollitent 1	minor in the second of the sec		D 64 cm - 1 cm - 1 cm - 2 cm - 3
	(Ib/MMSCF)	(lb/hr)	(T/vr)
×ON	100.0	0.15	0.64
VOC	5.5	0.01	0.04
00	84.0	0.12	0.54
PM	7.6	0.01	0.05
Benzene	0.0021	<0.0001	<0.0001
Formaldehyde	0.075	<0.0001	0.0005
n-Hexane	1.8	0.003	0.01
Toluene	0.0034	<0.0001	<0.0001

- 1. HAP emissions include Benzene, Formaldehyde, n-Hexane, and Toluene.
- 2. Emission factors obtained from AP-42 Section 1.4 (7/98), Table 1.4-1 through 1.4-3 for commercial boilers.
  - 3. Potential emissions based on AP-42 emission factors, maximum firing rate of 1.50 MMBtu/hr,
    - 1,020 Btu/scf fuel heating value, and 8,760 hours of operation per year.

# POTENTIAL EMISSIONS SUMMARY FLASH SEPARATOR HEATER (SEP-1) WJ CRISWELL 405 FACILITY ASCENT RESOURCES – MARCELLUS, LLC

Pollutant 1	Emission Factors <sup>2</sup>	Potential Emi	Potential Emission Rates <sup>3</sup>
	(lb/MMSCF)	(lb/hr)	(T/yr)
NOX	100.0	0.10	0.43
VOC	5.5	0.01	0.02
8	84.0	0.08	0.36
PM	7.6	0.01	0.03
Benzene	0.0021	<0.0001	<0.0001
Formaldehyde	0.075	<0.0001	0.0003
n-Hexane	1.8	0.002	0.01
Toluene	0.0034	<0.0001	<0.0001

- 1. HAP emissions include Benzene, Formaldehyde, n-Hexane, and Toluene.
- 2. Emission factors obtained from AP-42 Section 1.4 (7/98), Table 1.4-1 through 1.4-3 for commercial boilers.
  - 3. Potential emissions based on AP-42 emission factors, maximum firing rate of 1.00 MMBtu/hr,
    - 1,020 Btu/scf fuel heating value, and 8,760 hours of operation per year.

**TABLE 11** 

# ASCENT RESOURCES - MARCELLUS, LLC **CONDENSATE STABILIZER HEATER (CS-1)** POTENTIAL EMISSIONS SUMMARY **WJ CRISWELL 405 FACILITY**

,			
Pollutant 1	Emission Factors <sup>2</sup>	Potential Emi	Potential Emission Rates <sup>3</sup>
	(Ib/MMSCF)	(lb/hr)	(T/yr)
NOX	100.0	0.07	0.32
NOC	5.5	0.004	0.02
00	84.0	90.0	0.27
PM	7.6	0.01	0.02
Benzene	0.0021	<0.0001	<0.0001
Formaldehyde	0.075	<0.0001	0.0002
n-Hexane	1.8	0.001	0.01
Toluene	0.0034	<0.0001	<0.0001

- 1. HAP emissions include Benzene, Formaldehyde, n-Hexane, and Toluene.
- 2. Emission factors obtained from AP-42 Section 1.4 (7/98), Table 1.4-1 through 1.4-3 for commercial boilers. 3. Potential emissions based on AP-42 emission factors, maximum firing rate of 0.75 MMBtu/hr,
- 1,020 Btu/scf fuel heating value, and 8,760 hours of operation per year.

# POTENTIAL EMISSIONS SUMMARY CONDENSATE AND PRODUCED WATER STORAGE TANKS WJ CRISWELL 405 FACILITY ASCENT RESOURCES – MARCELLUS, LLC

					Poten	Potential VOC Emissions	sions			Pote	Potential HAP Emissions	ons	
				Annual	Annual	Annual							
		Annual	Tank	Breathing	Working	Flash	Flare Capture	Total Annual	Benzene	Toluene	Ethylbenzene	Xylenes	n-Hexane
Source	Source ID	Throughput	Capacity	Losses 2	Losses 2	Losses 3	Efficiency 4	Emissions <sup>5</sup>	Emissions 6	Emissions 6	Emissions 8	Emissions	Emissions <sup>6</sup>
		(gallons/year)	(gallons)	(sql)	(sql)	(T/yr)	(%)	(T/yr)	(T/yr)	(T/yr)	(T/yr)	(T/vr)	(T/vr)
Condensate Storage Tank (400-bbl)	CTK-1	255,500	16,800	1,619.94	2,798.68	88.82	%86	1.82	0.0001	<0.0001	<0.0001	<0.0001	0 0004
Condensate Storage Tank (400-bbl)	CTK-2	255,500	16,800	1,619.94	2,798.68	88.82	%86	1.82	0.0001	<0.0001	<0.0001	<0.0001	0.0004
Condensate Storage Tank (400-bbl)	CTK-3	255,500	16,800	1,619.94	2,798.68	88.82	%86	1.82	0.0001	<0.0001	<0.0001	<0.0001	0,0004
Produced Water Storage Tank (400-bbl)	PTK-1	1,277,500	16,800	1,619.94	7,614.51	0.15	%86	0.004	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001
Produced Water Storage Tank (400-bbl)	PTK-2	1,277,500	16,800	1,619.94	7,614.51	0.15	%86	0.004	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001
Produced Water Storage Tank (400-bbl)	PTK-3	1,277,500	16,800	1,619.94	7,614.51	0.15	%86	0.004	<0.0001	<0.0001	<0.0001	<0.0001	<0.0001

John.

1. Based on the following maximum annual throughput values:

Condensate = 18,250-bbls/yr Produced Water = 91,250-bbls/yr 2. Annual breathing and working losses were determined using AP-42 Section 7 (11/06).

3. Annual flash losses were based on Promax simulation method. A copy of the Promax output has been provided.

4. Breathing, working and flash emissions from the storage tank(s) are routed to an enclosed combustor, which has a capture efficiency of 98%. Refer to Table 14 for flare(s) emissions calculations. 5. To be conservative, breathing and working losses for produced water were calculated using condensate, assuming 1% is emitted. Flash losses for produced water were calculated using ProMax.

Total Annual Emissions (T/yr) = [((Breathing Losses (lbs) + Working Losses (lbs)) / 2000) + Flash Losses (T/yr)] x [1 - Enclosed Combustor Capture Efficiency (%)]
Total Annual Emissions (T/yr) = [((Breathing Losses (lbs) + Working Losses (lbs)) / 2000) x 1%) + Flash Losses (T/yr)] x [1 - Enclosed Combustor Capture Efficiency (%)]

6. Estimated HAP Composition (% by Weight), Promax output reports of a site specific sample.

Benzene = 0.004%
Toluene = 0.001%
Ethylbenzene = 0.000038%
Xylenes = 0.00095%
n-Hexane = 0.021%

# POTENTIAL EMISSIONS SUMMARY AP-42 SECTION 7 (EPA TANKS 4.0.9d) FIXED-ROOF TANK EMISSIONS WJ CRISWELL 405 FACILITY ASCENT RESOURCES – MARCELLUS, LLC

Tank Identification	WJ Criswell 405, CTK-1-3	WJ Criswell 405, PTK-1-6
Location for Calculation Purposes	Charleston, West Virginia	Charleston, West Virginia
Contents of Tank	Gasoline (RVP 15.0)	Gasoline (RVP 15.0)
Tank/Roof Type	Dome	Dome
Underground?	Aboveground	Aboveground
Diameter, ft	12.0	12.0
Shell Height or Length, ft	20.0	20.0
Nominal Capacity, gal	16,800	16,800
Throughput, gallons/yr	255,500	1,277,500
Tank Paint Color	White	White
Tank Paint Condition	Good	Good
Effective Diameter, ft	12.0	12.0
Geometric Capacity, gal	16,074	16,074
Maximum Liquid Height, ft	19.0	19.0
Average Liquid Height, ft	14	19.0
Cone Tank Roof Slope, ft/ft	0.0625	
Dome Tank Roof Radius, ft	12.00	0.0625
Dome Tank Roof Height, ft	1.608	12.00
Roof Outage, ft	0.823	1.608
Vapor Space Outage, ft	6.57	0.823
Vapor Space Volume, ft^3	743	6.57
Average Daily Minimum Ambient Temperature, F	44.22	743
Average Daily Maximum Ambient Temperature, F	65.75	44.22
Daily Total Solar Insolation Factor, Btu/ft^2/day	1251	65.75
Daily Average Ambient Temperature, F		1251
Tank Paint Solar Absorbance, dimensionless	55.0 0.170	55.0
Daily Vapor Temperature Range, R		0.170
Daily Average Liquid Surf. Temperature, F	21.5	21.5
Daily Minimum Liquid Surf. Temperature, F	56.7	56.7
Daily Maximum Liquid Surf. Temperature, F	51.3	51.3
Liquid Bulk Temperature	62.0	62.0
Vapor Molecular Weight, Ib/Ibmol	55.00 60.0	55.00
Antoine's Coefficient A	N/A	60.0
Antoine's Coefficient B	N/A N/A	N/A
Antoine's Coefficient C	N/A N/A	N/A
Type of Substance (for use in calculations)	Gas	N/A
Vapor Pressure at Daily Av. Liquid Surf. Temp., psia		Gas
Vapor Pressure at Daily Min. Liquid Surf. Temp., psia	7.668	7.668
Vapor Pressure at Daily Max. Liquid Surf. Temp., psia	6.935 8.460	6.935
vapor r ressure at Bally Max. Elquid Suri. Temp., psia		8.460
Vapor Pressure Calculation Method	AP-42 Figure 7.1-14b: RVP=15 ASTM Slope=3	AP-42 Figure 7.1-14b: RVP=15
Vapor Density, lb/ft^3		ASTM Slope=3
Daily Vapor Pressure range, psi	0.083030 1.525	0.083030
Breather Vent Pressure Setting, psig	0.0300	1.525
Breather Vent Vacuum Setting, psig		0.0300
Breather Vent Pressure Setting Range, psi	-0.0300	-0.0300
Ambient Pressure, psia	0.0600	0.0600
Vapor Space Expansion Factor	14.3	14.3
Vented Vapor Saturation Factor	0.2640	0.2640
Annual Turnovers	0.272	0.272
Turnover Factor	15.89	79.47
Working Loss Product Factor	1.00	0.54
Standing Storage Loss, Ib/yr	1.00	1.00
	1,619.94	1,619.94
Working Loss, Ib/yr	2,798.68	7,614.51
Total Losses, lb/yr	4,418.62	9,234.44
Standing Storage Loss, TPY	0.81	0.81
Working Loss, TPY	1.40	3.81
Total Losses, TPY	2.21	4.62

Based on AP-42, February 1996, Section 7.1.3.1.

**TABLE 14** 

# ASCENT RESOURCES - MARCELLUS, LLC POTENTIAL EMISSIONS SUMMARY ENCLOSED COMBUSTOR (CTRL-1) WJ CRISWELL 405 FACILITY

		Potential Tank	Tank	Flare Doctricotion		
	Emission Factors 1	Losses 2	2	Efficiency	Total Potential Emission Rates	Emission Rates 3
Pollutant	(ib/MMBtu)	(lb/hr)	(Ther)	(30)		
			(1,6,1)	(%)	(lb/hr)	(T/vr)
ò	9900					
× - :	200.0	1	1	-	10.1	1
S	0.370				67:1	5.49
	25:0	i	1	!	6 82	1000
200	!	61.73	00 000		20:0	29.62
		67:10	768.20	86	1.22	5.26
						20:0

# Notes:

1. Emission factors for NOx and CO obtained from AP-42 Table 13.5-1 (9/91) for industrial flares.

2. Potential tank emissions are estimated based on the breathing, working, and flash losses from the storage tank(s) and a 98% capture efficiency at the combustor (refer to Table 12).

3. Potential emissions for NOx and CO are based on AP-42 emission factors, an estimated heat value of 18.42 MMBtu/hr, and 8,760 hours of operation per year.
Potential emissions for VOC are based on a 98% capture efficiency from the storage tank(s), a 98% destruction efficiency from the enclosed combustor, and 8,760 hours of operation per year.

# ASCENT RESOURCES - MARCELLUS, LLC CONDENSATE TRUCK LOADING (TRL-1) POTENTIAL EMISSIONS SUMMARY WJ CRISWELL 405 FACILITY

Jncontrolled VOC Emissions	Annual Emissions <sup>5</sup> (T/yr)	2.82
Uncontroll	Hourly Emissions <sup>4</sup> (lb/hr)	58.95
	Annual Throughput <sup>3</sup> (gals)	766,500
	Maximum Hourly Throughput <sup>2</sup> (gals)	8,000
	Emission Factor <sup>1</sup> (Ib VOC/10 <sup>3</sup> gal)	7.369
	Temp of Loaded Liquid (°F)	55
	MW of Vapors (M) (Ib/Ib-mole)	09
	True Vapor Pressure (P)	8.46
	Saturation Factor <sup>1</sup> (S)	9.0
	Constituent	Noc
	Material Name	Condensate

1. Per AP-42, 5th Edition (6/08), Section 5.2, Equation 1

Emission Factor 
$$\left(\frac{lb\ VOC}{10^3gal}\right) = \left(\frac{S \times P \times M}{^{\circ}F + 460}\right) \times 12.46$$

- 2. Maximum hourly throughput is the amount of condensate loaded out from the storage tank(s).
  - 3. Annual Throughput is the amount of condensate loaded out from the storage tank(s).
- 4. Uncontrolled Hourly Emissions = Hourly Throughput / 1000 x Emission Factor 5. Uncontrolled Annual Emissions = Annual Throughput / 1000 x Emission Factor / 2000 lb/T

# Estimated HAP Composition (% by Weight)\*\*

		Uncontrolle	Uncontrolled Emissions
Pollutant	Wt%	(lb/hr)	(tpv)
Benzene	0.004%	0.002	0.0001
Toluene	0.001%	0.001	0.00003
Ethylbenzene	0.00004%	0.00002	0.000001
Xylenes	0.0001%	0.00006	0.000003
n-Hexane	0.02%	0.01	0.001
Fotal HAPs	0.03%	0.02	0.001
A 11 17 1 10 10 10 10 10 10 10 10 10 10 10 10 1	0.00.0	70.0	_

Estimated HAP Composition (% by Weight), Promax output reports of a site specific sample.

# POTENTIAL EMISSIONS SUMMARY PRODUCED WATER TRUCK LOADING (TRL-2) WJ CRISWELL 405 FACILITY ASCENT RESOURCES – MARCELLUS, LLC

controlled VOC Emissions	Annual Emissions <sup>5</sup> (T/yr)	0.14
Uncontrolled	Hourly Emissions <sup>4</sup> (lb/hr)	0.59
	Annual Throughput <sup>3</sup> (gals)	3,832,500
	Maximum Hourly Throughput <sup>2</sup> (gals)	8,000
	Emission Factor <sup>1</sup> (Ib VOC/10³ gal)	7.369
	Temp of Loaded Liquid (°F)	55
	MW of Vapors (M) (lb/lb-mole)	09
	True Vapor Pressure (P)	8.46
	Saturation Factor <sup>1</sup> (S)	9.0
	Constituent	voc
	Material Name	Condensate <sup>6</sup>

Notes:

1. Per AP-42, 5th Edition (6/08), Section 5.2, Equation 1

Emission Factor 
$$\left(\frac{lb\ VOC}{10^3 gal}\right) = \left(\frac{S \times P \times M}{^{\circ}F + 460}\right) \times 12.46$$

2. Maximum hourly throughput is the amount of produced water loaded out from the storage tank(s).

3. Annual Throughput is the amount of produced water loaded out from the storage tank(s).

4. Uncontrolled Hourly Emissions = Hourly Throughput / 1000 x Emission Factor

5. Uncontrolled Annual Emissions = Annual Throughput / 1000  $\times$  Emission Factor / 2000 lb/T

6. Loading emissions for produced water were calculated using condensate, assuming 1% is emitted.

# Estimated HAP Composition (% by Weight)\*\*

		Uncontrolle	Uncontrolled Emissions
Pollutant	Wt%	(lb/hr)	(tpy)
Benzene	0.003%	0.00001	0.000004
Toluene	0.001%	0.000005	0.000001
Ethylbenzene	0.00003%	0.0000002	0.00000004
Xylenes	0.0001%	0.0000004	0.0000001
n-Hexane	0.002%	0.00001	0.000003
Total HAPs	0.01%	0.00003	0.00001
0 100000			

Estimated HAP Composition (% by Weight), Promax output reports of a site specific sample.

# ASCENT RESOURCES - MARCELLUS, LLC PROCESS PIPING FUGITIVES (FUG-1) POTENTIAL EMISSIONS SUMMARY **WJ CRISWELL 405 FACILITY**

	Type of	Number of	Emission Factors		Potential VOC Emission Rates	mission Rates 4
Component Type	Service 1	Components 1	(lb/hr-component) 2	Percent VOC 3	(Ib/hr)	(T/yr)
Valves	Gas/Vapor	200	0.00992	16.02%	0.32	1.39
Flanges	Gas/Vapor	200	0.00086	16.02%	0.10	0.42
Relief Valves	Gas/Vapor	20	0.0194	16.02%	90:0	0.27
Connectors	Gas/Vapor	800	0.00044	16.02%	90.0	0.25
Valves	Light Liquid	200	0.0055	100.00%	1.10	4.82
Flanges	Light Liquid	25	0.000243	100.00%	0.01	0.03
Relief Valves	Light Liquid	15	0.0165	100.00%	0.25	1.08
Connectors	Light Liquid	200	0.000463	100.00%	0.23	1.01
Totals:		2,460		1	2.13	9.27

# Notes:

- 1. Number of each component and type of service estimated based on a similar station.
- 2. Emission factors based on EPA's natural gas processing factors for process piping fugitive emissions.
- 3. Percent VOC for Gas/Vapor service based on a gas analysis from the Facility (refer to Attachment 18).
  - 4. Emission rates based on 8,760 hours of operation per year.

Estimated the composition ( /a by resignity	II ( /u m) morganic)		
		Total Fug	Total Fugitive HAP
		Uncontrolle	Uncontrolled Emissions
Pollutant	Wt% <sup>1</sup>	(lb/hr)	(T/yr)
Benzene	0.028%	0.001	0.003
Toluene	0.118%	0:003	0.01
Ethylbenzene	0.0049%	0.0001	0.0005
Xylenes	0.025%	0.001	0.002
n-Hexane	0.136%	0.003	0.01
Total HAPs	0.312%	0.01	0.03
Total VOCs	16.021%	2.13	9.27

Based on Gas Analyses. An extended analysis was unavailable, therefore, GRI GlyCalc factors for production were used to estimate C6+ breakout

# GAS ANALYSIS WJ CRISWELL 405 FACILITY ASCENT RESOURCES – MARCELLUS, LLC

Component <sup>1</sup>	Molecular Weight	Mol % <sup>2</sup>	Molar Weight <sup>3</sup>	Average Mass % <sup>4</sup>
Carbon Monoxide	28.01	0.000%	0.000	0.000%
Hydrogen Sulfide	34.08	0.000%	0.000	0.000%
Oxygen	16.04	0.000%	0.000	0.000%
Helium	4	0.000%	0.000	0.000%
Nitrogen	28.02	0.000%	0.068	0.333%
Carbon Dioxide	44.01	0.241%	0.000	0.358%
Methane	16.04	79.701%	12.784	62.970%
Ethane	30.07	13.718%	4.125	20.319%
Propane	44.09	3.893%	1.716	8.455%
i-Butane	58.12	0.561%	0.326	1.606%
n-Butane	58.12	0.882%	0.513	2.525%
i-Pentane	72.15	0.002 %	0.196	0.963%
n-Pentane	72.15	0.271%	0.140	0.689%
Other Hexanes	86.17	0.134%	0.119	0.585%
n-Hexane	86.17	0.136%	0.028	0.365%
Heptanes	100.2	0.032%	0.063	0.130%
2,2,4-Trimethylpentane	114.23	0.003%	0.003	0.310%
Benzene	78.11	0.018%	0.006	0.101%
Toluene	92.14	0.007 %	0.024	0.028%
Octanes+	114.23	0.020%	0.096	0.474%
e-Benzene	106.17	0.004%	0.001	0.005%
Xvienes	106.17	0.001%	0.005	0.005%
7,101100	Totals:	100.00%	20.30	100.00%
	<sup>5</sup> VOC Totals:	6.18%	3.25	16.02%

# Notes:

- 1. Typical components listed in gas analysis for field gas.
- 2. Mol % values obtained from the gas analysis from the Facility.
- 3. Molar weight = Molecular weight x Mol % /100.
- 4. Average mass % = Molar weight / Total molar weight.
- 5. VOC Totals include the following components (C3+):

Propane n-Hexane
i-Butane Heptanes
n-Butane Benzene
i-Pentane Toluene
n-Pentane Octanes
Hexanes e-Benzene
Xylenes

TABLE 19

# POTENTIAL EMISSIONS SUMMARY UNPAVED ROADS (ROADS) WJ CRISWELL 405 FACILITY ASCENT RESOURCES – MARCELLUS, LLC

			ā	Emission Factor	2				PM Emissions <sup>4</sup>	ssions <sup>4</sup>		
Name	Vehicle Mile	Vehicle Miles Traveled 1	PM <sub>2.5</sub>	PM <sub>10</sub>	PM <sub>TOT</sub>	Control Efficiency <sup>3</sup>	PM <sub>2.5</sub>	2.5	PM <sub>10</sub>	10	PM <sub>Tor</sub>	5
	(VMT/hr)	(VMT/yr)	(Ib/VMT)	(Ib/VMT)	(Ib/VMT)	(%)	(Ib/hr)	(T/yr)	(lb/hr)	(T/yr)	(lb/hr)	(T/VF)
Unpaved Roads	0.33	2,920.0	0.15	1.46	4.93	%99	0.02	0.10	0.22	0.96	0.74	3.24
		Total					0.02	0.10	0.02 0.10 0.22 0.96 0.74 3.24	96.0	0.74	3.24

Notes:
1. Facility vehicle data based on estimates, GP5.1 and AP-42 Section 13.2.2 (17/06) defaults for industrial unpaved roads.

ucks)						
Heavy Irucks (Tanker Trucks)	23.7	18	2.0	2	365	1460.0
(Pick-up Trucks (Tanker Trucks) and Cers)	2.5	4	2.0	2	365	1460.0
	Average vehicle weight (tons):	Number of wheels per vehicle type:	Average number of round trips/day:	Distance per round trip (miles/trip)	Number of days operational (days/yr):	(ehicle miles travelled VMT (miles/yr):

Vehicle miles traveled was calculated with the following equation:

$$VMT = \sum_{vehicle Sypus} \frac{(avg.number of round trips}{day} \times \underbrace{vehicle nules traveled}_{round trip} \times \underbrace{vey}_{year}$$

2. Emission factor obtained from AP-42 Section 13.2.2 Table 13.2.2-1 (11/06), formula (1a) and formula (2).

$$E_{ext} = E\left[\frac{(365 - P)}{365}\right]$$
 where: 
$$E_{at} = \text{annual size-specific emission factor extrapolated for natural mitigation (Ib/VMT)}$$
 
$$E = \text{emission factor (Ib/VMT)}$$
 
$$E = \text{number of days in a year with at least 0.01 in of precipitation}$$
 
$$S = \text{surface meterial silt content (%)}$$
 
$$V_{B} = \text{near vehicle weight (tons)}$$
 
$$K, a, b = \text{empirical constants}$$

P (days/year): 150 s (%): 10 W (tons): 13.10

where:  $W_{avg} = \left(\frac{W_{empty} + W_{loaded}}{r}\right)$ 

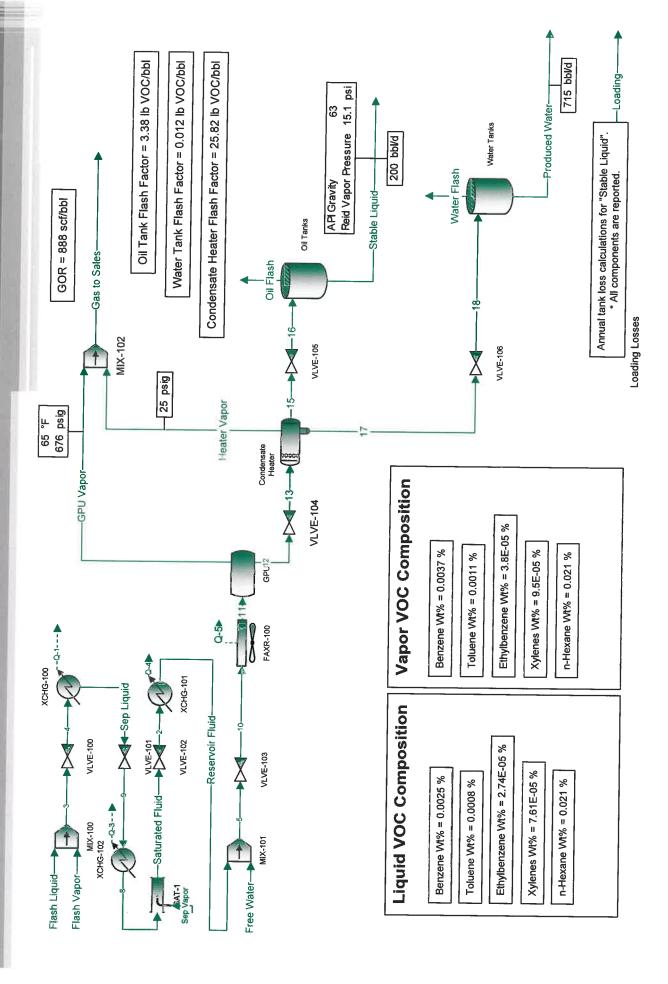
3. Natural control efficiency based on moisture ratio and AP-42 Section 13.2.2 Figure 13.2.2-2 (11/06). Controlled emissions are based on the natural rainfall cycles and no plant control.

Molsture Ratio: 2 Estimated based on 0.4% controlled and 0.2% uncontrolled surface water content Natural Control Efficiency (%): 55

4. Potential emissions based on AP-42 Section 13.2.2 Table 13.2.2-1 (11/06) emission factors and the listed control efficiecy.

Total Annual Emissions 
$$\binom{T/y_T}{2} = \left(\frac{VMT}{y_T \times Emission \ Factor}\right) \times (1 - Control \ Efficiency)$$

Criswell 405 Well No. 3H



# **Compositional Analysis of Separator Gas**

RFS ID No. 42552-02

Sample date and time: March 25, 2015 at 1625 hours Sampling Conditions: 676 psia at 80 °F Opening Conditions: 721 psia at 120 °F

	_		GPM at		Molecular
	Component	Mole %	14.85 psia	Weight %	Weight
$N_2$	Nitrogen	0.241	0.000	0.332	28.013
CO <sub>2</sub>	Carbon Dioxide	0.165	0.000	0.357	44.010
H <sub>2</sub> S	Hydrogen Sulfide *	0.000	0.000	0.000	34.082
C1	Methane	79.701	0.000	62.995	16.043
C2	Ethane	13.718	3.692	20.322	30.070
C3	Propane	3.893	1.081	8.457	44.097
iC4	Iso-Butane	0.561	0.185	1.608	58.123
nC4	N-Butane	0.882	0.280	2.524	58.123
iC5	Iso-Pentane	0.271	0.100	0.964	72.150
nC5	N-Pentane	0.194	0.071	0.689	72.150
C6	Hexanes	0.177	0.074	0.752	86.177
C7	Heptanes	0.089	0.040	0.427	97.327
C8	Octanes	0.056	0.026	0.299	107.827
C9	Nonanes	0.052	0.020	0.274	106.167
C10+	Decanes Plus	0.000	0.000	0.000	134.000
	Total	100.000	5.569	100.000	

 $<sup>^{\</sup>star}$  Please note that 0 ppm  $\mathrm{H_2S}$  was detected in the field by stain tube

# Calculated Properties of Gas

Data at 14.85 psia

Gas Specific Gravity (Air = 1.00)  Net Heat of Combustion (Btu/Cu.Ft. at 60 °F)	Dry	=======================================	0.7029 1.130.8	Real				
Gross Heat of Combustion (Btu/Cu.Ft. at 60 °F)	Dry	=	1,247.5	Real				
Gross Heat of Combustion (Btu/Cu.Ft. at 60 °F)	Wet	=	1,225.7	Water Sat.				
Gas Compressibility (1 Atm. at 60 °F)	Z	=	0.9967					
Heat of combustion is the quantity of heat produced when gas is burned completely to carbon dioxide and water.  □ Wet and dry refer to the condition of the gas prior to combustion.  □ Wet refers to a gas that is saturated with water vapor, and dry refers to a gas that contains no water vapor prior to combustion.  □ Refers to the condition of the water resulting from combustion.  □ Gross heat is the heat produced in complete combustion under constant pressure with the combustion products cooled to standard conditions and the water of the combustion products condensed to the liquid state.  □ Net heat is the heat produced in complete combustion under constant pressure with the combustion products cooled to standard conditions and the water of combustion products remains in the vapor phase.								

# Separator Liquid Composition RFS ID No. 42552-04

Flash Summary (1,800 psia and 80 °F to atmospheric pressure and 60 °F)

		-,	a de la della pilla pi	cooule all	4 00 F)
Gas-Oil Ratio	873	Scf/Stb	Color	Dark Amber	
Vapor Gravity	1.250	(Air = 1.00)	API Gravity (water free)		°API at 60 °F
Shrinkage	0.643	Vstd / Vsat	Water content by Karl Fisher	-	Weight %
Separator Liquid Density	0.624	g/cc at 676 psi	•	5.55	TV Signit 70

	Component	Flash	Flash	Flash	Molecular	Specific	Separator	Separator
1		Vapor	Liquid	Liquid	Weight	Gravity	Liquid	Liquid
	(Symbol / Name)	(mole %)	(mole %)	(weight %)		(water = 1.0)	(mole %)	(weight %)
N <sub>2</sub>	Nitrogen	0.000	0.000	0.000	28.01	0.809	0.000	0.000
CO <sub>2</sub>	Carbon Dioxide	0.091	0.000	0.000	44.01	0.818	0.046	0.027
H <sub>2</sub> S	Hydrogen Sulfide	0.000	0.000	0.000	34.08	0.801	0.000	0.000
C1	Methane	33.495	0.118	0.016	16.04	0.300	17.150	3.675
C2	Ethane	26.600	0.091	0.024	30.07	0.356	13.618	5.470
C3	Propane	19.211	1.024	0.391	44.10	0.507	10.305	6.070
iC4	i-Butane	4.369	1.080	0.543	58.12	0.563	2.758	2.142
nC4	n-Butane	7.933	3.511	1.767	58.12	0.584	5.767	4.478
iC5	i-Pentane	3.005	4.399	2.747	72.15	0.624	3.688	3.554
nC5	n-Pentane	2.141	5.764	3.600	72.15	0.631	3.915	3.773
C6	Hexanes	1.843	13.368	9.974	86.18	0.664	7.487	8.619
C7	Heptanes	0.724	15.345	12.931	97.35	0.700	7.884	10.252
C8	Octanes	0.309	16.603	15.799	109.89	0.724	8.288	12.167
C9	Nonanes	0.063	10.208	10.764	121.79	0.756	5.031	8.185
C10	Decanes	0.216	6.584	7.638	135.68	0.779	3.335	6.043
C11	Undecanes		4.523	5.756	147.00	0.790	2.215	4.349
C12	Dodecanes		4.408	6.143	161.00	0.801	2.159	4.642
C13	Tridecanes		4.922	7.457	175.00	0.812	2.410	5.635
C14	Tetradecanes		3.702	6.090	190.00	0.823	1.813	4.601
C15	Pentadecanes		2.184	3.895	206.00	0.833	1.070	2.943
C16	Hexadecanes		1.166	2.242	222.00	0.840	0.571	1.693
C17	Heptadecanes		0.509	1.044	237.00	0.848	0.249	0.789
C18	Octadecanes		0.255	0.554	251.00	0.853	0.125	0.419
C19	Nonadecanes		0.065	0.147	263.00	0.858	0.032	0.413
C20	Eicosanes		0.046	0.110	275.00	0.863	0.032	0.083
C21	Heneicosanes		0.017	0.042	291.00	0.868	0.028	0.032
C22	Docosanes		0.017	0.044	305.00	0.873	0.008	0.032
C23	Tricosanes		0.017	0.047	318.00	0.878	0.008	0.035
C24	Tetracosanes		0.015	0.043	331.00	0.882	0.007	0.032
C25	Pentacosanes		0.016	0.049	345.00	0.886	0.008	0.032
C26	Hexacosanes		0.015	0.045	359.00	0.890	0.007	0.035
C27	Heptacosanes		0.010	0.034	374.00	0.894	0.007	0.035
C28	Octacosanes		0.006	0.021	388.00	0.897	0.003	0.024
C29	Nonacosanes		0.006	0.019	402.00	0.900	0.003	0.016
C30+	Triacontanes Plus		0.006	0.024	426.00	0.906	0.003	0.016
Total		100.000	100.000	100.000				
	ed Mole Weight	35.85	115.51	100.000			100.000	100.000
	ed Mole Weight	00.00	123.54				74.86	
	nositional groupings h	<del>-</del>						

- $\hfill\Box$  Compositional groupings based on normal to normal carbon distribution.
- $\hfill \Box$  Pristane is included as  $C_{17}$  and Phytane is included as  $C_{18}.$

Compositional Groupings of Separator Liquid

Group	Mole %	Weight %	MW	SG
Total Fluid	100.000	100.000	74.86	
C7+	35.266	62.192	132.02	0.764
C10+	14.062	31.587	168.17	0.808
C20+	0.084	0.360	322.19	0.879
C30+	0.003	0.017	426.00	0.906

# **Compositional Analysis of Separator Gas**

RFS ID No. 42552-02

Sample date and time: March 25, 2015 at 1625 hours Sampling Conditions: 676 psia at 80 °F Opening Conditions: 721 psia at 120 °F

	0	**   0/	GPM at		
	Component	Mole %	14.85 psia	Weight %	Weight
$N_2$	Nitrogen	0.241	0.000	0.332	28.013
CO <sub>2</sub>	Carbon Dioxide	0.165	0.000	0.357	44.010
H <sub>2</sub> S	Hydrogen Sulfide *	0.000	0.000	0.000	34.082
C1	Methane	79.701	0.000	62.995	16.043
C2	Ethane	13.718	3.692	20.322	30.070
C3	Propane	3.893	1.081	8.457	44.097
iC4	Iso-Butane	0.561	0.185	1.608	58.123
nC4	N-Butane	0.882	0.280	2.524	58.123
iC5	Iso-Pentane	0.271	0.100	0.964	72.150
nC5	N-Pentane	0.194	0.071	0.689	72.150
C6	Hexanes	0.177	0.074	0.752	86.177
C7	Heptanes	0.089	0.040	0.427	97.327
C8	Octanes	0.056	0.026	0.299	107.827
C9	Nonanes	0.052	0.020	0.274	106.167
C10+	Decanes Plus	0.000	0.000	0.000	134.000
	Total	100.000	5.569	100.000	

<sup>\*</sup> Please note that 0 ppm H<sub>2</sub>S was detected in the field by stain tube

## Gas Specific Gravity (Air = 1.00) 0.7029 Net Heat of Combustion (Btu/Cu.Ft. at 60 °F) Dry = 1,130.8 Real Gross Heat of Combustion (Btu/Cu.Ft. at 60 °F) Dry = 1,247.5 Real Gross Heat of Combustion (Btu/Cu.Ft. at 60 °F) Wet = 1,225.7 Water Sat. Gas Compressibility (1 Atm. at 60 °F) Ζ 0.9967 ☐ Heat of combustion is the quantity of heat produced when gas is burned completely to carbon dioxide and water. Wet and dry refer to the condition of the gas prior to combustion. Wet refers to a gas that is saturated with water vapor, and dry refers to a gas that contains no water vapor prior to combustion. Net and gross refer to the condition of the water resulting from combustion. Gross heat is the heat produced in complete combustion under constant pressure with the combustion products cooled to standard conditions and the water of the combustion products condensed to the liquid state. □Net heat is the heat produced in complete combustion under constant pressure with the combustion products cooled to standard conditions and the water of combustion products remains in the vapor phase.

Calculated Properties of Gas

Data at 14.85 psia

# Attachment O: Monitoring/Recordkeeping/Reporting/Testing Plans

# Monitoring/Recordkeeping/Reporting/Testing Plans

Ascent will monitor, record, report, and test as required by 45CSR6 and 45CSR13.

Ascent will maintain a Certificate of Conformity for the generator (ENG-2), as required by 40 CFR Part 60 NSPS Subpart JJJJ.

# **Attachment P: Public Notice**

# AIR QUALITY PERMIT NOTICE Notice of Application

Notice is given that Ascent Resources – Marcellus, LLC has applied to the West Virginia Department of Environmental Protection, Division of Air Quality, for a Construction Permit for the WJ Criswell 405 facility located near Wileyville, in Wetzel County, West Virginia. The latitude and longitude coordinates are: 39.60737°N, -80.61828°W

The applicant estimates the potential to discharge the following Regulated Air Pollutants will be:

 $NO_x = 10.07 \text{ TPY}$  CO = 34.82 TPY VOC = 23.33 TPY  $PM_{10} = 0.28 \text{ TPY}$   $SO_2 = < 0.01 \text{ TPY}$ HAPs = 0.17 TPY

Startup of operation is planned to begin on or about the 16th day of November, 2016. Written comments will be received by the West Virginia Department of Environmental Protection, Division of Air Quality, 601 57<sup>th</sup> Street, SE, Charleston, WV 25304, for at least 30 calendar days from the date of publication of this notice.

Any questions regarding this permit application should be directed to the DAQ at (304) 926-0499, extension 1250, during normal business hours.

Dated this the 16th day of November, 2016.

By: Ascent Resources – Marcellus, LLC Tim Cummings VP - Operations PO Box 13678 Oklahoma City, OK 73113

# Attachment Q: Business Confidential Claims (Not Applicable)

# Attachment R: Authority Forms (Not Applicable)

# Attachment S: Title V Permit Revision Information (Not Applicable)

# **Application Fee**